

# FUNGIBLE AND COMPATIBLE BIOFUELS: LITERATURE SEARCH, SUMMARY, AND RECOMMENDATIONS

September 30, 2010

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Oak Ridge National Laboratory Fuels, Engines, and Emissions Research Center



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#### 1. PURPOSE

#### 1.1 PURPOSE OF STUDY

The purpose of this study is to summarize the various barriers to more widespread distribution of biofuels through our common carrier fuel distribution system, which includes pipelines, barges and rail, fuel tankage, and distribution terminals, and with a special focus on biofuels, which may come into increased usage in the future. Addressing these barriers is necessary to allow the more widespread utilization and distribution of biofuels, in support of a renewable fuels standard and possible future low-carbon fuel standards. By identifying these barriers early, for fuels not currently in widespread use, they can be addressed in related research and development. These barriers can be classified into several categories, including operating practice, regulatory, technical, and acceptability barriers. Possible solutions to these issues are discussed, including compatibility evaluation, changes to biofuels, regulatory changes, and changes in the distribution system or distribution practices. No actual experimental research has been conducted in the writing of this report, but results are used to develop recommendations for future research and additional study as appropriate.

This project addresses recognized barriers to the wider use of biofuels in the areas of development of codes and standards, industrial and consumer awareness, and materials compatibility issues.

Specific information tasks for the report include the following. Where possible, the information provided is linked to characteristics of specific biofuels, both current and emerging.

- **Background and current operating practices.** Fuel blending, pipelines, and distribution practices have developed over a long period of time and operate very efficiently and safely for fuels of specific types. This section will describe how the current pipeline and distribution system are constructed and operated and how this may limit the ability to refinery-blend and distribute biofuels.
- Regulatory barriers to expanded distribution of biofuels. Fuels that are shipped over common carrier distribution must be acceptable to all parties receiving the fuel, and this has resulted in the development of fungibility specifications for fuels. Fuels accepted by pipelines must generally meet fungibility specifications, compatibility specifications, and all legal requirements. This section will describe how current fungibility specifications and pipeline specifications affect the ability to refinery-blend and distribute biofuels.
- **Technical barriers to pipeline distribution of biofuels.** Legal requirements and fungibility specifications aside, there may also be valid compatibility reasons for not introducing specific biofuels into the common carrier distribution system. This section will discuss the actual physical and technical barriers to biofuel distribution which must be solved to allow the more widespread distribution of biofuels.
- Additional barriers and concerns. This section will describe other barriers to more widespread
  distribution of biofuels which do not fall readily into the other categories. Examples of these include
  cross contamination of product, ground water contamination, consumer acceptance and perception,
  lack of operating experience with a new fuel, and compatibility concerns with existing and future
  engines and vehicles.
- **Possible solutions to problems outlined.** The barriers outlined above can be overcome by a number of means, some of which are most applicable to a given barrier and some of which may be easier or more difficult to implement. These solutions fall into the categories of verification of performance

and compatibility of possible future biofuels, chemical modification of biofuels, changes in current fuel specifications, modifications of fuel distribution procedures and operating practices, or modifications to the current fuel distribution system.

#### 1.2 DEFINITION OF FUNGIBILITY

Fungible fuels are those fuels in common use, with common specifications, distributed in a comingled manner, and with sufficient specifications and quality control that they, within a given type, can be substituted for each other without concern of source or end use. Fungible fuels of specific types can be intermixed during distribution and storage without concerns relative to quality or specifications. Fuel specifications are published by a number of regulatory agencies, including ASTM, the U.S. Environmental Protection Agency, and state agencies, and then adopted as controlling specifications for the receipt, distribution, and delivery of fuels on common carrier systems. There are many fungible fuel specifications, and they vary by fuel type, fuel grade, area of the country where sold, and season [26, 37, 40, 50, 61, 95, 102, 118, 125, 145, 149, 162].

#### 1.3 DEFINITION OF COMPATIBILITY

Compatible fuels are fuels that would be considered compatible with the infrastructure transporting them, both from the standpoint of no damage by or to the equipment and from the standpoint of no harm from or to other fuels using the same distribution infrastructure [104]. Compatible fuels would also be suitable for use in the vehicle or application intended, in a manner indistinguishable from other fuels. Distribution system compatibility in a fuel may require additional specifications to be met, beyond a fuel's regulated and performance specifications, and these additional requirements are normally included in a fungible fuel specification.

# 2. DESCRIPTION OF FUEL MANUFACTURING AND DISTRIBUTION IN THE UNITED STATES

The following description of petroleum refining and distribution is taken from public sources on this subject, ranging from books to company and association websites. This description is intended to set the stage for a discussion of the differences between biofuels and petroleum-derived fuels and how these differences might affect distribution operations.

Petroleum fuels are manufactured in the United States from crude oil at oil refineries and are then distributed to terminals for final distribution to service stations and end users. Most commonly, crude is received at refineries by pipeline, barge, tanker, or rail and distributed by pipeline, rail, barge, or truck. Most crude oil and finished fuels are moved by pipeline. The United States consumes about 19.5 million barrels per day of finished petroleum-based fuels, mainly as gasoline, diesel fuel, jet fuel, and heating oil. Of this, 43% is refined in the United States, and 57% is received from other countries [152]. U.S. oil refining, fuel distribution, and fuel specifications have grown and evolved over many years to meet demand, product requirements, and quality requirements and now represent a large entrenched infrastructure and a correspondingly large investment, designed specifically for processing and distribution of petroleum-based products.

#### 2.1 CRUDE REFINING

In the processing of crude oil, an oil refinery uses distillation (separation by boiling point) to split crude into a number of fractions for further processing at more specialized process units. Distillation is also used at the output of many of these units to separate finished streams from materials recycled for further processing. Various types of process units can remove sulfur, nitrogen, or oxygen, add hydrogen, reshape molecules, or split or combine molecules. These individual refinery streams are then transferred to blending operations where they are combined to produce finished fuels of required specifications. The balancing of a refinery operation is complex and adjusted both daily and seasonally to compensate for product demands, product shipping cycles, crude characteristics, and process unit operation. Diesel fuel is typically composed of three to five blending streams and gasoline of five to seven blending streams, which are blended to meet the specifications for the given product, season, and region of use. Products can be blended in real time, on line, and immediately put into a pipeline or other form of transportation or batched to storage tanks for later shipment.

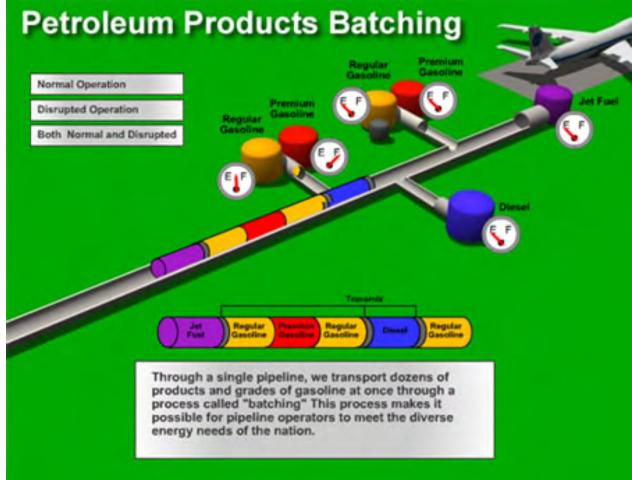
#### 2.2 PIPELINE DISTRIBUTION

The majority of the distribution infrastructure, mainly pipelines, tanks, and related equipment, is composed of low carbon and low alloy steels, and controlling rust and corrosion is of primary importance. This is largely monitored by a series of standard rust and corrosion tests and periodic thickness measurements and controlled through the use of corrosion and rust inhibitor additives. Generally, pipelines only allow specific additives to be used, at minimum concentrations necessary to achieve a desired result. Petroleum products leaving a refinery will often be above ambient temperature and will contain some dissolved water from various refining operations. In addition, water can sometimes enter finished products through storage tanks or by contact in barges and tankers. With time and cooling, this water will drop out in storage tanks and can be disposed of. Storage tanks are designed to allow the accumulation of water and dirt for periodic removal. Since water bottoms are often considered hazardous waste, there is limited opportunity for continuous removal and disposal at product terminals. As long as the water or dirt is not reentrained into product being sold, it causes no harm to remain in contact with petroleum-derived fuels, although bacteria growth must be controlled at the water-petroleum interface. Tank inlets and suctions are designed to minimize stirring of a product during normal operations to prevent reentrainment of water or dirt.

Pipelines run products in cycles, with batches of one type of product being followed by a batch of another product. Large batches of a given product may originate from several refineries and breakout tanks and end up at multiple terminals along a pipeline. Fungibility allows the co-mingling of product without concern for source or end user. Products follow a defined sequence to minimize cross-contamination and to allow ability to detect product and batch changes. Normally, batch detection is done by monitoring for fluid density changes between the sequential batches. Between batches, a small amount of co-mingled product, known as interface or transmix, is generated and is normally segregated for refractionation to diesel and gasoline or returned to a refinery for processing. Figure 1 shows a typical batch sequence for refined pipeline products.

#### 2.3 TERMINAL BLENDING

At a product terminal, individual tanks store specific products, which are then sent to a truck loading rack for distribution to service stations or other users. Tanker trucks can have one large compartment or several smaller compartments. Occasionally, smaller pipelines may send product directly to an end user such as an airport or for a dedicated service station located near a terminal. For biofuels, the loading rack at a product terminal is currently the most common entry point into the distribution system. On-line blending equipment is used to blend a petroleum-based product with biofuels, proportionally by volume,



Source: (www.pipeline101.com)

Figure 1. Typical batch sequence for refined pipeline products. [167]

during truck loading. The biofuels (ethanol and fatty ethyl methyl esters, or FAME) are brought into a terminal by truck, rail, or barge and kept in dedicated tanks until blended. FAME is the most common form of biodiesel in use today and is often referred to as biodiesel. In this report, the term *FAME* is used to describe 100% FAME, *FAME biodiesel* is used to describe blends of FAME and diesel fuel, and *biodiesel* is used to describe other forms of bio-derived diesel fuels.

Refinery blending of products differs in several ways from blending done at a terminal. First, a refinery has a number of blending streams available and generally has multiple options to achieve a fuel specification. A refinery has an analytical laboratory and on-line monitoring equipment that allows blending to product specifications. A refinery also has storage tankage and more options for dealing with any off-specification product. In contrast, a terminal has only the capability to blend to volume percentage, during truck loading, between two components. These blended components must be designed to meet a final product specification after blending, since a terminal does not typically have the capability (in the form of additional blend streams, additional storage tankage, or analytical equipment) to blend to specification or to adjust off-specification product.

#### 2.4 EXAMPLE PIPELINE DISTRIBUTION MAP

Figure 2 provides an example of part of the petroleum distribution infrastructure in the United States. The map displays the distribution and storage holdings of Nu Star Logistics, one of the ten largest U.S.-based pipeline companies, with over 8000 miles of pipeline transporting over 800,000 barrels per day. This particular pipeline network (including a variety of pipeline types, such as crude, refined, ammonia, singleuse, etc.) is centered in the Midwest, as are the crude oil storage facilities. There are a number of product terminals on the east and west coasts that are not served by a Nu Star pipeline. These are either reached by rail, truck, barge (likely for port cities), third-party pipelines, or a combination thereof. This particular map is included for illustrative purposes and does not portray the entire U.S. fuel distribution infrastructure.



**Figure 2. Nu Star Logistics distribution map.** [118] Note that there are at least ten major pipeline companies operating in the United States, and this particular map has been included to illustrate one of them. It does not provide a total picture of pipeline infrastructure.

#### 3. INCORPORATING BIOFUELS INTO THE CURRENT DISTRIBUTION SYSTEM

#### 3.1 ISSUES WITH OXYGENATED BIOFUELS

Current biofuels (ethanol and FAME) contain oxygen and are polar molecules. This polarity makes them behave differently than hydrocarbon fuels and results in the need for different handling and distribution practices. This polarity results in a greater affinity for other things, such as water, dirt, and surfaces. Water, which is normally present in the fuel distribution system for reasons described above, can be dissolved into a biofuel at greater amounts than in a corresponding petroleum fuel, and this can result in product quality problems during use. FAME can dissolve substantially more water than can petroleum fuels [111, 114], and ethanol is highly soluble with water and can dissolve large amounts of water into an ethanol-gasoline mix; ethanol can segregate out of an ethanol gasoline mix and into a water phase [42]. Dissolved water in biofuels can also contribute to corrosion and stress corrosion cracking. Stress corrosion cracking of mild steel may be of particular concern with ethanol [124], and further study of ethanol-induced corrosion is one of the recommendations of this report. The polarity of ethanol and FAME can also make the separation of dirt and water more difficult or slower than for petroleum fuels. Low-level FAME contamination in jet fuel is also of current concern and is being studied. Possible solutions to this issue include careful batch sequencing or the use of a separate, parallel pipeline to segregate jet fuel from FAME biodiesel.

#### 3.2 CURRENT PRACTICES AND PROPOSED SOLUTIONS

The current practices of adding FAME and ethanol during truck loading minimizes the opportunity for contact with water and dirt but may be more difficult for the larger volumes of biofuels required in the future. Expansion of the use of bio-derived fuels would be easier if they did not require separate shipping to multiple distribution points but could be handled with existing infrastructure at refineries. The problems cited can be alleviated by modifications to the fuels themselves or by modifications to the distribution equipment and practices. Table 1 outlines some of the distribution problems associated with biofuels usage, with a variety of solutions including fuel, equipment, or operating practice modifications.

Examination of the table indicates the possibility of multiple or combined solutions ranging from product changes, equipment modifications, and changes in operating practices. None of these changes are particularly difficult from a science or engineering viewpoint, but some may require considerable investment in modifying distribution or refining equipment. It is likely that final solutions will be a combination of several of these options. Additional study, development, and research by the Department of Energy and the companies involved should provide the necessary information and guidance to allow such decisions to be made.

Table 1. Distribution problems related to biofuels and possible fixes

Distribution problem	Fuel fix	Equipment fix	Operating fix
Water in product	Less polar form of biofuel, such as butanol vs. ethanol or converting oils or fats to hydrocarbons rather than esters	Design tankage to minimize contact between water and product, use of separators to remove water	Drain water bottoms more frequently, combined with careful monitoring*
Dirt in product	Less polar form of biofuel	Design tanks to reduce reentrainment of dirt,* use filtration to remove dirt	Keep tanks clean, combined with careful monitoring*
Cross- contamination of products	Less polar form of biofuel	Equipment for better interface detection and separation of transmix	Batch sequencing, combined with careful monitoring and separation of transmix*
Corrosion and rust of mild or low alloy steel	Make fuel more petroleum- like, reduce dissolved water, reduce fuel polarity, selection and use of effective corrosion inhibitors	Use corrosion resistant steels	Monitoring and maintenance, corrosion inhibitors*
Material compatibility other than corrosion and rust	Make fuels more petroleum- like	Change to more compatible materials	Maintenance and monitoring*

<sup>\*</sup>Current practices may need to be executed more frequently with biofuels.

#### 4. CURRENT STATE OF THE MARKET

#### 4.1 RFS2 REQUIREMENTS

The Renewable Fuel Standard (RFS1) was established by the U.S. Energy Policy Act of 2005. It was the first specific renewable fuel volume mandate in U.S. history. It mandated that by 2012 at least 7.5 billion gallons of renewable fuel be blended into gasoline annually. RFS1 delineated three specific types of renewable fuel: grain ethanol, ethanol from cellulosic sources, and biomass-based diesel, which was defined but not mandated. Under the Energy Independence and Security Act of 2007, the Renewable Fuel Standard was revised and its scope expanded in an effort to accelerate energy independence and security, to keep pace with emerging renewable fuel technologies, and to provide greater detail concerning the ways in which the mandate is to be met. This set of extensive revisions became known as RFS2 [51].

RFS2 significantly increases the renewable fuel volume mandate, starting with 9 billion gallons required by 2008 and increasing yearly to 36 billion gallons by 2022. The mandate also applies to blending with diesel fuels as well as with gasoline. Consequently, the number and types of renewable fuels that fall under the RFS2 are increased over those of RFS1. Renewable fuels covered under RFS2 now fall into one of five categories: cellulosic biofuel made from cellulose, hemicellulose, or lignin sources; biomass-based diesel defined as any non-co-processed diesel fuel from renewable sources; advanced biofuel, which is defined as any renewable fuel not made from corn starch; renewable biofuel, which is meant to include corn-based ethanol; and a special class that includes cellulosic-based diesel fuel. Each of these categories has its own corresponding volume mandate and lifecycle greenhouse gas emissions requirements, summarized in Figure 3 and Table 2.

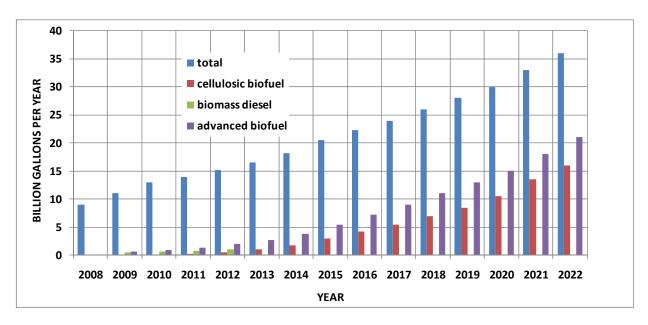


Figure 3. RFS2 mandated annual biofuels usage. [51]

Table 2. RFS2 fuel categories [51]

Fuel type	2010 mandated volume (billion gallons)	2022 mandated volume (billion gallons)	Life-cycle GHG reductions^	Possible fuels included	Example feedstocks
Cellulosic biofuel	0.1	16	60%	Ethanol	Corn stover, switchgrass
Biomass-based diesel	0.65	TBD	50%	FAME, Green diesel, Algae biodiesel	Soy, palm, rapeseed, algae oil
Advanced biofuel	0.95	21	50%	Green gasoline	Sugar cane, agricultural residue
Renewable biofuel	12.95 – CBA*	36 – CBA*	20%	Ethanol	Corn starch
Cellulosic biodiesel <sup>#</sup>	N/A	N/A	60%	Pyrolysis oil- based biodiesel	Wood chips

<sup>\*</sup> Can be adjusted—Renewable biofuel volume is the difference between the total yearly volume mandate and the sum of the individual volume mandates for the cellulosic, biomass-based diesel, and advanced categories. The EPA can determine that the yearly mandate for an individual category cannot feasibly be met, but it does not have the authority to reduce the total RFS2 volume mandate. Renewable biofuels derived from grain are limited to 15 billion gallons per year.

<sup>^</sup>Each fuel category has a corresponding life-cycle greenhouse gas (GHG) emissions reduction requirement when compared to the petroleum-based fuel counterpart (either gasoline or diesel).

<sup>#</sup> Cellulosic biodiesel is a special category that is comprised of cellulosic biomass-based diesel fuel. When this fuel also provides a greenhouse gas emissions reduction of at least 60% compared to petroleum diesel, the fuel can be used to satisfy either the cellulosic requirement or the biomass-based diesel requirement.

The RFS2 regulations also provide specific rules governing land use for biofuel feedstocks. Numbers and credits are affixed to each gallon of qualifying biofuel produced. Once the biofuel is transported to the end user, the credits are detached and become tradable commodities and serve as proof that individual mandates have been met by the fuel manufacturer, blender, or importer. All of these improvements to RFS1 create a policy climate that places emphasis on both biofuel diversification and biofuel cost. RFS2 will play a dominating role in biofuels utilization for the foreseeable future.

#### 4.2 CURRENT PRODUCTION OF ETHANOL AND FAME

Table 3 summarizes available information concerning current or recent biofuels production and capacity in the U.S. for biofuels discussed in this report.

Fuel	U.S. production (billion gallons)	U.S. production capacity (billion gallons)	Year of available data
FAME [171]	0.545	2.74	2009
Ethanol [170]	11.88	13.03	2010

Table 3. Current U.S. biofuels production

### 4.3 HOW THE CURRENT MARKET DEALS WITH COMPATIBILITY AND FUNGIBILITY ISSUES

The two major current biofuels in the United States, ethanol as a gasoline blending component and FAME as a diesel blending component, are either expressly or de facto prohibited in pipelines operated by most of the ten largest pipeline companies. The compatibility and fungibility issues associated with both ethanol and FAME, as well as the other biofuels in this report, are discussed in greater detail later in this report and in the Excel workbook. The most notable compatibility issues are water solubility and stress corrosion cracking for ethanol, and fuel contamination and cold flow performance for FAME. Five of the ten largest U.S. pipeline companies expressly prohibit alcohols and ethers as "blending components in gasoline at (refinery) origin." Six of the ten companies either expressly prohibit FAME or place freeze and cloud point restrictions on diesel fuel that serve as de facto prohibitions on FAME blending at the refinery [26, 37, 40, 50, 61, 95, 102, 118, 125, 145, 149, 162].

While there are emerging exceptions to the above prohibitions (see the following discussion of Kinder Morgan's experience with biofuels fungibility), ethanol and FAME biodiesel are generally not transported via the existing petroleum pipeline infrastructure. They are generally rack-blended with gasoline or diesel fuel at distribution terminals, and the mixtures are then sent to service stations via truck.

#### 4.4 CASE STUDY: THE KINDER MORGAN EXPERIENCE

Kinder Morgan Energy Partners, one of the largest oil pipeline companies in the United States, is one of the several companies that have successfully demonstrated biofuel transport through the petroleum pipeline infrastructure [95]. In 2008, Kinder Morgan began shipping neat ethanol through a 115-mile stretch of gasoline pipeline in Central Florida. To prevent or mitigate the major impedances to ethanol pipeline shipment—namely, water solubility, stress corrosion cracking, and the cleaning effect—the pipeline was first cleaned and all potential water sources were removed. Kinder Morgan utilized a proprietary mix of corrosion inhibitors in an effort to prevent stress corrosion cracking. Neat ethanol is, as of early 2010, routinely shipped on this pipeline, and no problems have been reported.

Kinder Morgan has also experimented with shipping FAME biodiesel over the Plantation pipeline network located in the southeastern United States. Initially, a B5 blend was shipped over 500 miles of diesel pipeline. The critical issue of FAME contamination of jet fuel was bypassed due to the existence of a parallel pipeline that allowed jet fuel and FAME biodiesel to remain segregated. The results of this experiment were ultimately positive. As of early 2010, Kinder Morgan allows the shipment of B2, B5, and/or B100 over 8000 miles of pipeline.

This case study demonstrates that while the water solubility, cleaning effect, contamination, and stress corrosion issues associated with ethanol and FAME pipeline shipping are significant, they are not insurmountable. Proper cleaning, chemical additives, segregation/batch sequencing, parallel pipelines, and monitoring can either eliminate or greatly mitigate these problems and make ethanol and FAME pipeline shipment possible.

#### 5. FUEL SOURCES

#### 5.1 FUELS CONSIDERED

The biofuels considered in this report are discussed in three sections, with more detail as the options are narrowed to biofuels considered to be of greater importance and higher likelihood for future use. The three sections are "all biofuels," "all biofuels of higher priority," and "biofuels of higher priority which would benefit from further study on certain key questions." Each of these fuel sections is also classified by end use by separation into four categories: gasoline-like fuels, diesel-like fuels, biocrudes and refinery intermediates, and other fuels. Gasoline-like and diesel-like fuels are biofuels that are intended for combustion in spark-ignition and compression-ignition engines, respectively, and possess physical and chemical properties that are intended to be similar to gasoline or diesel fuel. These categories include fuels such as ethanol, butanol, and FAME. The biocrudes and intermediates category contains biofuels that are not fuels until they are further refined, in much the same way as petroleum crude is further refined into gasoline, diesel, etc. before reaching the end-user. Biocrudes and intermediates include pyrolysis oil and syngas. The other fuels category includes methane and hydrogen, fuels that do not have similar properties to either gasoline or diesel but nevertheless can be utilized in dedicated vehicles. These latter fuels are examined with the understanding that they, by nature, cannot be incorporated into the existing petroleum distribution infrastructure, but rather their own distribution infrastructures are extensive enough to warrant research into the fungibility prospects of their biomass-based equivalents.

#### 5.2 ALL BIOFUELS

Table 4 lists all the fuels considered in the preparation of this report, classified by the types discussed previously. Each of these fuels is discussed in detail in the exhibits at the end of this report. Each fuel has two exhibits. The first consists of available fuel properties and environmental impact data for each fuel as compared to its petroleum-derived counterpart. The second exhibit consists of materials compatibility data, vehicle compatibility data, transporting precautions, environmental and health concerns, fungibility and distribution issues, current production, and overall advantages and disadvantages of distribution and use of each particular fuel, along with references.

Also included in the exhibits is information concerning the ten largest oil pipeline companies in the United States in terms of daily transported volume. This information includes pipeline network location and mileage, products transported, and prohibitions, particularly how these relate to biofuel distribution. Other exhibits include federal hazmat transport regulations, information on where specific biofuels can theoretically be inserted into the distribution chain, capital and operating cost analysis for several types of biofuel production facilities, and a list of federal and state policies and initiatives designed to drive

increased biofuel usage. (The information contained in the exhibits can be acquired from the authors as an Excel workbook.)

The list of fuels considered in Table 4 was narrowed to those which are of higher priority or of greater interest to DOE during preliminary discussions of results. These fuels are discussed in greater detail in the next section.

Table 4. Fuel types considered

		Gasoline-like	Biocrudes and	
Fuels	Diesel-like fuels	fuels	intermediates	Other fuels
FAME	X			
Green diesel	X			
F-T diesel	X			
Algae biodiesel	X			
DME	X			
Glyme	X			
Ethanol-diesel blends	X			
Sesquiterpene	X			
Green gasoline		X		
F-T gasoline		X		
Ethanol		X		
Biobutanol		X		
Methanol		X		
Propanol		X		
Higher C alcohols		X		
Pyrolysis oils			X	
Syngas			X	
Lignin liques			X	
Sugars and alcohols			X	
Terpenes			X	
Isoprene			X	
Methane				X
Hydrogen				X

#### 5.3 FUELS OF HIGHER PRIORITY OR INTEREST

From Table 4, ten fuels were chosen for examination in greater depth. These fuels are of higher priority or of greater interest as they are most likely to provide a significant portion of bio-derived fuels in the future. These fuels are listed in Table 5, which also summarizes the knowledge we were able to uncover about

Table 5. Detailed summary table for fuels considered to be of higher priority or greater interest

Compound, fuel,					Environmental	Compatibility	Areas needing	Cost compared to	
or component	Use, purpose	Advantages	Property issues	Infrastructure issues	characteristics	questions	further atudy	petroleum derived	References
FAME (biodiesel)	Diesel substitute or blend component	Currently in use, relatively easy to manufacture, generally higher cetane	Cold flow, stability, filter plugging, higher viscosity, lower energy content	Pick up of dirt and water, cleaning effect, contamination of other fuels, storage stability, prohibited in most pipelines	Relatively non-toxic, biodegerades easily	Problems with terne- coated steel (older vehicle fuel tanks), nitrile and natural rubber	Shipment over common carrier pipelines, cross contamination on other fuels	Same to higher depending on feedstock	8, 17, 36, 39, 89, 99, 101, 111,112, 114, 139, 146
Green diesel	Diesel substitute or blend component	Closest to drop-in replacement, option to optimize further	Very little information or production at present, chemistry may be somewhat different from petroleum derived fuels	None known	Similar to petroleum diesel, well understood	Similar to petroleum diesel, well understood	More definition of chemistry and properties, use as a blending component or finished fuel	Not known	76,92, 115, 130, 142, 155, 165
Fischer-Tropsch (F-T) diesel	Diesel substitute or blend component	Generally higher cetane, zero sulfur, option to optimize further	Possible cold flow problems, can be controlled with chemistry, slightly lower energy content	None known	Similar to petroleum diesel, well understood	Similar to petroleum diesel, well understood	Probably none, well understood	Higher	7, 34, 86, 93, 110
Algae biodiesel	Diesel substitute or blend component	Completely new source of fuel with potential for high volume	Cold flow, stability, filter plugging, higher viscosity, lower energy content, more unsaturates than fame	Pick up of dirt and water, cleaning effect, contamination of other fuels, storage stability, prohibited in most pipelines	Relatively non-toxic, biodegrades easily	Problems with terne- coated steel (older vehicle fuel tanks), nitrile and natural rubber	Same as FAME + study of detailed chemistry and properties, production, and logistics	Not known	33, 108
Green gasoline	Gasoline substitute or blend component	Closest to drop-in replacement, option to optimize further	Very little information or production at present, chemistry may be somewhat different from petroleum derived fuels	None known	Similar to petroleum diesel, well understood	Similar to petroleum diesel, well understood	More definition of chemistry and properties, use as a blending component or finished fuel	Not known	None found
Fischer-Tropsch (F-T) gasoline	Gasoline substitute or blend component	Zero sulfur, option to optimize further	May have slightly lower energy content	None known	Similar to petroleum diesel, well understood	Similar to petroleum diesel, well understood	Probably none—well understood	Higher	93
Ethanol	Gasoline blend component	High octane, largest current biofuel volume, well understood	Lower energy content (up to 28% MPG penalty), requires special low RVP blend stock (readily available)	Segregation into and dissolving of water in distribution system, cleaning effect, prohibited in most pipelines	Miscible in water, toxic in high concentrations, biodegrades easily	Incompatible with hose and fuel tank material in older vehicles, but current approved as 10% blend in all vehicles	Potential for pipeline shipments, stress corrosion cracking	Similar to higher depending on feedstock	11, 20, 21, 42, 124, 143, 158, 163
Butanol	Gasoline blend component	Similar characteristics to ethanol, but differences compared to petroleum gasoline are much less, can be same or slightly higher octane, provides more renewable gallon credits for same oxygen blend limit	Limited experience with use of butanol	Goal is to ship blends over common carrier pipelines, but currently prohibited in most pipelines	Miscible in water (less than ethanol), toxic in high concentrations, should biodegrade easily, but requires more study	Similar characteristics to ethanol, but differences compared to petroleum gasoline are much less	Properties of various isomers and isomer mixtures, shipping studies for common carrier distribution system	Not known, probably higher than ethanol	1, 6, 10, 12, 25, 27, 70, 103, 121, 135, 154, 156
Pyrolysis oil	Biocrude, refiner feedstock	Direct route from biomass to liquid product	Stability problems, not miscible with petroleum crude, high water and oxygen content, high viscosity, corrosive, solids content	Can't be shipped as crude oil, must be stabilized before storage and shipment	Moderately toxic, biodegrades quickly	Deposits and filter plugging, settling of solids, corrosive to aluminum and mild steel	Amount of stabilization required to allow shipping as or with crude oil, study of stabilization methods	Probably lower than crude oil, but also lower fuel value and requires both stabilization and refining	22, 35, 44, 49, 119, 129, 140
Syngas	Biocrude, refiner feedstock	Can be derived from biomass, provides CO and H2 for refinery applications	Also contains CO2, H2O and other impurities, unless purified	Currently no infrastructure for shipping, generated at point of use	CO is highly toxic, syngas very flammable	Can be corrosive depending on impurities and presence of water, hydrogen difficult to seal and contain	Generation, distribution, and use of support liquid motor- fuel market	Depends on feedstock, process, and amount of purification needed	16, 58, 59, 64, 84, 100, 111

each of these fuels and identifies gaps in this knowledge. Since many of these fuels are just emerging or considered future options, identification of knowledge gaps could be important in planning future research and development activities. Each of the fuels listed in Table 5 is discussed here in greater detail to highlight possible issues or problems with each of them.

#### 5.4 DIESEL-LIKE FUELS

FAME is used extensively as a diesel supplement due to its similarity to diesel both physically and chemically and due to its ability to be blended with diesel in any combination. Three major issues facing FAME biodiesel distribution are a higher cloud point than diesel, lower stability, and the cleaning effect. The higher cloud point may necessitate the use of heating or insulation along the distribution channels in colder climates to prevent separation from the diesel mixture and to minimize pumping work. Stability can lead to filter plugging issues, especially in cold weather, but can be largely controlled by additives. The cleaning effect, whereby accumulated sediments dissolve into the FAME, increasing the likelihood of filter plugging and injector deposits, necessitates proper washout of pipes and vessels and removal of all residual water and dirt. In addition, batch sequencing in the pipeline becomes an important issue due to the potential of FAME contamination of jet fuel. The polarity resulting from the high oxygen content in FAME can cause it to cling to pipe and vessel walls, making contamination of subsequent batches more likely. These issues have led most large U.S. pipeline operators to expressly prohibit FAME in pipelines. However, as discussed previously, a notable exception to this is Kinder Morgan.

Green diesel's major advantage over FAME is the deoxygenation that occurs during processing, so that green diesel does not display a cleaning effect and should exhibit improved storage stability. It also has a comparable cloud point to diesel, making it compatible with the existing oil pipeline in the opinions of several of its current producers. This potential, coupled with the current lack of extensive research on its compatibility and fungibility, makes green diesel a good candidate for future study.

Similarly, **Fischer-Tropsch (F-T) diesel** has the advantage of being non-oxygenated with a comparable cloud point to diesel. Many of its current producers also claim that it is compatible with the existing oil pipeline, necessitating further research into this fuel. It can be derived from gasified biomass, although most F-T fuel currently manufactured is derived from natural gas or coal.

**Algae-derived FAME**, derived from converting oils or fats extracted from algae to FAME, can be rich in unsaturated fats, leading to oxidation susceptibility. For this reason, algae biodiesel does not currently comply with the biodiesel regulations of the European Union. It also has a higher viscosity than diesel, which could result in additional pumping work to move it through a pipeline. Little information is available, since commercial production is limited and further research is needed.

#### 5.5 GASOLINE-LIKE FUELS

Ethanol is extensively distributed and utilized as a fuel blend component throughout the United States. Its low freezing point makes it suitable for use in cold climates, it can be blended with gasoline in any combination, and it is currently approved as a 10% blend for all vehicles and as an 85% blend for flexfuel vehicles. There are, however, several distribution-related challenges associated with ethanol. It is completely miscible with water and will separate from a gasoline mixture if enough water is present either in the pipeline or as water bottoms in a storage tank. Similarly to FAME, it also displays a cleaning effect, necessitating washout before utilizing ethanol. Additionally, numerous studies have cited ethanol's role in corrosion or stress corrosion cracking of pipeline walls. All of these challenges have led to many major U.S. pipeline operators expressly prohibiting ethanol and ethanol-gasoline mixtures in the pipeline. As discussed previously, Kinder Morgan is allowing the shipment of neat ethanol on one pipeline.

As with ethanol, **butanol** is also an oxygenated fuel that can be blended with gasoline in any combination and requires only minor modifications for use in existing vehicles. This fuel's producers also claim that butanol is compatible with the existing oil pipeline infrastructure, but these claims have yet to be verified. Further research into butanol is warranted. Butanol has four isomers (molecular arrangements), and there is little existing data regarding optimization of these isomers from either a manufacturing or fuel performance standpoint.

Both **green gasoline** and **Fischer-Tropsch gasoline** have thus far been the subject of very little published research. Initial studies indicate that the latter could potentially exhibit physical and chemical properties similar to those of gasoline.

#### 5.6 BIOCRUDES AND REFINERY INTERMEDIATES

**Pyrolysis oil** is a promising biocrude, but there are several significant issues associated with its distribution in and compatibility with the crude pipeline infrastructure. It can have a very high oxygen and water content, which must be removed, it is highly corrosive, and it is chemically unstable due to the high char and solids content. Suspended char particles can also contribute to phase separation. In addition, its alkali metals content can lead to deposits in filters, boilers, etc. and can contribute to catalyst poisoning. The higher viscosity of pyrolysis oil compared to petroleum crude necessitates increased pumping work. The high oxygen content contributes to its polarity, causing pyrolysis oil residue to cling to pipe and vessel walls. It is likely that pyrolysis oil will need some intermediate upgrade step before it can be shipped long distances to an oil refinery for further processing.

**Syngas** derived from biomass is a gas at ambient conditions composed mainly of CO and H<sub>2</sub>. Syngas is normally used as a feed to the manufacture of F-T fuels and can also be used as a fuel to supply heat in refining operations. The hydrogen is also useful for hydrotreating operations, necessary to upgrade fuels and to remove impurities. It would require a distribution infrastructure similar to that required by natural gas if shipped long distances. Syngas can promote corrosion if exposed to water. The hydrogen component is prone to leaks and the carbon monoxide component is highly toxic. This would necessitate additional modifications and maintenance in order to prevent syngas leaks.

One potential hurdle to the future utilization of biocrudes is the RFS2 legislation concerning co-processing. If a biocrude is co-processed with petroleum crude and the resulting mixture is refined to produce a diesel-biodiesel mixture, this fuel will not qualify as a biomass-based diesel fuel. Biomass-based diesel fuels can be blended with petroleum diesel, but they cannot, by RFS2 definition, be the product of co-processing operations. If the appropriate greenhouse gas emissions requirements are met, the resulting fuel would qualify as an advanced biofuel or cellulosic biofuel. This could potentially hinder the flexibility of the biocrude medium, specifically as it pertains to biodiesel production and distribution.

#### 5.7 SHIPPING PYROLYSIS OIL AS CRUDE OIL OR CO-MINGLED WITH CRUDE

Crude oil is gathered from production fields and then consolidated and shipped through a large series of dedicated pipelines in the United States and Canada between production locations, shipping and receiving locations, storage facilities, and petroleum refineries. In this section, we provide a preliminary comparison of crude oil requirements and typical pyrolysis properties and chemistry, with the recommendation that this area of study be revisited next year. Crude oil is shipped as segregated batches, and the concept of fungibility has not been applied to these shipments. No doubt, trading of crude does take place, but controlled by the individual parties involved rather than by commonly accepted fungibility specifications such as those applied to finished petroleum products. Pipeline requirements for crude oil are designed to allow a given system to operate safely, in compliance with various laws, and within its engineering design capabilities.

The information discussed in this section was obtained from the Sunoco Pipeline L.P. website [168], www.sunocologistics.com. Five documents were selected to be representative of typical crude oil shipping requirements: Sunoco Pipeline L.P. Rules and Regulations Governing the Transportation of Crude Petroleum, Texas R.R.C. No. 11 and F.E.R.C. No. 3, Sunoco Pipeline L.P. Local Proportional Pipeline Tariff, Texas R.R.C. No. 11 and F.E.R.C. No. 142, and Sunoco Pipeline L.P. Viscosity Table. These references do not represent universal pipeline requirements for crude oil but are used to provide a comparison between typical crude oil and typical pyrolysis oil.

Crude oil varies greatly worldwide and is mainly described by three properties—density, percent sulfur, and viscosity—with these properties showing only limited correlation to each other. A summary of 98 crudes shown on the Sunoco Pipeline L.P. website indicates density ranging from 0.73 to 0.93 specific gravity or 21 to 61 API gravity (an inverse scale), sulfur ranging from 0.02 to 3.8%, and viscosity ranging from 2.7 to 1541 SUS at 60°F and averaging 163 SUS. Typically, crude with sulfur less than 0.5% is called sweet, and with sulfur greater than 0.5%, sour. Crude with a density of less than 0.87 kg/m³ is called light; 0.87 to 0.92, medium; 0.92 to 1.00, heavy; and greater than 1.00, extra heavy.

Since crude oil is normally shipped in segregated batches, details of properties and chemistry are of interest to the pipeline company only to the extent that they affect operations or other batches of crude being shipped. Crude oil (direct liquid products) can be co-mingled with other products at point of origin or other reception points, such as gas condensate or other hydrocarbons (indirect liquid products), providing that the shipper, consignee, and destination are the same and that material entering the pipeline system meets appropriate specifications and requirements. Specifications for crude and mixtures of crude oil and other products that must be met for material to be accepted for shipment are shown in Table 6. These specifications were set assuming that the majority of materials shipped as crude oil would be, in fact, crude or condensate from natural gas collection wells. As such, they would probably require further definition if something as different as pyrolysis oil was shipped as crude oil or blended with crude oil. As a market develops, requirements will probably be revised and further defined to reflect operating experience and market demand.

A comparison between the crude requirements in Table 6 and the pyrolysis oil properties in the exhibits reveals a large discrepancy between pyrolysis oils and crude oil. Pyrolysis oil is not soluble in hydrocarbons but is soluble in water and alcohols. It contains both large amounts of water and chemically bound oxygen and smaller amounts of nitrogen. It can contain large amounts of carbon and smaller amounts of residual agricultural minerals (sodium, potassium, calcium, magnesium). Pyrolysis oil is denser than crude oil, can have high viscosity, and contains less carbon and hydrogen than crude oil with corresponding lower energy content. The upgrading of pyrolysis oil to match crude requirements for shipment appears to be extensive, and it is unclear if this would be economically and technically feasible. Other options for pyrolysis oil would be to use as fuel for boilers, turbines, or large, slow-speed engines, all of which may be more accepting of lower grade fuels or mixing of lower grade with current grade fuels. Residual metals in the pyrolysis oil (Na, K, Ca, Mg) may also prove difficult to remove and could act as poisons for upgrading catalysts and for emissions control catalysts when upgraded pyrolysis oil is burned as a fuel. The authors of this report recommend further study of the upgrade options for pyrolysis oil and further study of the compatibility of its use as a refinery feed to supplement crude oil.

Table 6. Representative crude requirements for pipeline shipments [168]

Property	Limit per Texas R.R.C. No. 11 and 40	Limit per F.E.R.C. No. 3 and 142
Vapor pressure, petroleum	9 psi summer, 10.7 psi winter @ 100°F	12 psi at 100°F
Vapor pressure, condensate or	11.5 psi summer, 13.7 psi winter at 100°F	12 psi at 100°F
other indirect product		
Proportion of indirect product	<20%	
Vapor pressure	In compliance with all federal, state, and	In compliance with all federal, state,
	local requirements	and local requirements
API gravity	20 to 65	20 to 120
Evaporative loss correction	0.2% for API gravity below 50	
Foreign sediment and water	<2%	<1% with <0.3% water
Contamination	Incrustation of tanks n ot excessive	Incrustation of tanks not excessive
Contamination	Sediment in tanks 4 in. below bottom of	Sediment in tanks 4 in. below bottom
	pipeline connection	of pipeline connection
Contamination	Iron <75 ppm	
Contamination	Lead <0.05 ppm in naphtha fraction	
Contamination	Organic chlorides <5 ppm	
Contamination	Excessive metals, chemicals, salts,	
	refinery or process plant by-product	
Temperature	<120°F	
Viscosity	Additional tariff charged when viscosity	Additional tariff charged when
	exceeds 150 SUS at 100°F, up to 118% of	viscosity exceeds 110 SUS at 60°F,
	base tariff	up to 30% of base tariff
Viscosity	<250 SUS at 100°F	<300 SUS at 60°F, >200 SUS not
		accepted if degrades pipelline
		capacity
Additives	Carrier reserves right to inject or to	Carrier reserves right to inject or to
	approve injection of corrosion inhibitors	approve injection of corrosion
	or drag reducing agens	inhibitors

#### 6. A MARKET FOR BIO-DERIVED HYDROCARBONS

Today's fuels are blended from a number of refinery intermediate streams (about five to seven for gasoline and three to five for distillate fuels). The resulting finished fuels contain a large number of compounds with various molecular weights. Overall, gasoline contains about 300 individual compounds, and distillate fuels, about 2500. The use of multiple processing options and resulting blending streams allows maximum utilization of crude oil and multiple options for blending to allow for refinery optimization. Some molecules are desirable for building required properties or meeting specifications, some are more neutral in effect but expand fuel volumes in a cost-effective manner, and some are undesirable in certain products but may be helpful in others.

With biofuels, it may not be economical to supply the entire range of property and specification requirements of today's petroleum fuels, and it may be more efficient if bio-derived materials are used as blending streams along with petroleum-derived components for fuel blending. Overall, bio-derived blending streams can be utilized via three paths to market: (1)They can be manufactured and used within a specific refinery fuel blending operation. (2) The biofuel blend streams could be transported to a specific refinery or blending site by proprietary or common carrier pipeline or other means such as truck or barge for private sale to an energy company. Finally, (3) certain biofuel blending streams can be sold or traded on the open market.

Platts (www.platts.com), in their *Refiner* newsletter [169], lists pricing for the blendstocks and intermediate refinery components, and their website also lists partial specifications. Prices are shown for April 3, 2009, and change daily (this date was chosen because it happened to be the date of a sample newsletter that could be freely downloaded). These materials are typically traded in volume increments of 50,000 barrels. Table 7 provides specifications, use, and representative pricing for commonly traded blending streams and refinery intermediates. The table shows product information listed in the newsletter. When batches of these products are actually traded, a full analysis is normally required.

The properties of the more highly valued streams could be targeted for biofuel manufacturing and would consist of mixed, longer chain paraffins for distillate blending and aromatics and isoparaffins for gasoline blending.

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Table 7. Commonly traded fuel blending streams and refinery intermediates<sup>a</sup> [169]

Product	Chemistry	Use	Pricing	Sulfur, max	API gravity	RVP (psi)	R+M/2 octane	RON	N+A, min (%)	P, min (%)
Alkylate	C5 to C8 isoparaffins	Gasoline blending	Gasoline + \$0.20	(11)		5.5	92-93		(11)	(13)
Reformate	Mixed aromatic, isoparaffin, and	Gasoline blending	Gasoline + \$0.46	0.5	30-55	0.5-2.5		95-100		
Raffinate	Reformate with BTX removed	Gasoline blending	Gasoline – \$0.08	0.5	60-70	2.0-6.0		55-65		
Xylene	Pure aromatic	Gasoline blending or petrochemical	\$2.10							
Toluene	Pure aromatic	Gasoline blending or petrochemical	\$1.85							
Low sulfur straight run	Mixed paraffinic	Distillate blending or cat cracker feed	\$1.24/gallon	0.3	20-22					
Standard naphtha	Mixed paraffinic	Reforming feed	\$1.25		56-60				40	
Paraffinic naphtha	Mixed paraffinic	Gasoline blending	\$407/mt	500 ppm	65 max	12.5 max				65
Heavy naphtha	Mixed paraffinic	Reforming feed	\$1.25		56	XXII 1 . 1			40	

<sup>&</sup>lt;sup>a</sup> This table shows information listed in Platts' *Refiner* newsletter defining general characteristics of these products. When batches are actually traded, a full analysis is required.

## 7. ENTRY POINTS FOR BIO-DERIVED PRODUCTS INTO FUEL INFRASTRUCTURE

Bio-derived fuels or intermediates could enter the existing refining and distribution infrastructure based on their properties and composition. Table 8 indicates entry points for bio-products of various properties and composition. These possibilities are based on current refining, blending, and distribution practices and would be expected to evolve in the future.

Table 8. Possible entry points for bio-derived materials into petroleum fuel infrastructure

Entry point	Oxygenated feed	Deoxygenated, partially refined feed	Oxygenated blending component	Hydrocarbon blending component	Finished fuel
Refinery feed	Yes, but oxygen may limit feed percentage or require preprocessing	Yes, but must resemble refinery unit feed	NO	NO	NO
Refinery blending operation	NO	Yes, but must be similar to current blend streams	NO	YES	YES
Terminal	NO	NO	Yes, but must meet ethanol or FAME specifications	NO	YES

#### 8. COST ESTIMATES FOR BIO-DERIVED FUELS

Table 9 summarizes the cost data for several biofuels production facilities. More detailed cost information can be found in the exhibits. The table displays examples of biofuel manufacturing plants and shows annual volume of biofuel produced, capital and operating costs, and feedstock cost.

It should be noted that there is a large variation in capital costs, ranging from roughly \$6.6 million for a 4 million gallon/year (MMGPY) FAME facility to \$341 million for a 35 MMGPY F-T diesel facility. Cellulosic ethanol and F-T diesel facilities appear to require significantly larger capital investment than do grain ethanol, FAME, and pyrolysis oil facilities. This may be partially attributable to the fact that the latter three are preexisting technologies that have been studied and iterated extensively, whereas the former two are relatively new and less researched technologies. If examined on a volume basis, the operating costs for all facilities also differ.

Both Table 9 and the exhibits clearly demonstrate that feedstock cost is by far the most significant component of operating costs—for example, amounting to 80% of total operating costs in the FAME facility study. Feedstock costs are also volatile, and small shifts in price can translate into substantial shifts in operating costs for a biofuel producer. This subsection is not intended to provide set price guidelines for building, operating, and maintaining a biofuels production facility but, rather, to provide a relative comparison between the current prices of various biofuels.

Table 9. Summary of capital and operating costs for several biofuels facilities

Product	Volume (million gallons/year)	Volume (barrels/ day)	Capital costs (\$ million)	Yearly operating costs (\$ million)	Feed	Feed costs	Operating + feed costs (\$/gallon)
Pyrolysis oil [94,111,132, 164]	30	1950	48	9.6	Wood chips	\$30 per dry ton	0.32
Ethanol [11,163]	25	1630	27.9	22	Grain		0.88
Ethanol [11,163]	50	3260	294	76	Cellulosic		1.52
Methanol [163]	87	5675	254	56.5	Biomass syngas		0.65
F-T diesel [111,147, 163]	35	2283	341	87.5	Biomass syngas		2.50
FAME [38,69]	4	260	6.6	8	Yellow grease	\$0.17 per lb	2.00
FAME [38,69]	4	260	6.6	12.5	Soy oil	\$0.31 per lb	3.13
FAME [38,69]	10	650	8.8	18	Yellow grease	\$0.17 per lb	1.80
FAME [38,69]	10	650	8.8	29.2	Soy oil	\$0.31 per lb	2.97

Limited cost data analysis references were available, and much of the data is unconfirmed by multiple sources. Specific capital, operating, and feedstock costs are thus associated with specific studies and may not necessarily be applied as general cost guidelines for all biofuels production facilities.

Some of the studies used for cost estimates examine several different types of biofuels facilities, such as one study that examined F-T diesel, ethanol, and pyrolysis oil, and another that examined F-T diesel, ethanol, and methanol. Most, however, specialize in one particular type of biofuel. Each study has a specific set of methods employed in its cost data analysis which result in capital and operating cost conclusions that are not necessarily directly comparable. The operating cost figure in the FAME study, for example, includes profits gained by selling the by-product glycerin at \$0.26 per pound. One of the pyrolysis oil studies applies its analysis for the *n*<sup>th</sup> number facility, as opposed to a pioneer plant, while others are not specific as to which facility is being studied. As was stated earlier, this subsection is not meant to provide price guidelines for building and operating a biofuels production facility but, rather, to provide a relative comparison between the projected prices of biofuels production and how this, along with numerous other factors, might determine the extent of their role in the U.S. biofuels portfolio.

#### 9. CONCLUSIONS AND RECOMMENDATIONS

The expansion and further development of the biofuels industry will require that a number of decisions and investments be made. It is likely that ethanol will remain a major renewable fuel component and will continue to be terminal blended, with manufacturing of ethanol separate from oil refineries and with separate transportation to the blend site. Although EPA no longer requires oxygen in reformulated gasoline for nonattainment areas (*Federal Register*, May 8, 2006 [Vol. 71, No. 88, Rules and Regulations,

pp. 26691–26702]), its use as a renewable fuel component is likely to continue and grow due to existing capacity, familiarity, financial incentives or tax breaks, and requirements of state or federal laws related to pollution reduction, farm support, or renewable content. It is technically possible that ethanol could be refinery blended and shipped over pipelines, but the economic benefits of doing this would depend on where ethanol is manufactured and used, form of transportation available, and pipeline capacity to handle the resulting larger gasoline/ethanol volumes. It would also require continued removal and monitoring of water in the distribution system and further study of the potential issues of ethanol-induced rust, corrosion, or stress corrosion cracking in distribution equipment. Elastomeric gaskets, seals, and piping would also have to be proven or changed to be compatible with ethanol fuels, but this is not expected to be a major roadblock.

Oils, fats, and greases are normally converted to fatty acid methyl esters or FAME, which is the most common form of biodiesel. FAME and FAME blends with diesel fuel are polar and therefore subject to water contamination, can contaminate other fuels shipped after biodiesel, can have a cleaning effect, and can have cold flow, filtration, or long-term stability problems. FAME quality issues were probably more frequent during the development of the industry and start-up of new manufacturing plants and have been largely eliminated with ASTM specifications covering both B100 and blends, with more manufacturing and distribution experience, and with the use of stability and filtration additives. FAME is normally added at a product terminal during truck loading, using on-line rack blending similar to that used for ethanol. This practice keeps the B100 FAME segregated from other products and results in the faster turnover of product. Production of FAME will likely increase in the future, due to the use of palm oil, increased use of waste oils and fats, and because of the algae potential for manufacturing fats and oils from CO<sub>2</sub> and water. There is limited experience with the shipping of FAME biodiesel over pipelines, and it appears to be successful. This experience is with pipelines that do not also ship jet fuel, but there is ongoing work relative to contamination and detection of contamination of jet fuel with FAME which may help support more flexible shipping practices in the future.

Currently, ethanol and FAME are largely manufactured from purpose-grown crops, with starch and sugar plants being used to supply ethanol fermentation and oil plants being used to supply oil and fats for FAME production. An emerging method for biofuel production is from gasified or pyrolyzed biomass on a large scale. Gasification results in CO and H<sub>2</sub>, which can be recombined to liquid hydrocarbons using Fischer-Tropsch processing. Pyrolysis results in a liquid known as pyrolysis oil, which could be considered as a bio-derived crude oil. Unfortunately, such pyrolysis oil is heavily contaminated by residual plant compounds, has a very high oxygen and water content, has a high total acid number and corresponding low pH, and is relatively unstable. This could be an important source of fuel, providing these problems can be overcome economically. Pyrolysis oil could be upgraded in several steps: In the first step, it could be upgraded sufficiently to allow it to be shipped in a manner similar to crude oil; in the second step, it could be upgraded sufficiently to be used as a refinery unit feed; in the third step, it could be refined sufficiently to be used directly as a fuel blending component with petroleum-derived blending streams; and in the fourth step, it could be refined sufficiently to act as a final fuel and direct substitution for diesel fuel or gasoline. The authors speculate that the easiest entry point into existing infrastructure would be to upgrade sufficiently to allow the shipping of pyrolysis oil in a similar manner to crude oil, which would allow entry to the refining, blending, and distribution infrastructure already in use for petroleum-derived fuels. The options for this level of upgrading and the degree of upgrading required are recommended as a topic for additional study.

In addition to producing ethanol by fermentation of sugar, starch, or cellulose, or the conversion of oils and fats to FAME, these materials can also be converted to other hydrocarbon components using catalytic (refining-like) processes. There are many options—some are under current investigation, some may already be in use for fuel manufacturing or for making other industrial chemicals, and some have been discussed but not experimentally investigated. Further study of the processes and information available

about each process is recommended. Overall, the recommendations for further study are summarized in Table 10. These tasks have been used to form a basis for discussions related to continuing this research.

Table 10. Recommendations for further study

Recommendation number	Feed material	Fuel	Recommended areas for future investigation
1	Sugar, starch, cellulose	Ethanol	Study of rust, corrosion, and stress corrosion cracking of mild and low alloy steel by ethanol and ethanol containing fuels and related industrial experience
2	Sugar, starch, cellulose	Ethanol	Study of control and removal of water bottoms from fuel distribution system and related industrial experience
3	Fats, oils	FAME biodiesel	Study of issues associated with shipping FAME biodiesel over common carrier distribution system, including batch sequencing with and possible contamination of jet fuel, and related industrial experience
4	Biomass	Pyrolysis oil	Study of the issues, options, and degree of upgrading required to allow pyrolysis oil to be treated like crude oil for shipping purposes
5	Sugars, starch, oils, fats	Hydrocarbon fuel blending components	Study of the options and current state of knowledge relative to converting biofeeds to fuel compatible hydrocarbons

# 10. REVIEW OF COMMENTS RECEIVED AND SUGGESTED MODIFICATIONS OR ADDITIONS FOR FUTURE STUDY

This report, in draft form, was distributed to four integrated oil companies, two of which provided comments with the understanding that the comments do not represent official company views and would not be attributed to the companies or individuals. DOE also provided guidance and comments relative to priorities for a possible continuation of this research. All of these comments have been combined in this section, without attribution, as possible technical recommendations for future work. We note that many of these recommendations are beyond the scope of the current study and have been or are being addressed in other studies. They are listed here for completeness and to help provide guidance for this and other projects.

- 1. Suggestion was made to de-emphasize study of ethanol-related infrastructure issues, since ethanol has already been and is being heavily studied in other projects. (These are topics 1 and 2 in Table 10.)
- 2. Provide more information or recommendations related to health effects of new biofuels with discussion related to the amount or type information that might be required for EPA approval of these new fuels. (This would be a new addition to Table 10.)
- 3. Extend infrastructure compatibility evaluation to include service stations, current vehicles, and future vehicles. Provide survey of types of materials in current use and industry plans for material changes or upgrading. Provide summary of approvals necessary for fueling equipment. (This would be a new addition to Table 10.)

- 4. Discuss in more detail how oxygen in fuels affects engine operation and infrastructure compatibility. Discuss changes that could mitigate these effects. (This would be a new addition to Table 10.)
- 5. Expand study of pyrolysis oils in the areas of chemistry, properties, and material compatibility. (This is an expansion of topic 4 in Table 10.)
- 6. Topics 3 and 5 in Table 10 should remain as written.
- 7. Review and coordinate research with other labs or companies working on infrastructure-related issues in order to disseminate results, gather information, build synergy, and avoid duplication.

#### 11. REFERENCES

The following list of references was compiled during preparation of the exhibits at the end of this report. The fuel or information about which the reference pertains is given at the end of each reference.

- Acros Organics, "1-Butanol Material Data Safety Sheet," www.acros.com, December 2009 1-Butanol compatibility.
- Adu-Gyamfi, Villa, Coulon, "Renewable Energy, Landfill Gas and EfW: Now, Next and Future," http://www.geotech.co.uk/press\_releases/Geotech%20sponsored%20paper.pdf – Methane partial properties.
- Aguayo, Gayubo, Tarrio, Atutxa, Bilbao, "Study of Operating Variables in the Transformation of Aqueous Ethanol into Hydrocarbons on a HZSM-5 Zeolite," *Journal of Chemical Technology and Biotechnology* 77, 211–216 (2002) Sugars and alcohols information.
- Air Liquide, "1-Propanol MSDS," http://www.scottecatalog.com/msds.nsf/MSDSNo/71-23-8 1-Propanol partial properties.
- Air Products and Chemicals for DOE, *Alternative Fuels and Chemicals from Synthesis Gas, Quarterly Report Jan. 1–Mar. 31, 1998* Glyme information.
- Alasfour, Butanol, "A Single Cylinder Engine Study: Engine Performance," *International Journal of Energy Research* **21**, 21–30 (1997) Butanol partial properties.
- Alleman, McCormick, *Fischer-Tropsch Diesel Fuels—Properties and Exhaust Emissions: A Literature Review*, SAE Technical Paper 2003-01-0763 FT diesel partial properties.
- Alvarado, Peter J., "Steel vs. Plastics: The Competition for Light-Vehicle Fuel Tanks," *JOM* **48**(7), 22–25 (1996) Vehicle materials.
- Amerada Hess Corporation, *Methyl tert-Butyl Ether (MTBE)*, Material Safety Data Sheet No. 9922, April 1998 MTBE partial properties.
- American Chemical Society, Organic Chemistry Division, "Common Organic Solvents—Table of Properties," http://organicdivision.org/organic\_solvents.html Butanol partial properties.
- Anex, Aden, Kazi, Fortman, Swanson, Wright, Satrio, Brown, Daugaard, Platon, Kothandaraman, Hsu, Dutta, "Techno-Economic Comparison of Biomass-to-Transportation Fuels Via Pyrolysis, Gasification, and Biochemical Pathways," accepted to *Fuel* in February 2010 Pyrolysis oil, ethanol, and FT production facility costs.
- Argonne National Laboratory, "Biobutanol Properties," http://www.greencarcongress.com/2008/08/argonne-investi.html Biobutanol partial properties.

- Assael, Polimatidou, "Measurements of the Viscosity of Alcohols in the Temperature Range 290-340 K at Pressures up to 30 Mpa," *International Journal of Thermophysics* **15,** 95–107 (1994) Methanol partial properties.
- Atsumi, S., Hanai, T., Liao, J. C., "Non-fermentative Pathways for Synthesis of Branched-Chain Higher Alcohols as Biofuels," *Nature* **451** (2008), doi:10.1038/nature06450 Higher C alcohols information.
- Avantec Performance Chemicals, www.inventec.dehon.com, December 2009 DME compatibility.
- Bain, Richard, "An Introduction to Biomass Thermochemical Conversion," DOE/NASLUGC Biomass and Solar Energy Workshops, Aug. 3–4, 2004 Syngas partial properties.
- Bechtold, Richard L., *Alternative Fuels Guidebook: Properties, Storage, Dispensing, and Vehicle Facility Modifications*, SAE Order Number R-180, 1997 Gasoline partial properties.
- Bedoukian Research Inc, *(e)-beta-Farnesene*, MSDS P3500-90, http://www.bedoukian.com/products/displayGraphic.asp?type=m&product=P3500-90, Aug. 3, 2007 Sesquiterpene (farnasene) partial properties.
- Bertola, Boulouchos, Oxygenated Fuels for Particulate Emissions Reduction in Heavy-Duty Di-Diesel Engines with Common-Rail Fuel Injection, SAE Technical Paper 2000-01-2885 Diesel and glyme partial properties and compatibility.
- Biofuels Digest, "US Ethanol Production Capacity to Increase to 13.3 Billion Gallons in 2008," www.biofuelsdigest.com, Jan. 9, 2008 US ethanol production and capacity.
- Biofuels Journal, "Annual and Monthly US Ethanol Production," www.biofuelsjournal.com, Dec. 5, 2006 U.S. ethanol production and capacity.
- Blin, Volle, Girard, Bridgwater, Meier, "Biodegradability of biomass pyrolysis oils: Comparison to conventional petroleum fuels and alternatives fuels in current use," *Fuel* **86**, 2679–2686 (2007) Pyrolysis oils environmental/ compatibility.
- Blommel, Cortright, *Production of Conventional Liquid Fuels from Sugars*, White Paper, Virent Energy Systems, Inc., Aug. 25, 2008 Sugars and alcohols information.
- BOC Gases, "MSDS: Hydrogen," www.fergusongases.com, June 7, 1996 Hydrogen compatibility.
- BP, "Biobutanol Fact Sheet," www.bp.com, 2009 Biobutanol compatibility.
- Buckeye Partners LP, www.buckeye.com, December 2009 Pipeline map/shipping information.
- California Air Resources Board Solvents Database, "Butanol," http://www.arb.ca.gov/db/solvents/solvent\_pages/alcohols-html/butanol.htm – Biobutanol partial properties.
- California Air Resources Board, "Solvents Database, 1-propanol," http://www.arb.ca.gov/db/solvents/solvent\_pages/Alcohols-HTML/propanol.htm – 1-propanol partial properties.
- Cameo Chemicals Inc., "Isoprene," www.cameochemicals.noaa.gov, June 1999 Isoprene compatibility.
- Cameo Chemicals, "n-Propanol Chemical Data Sheet," www.cameochemicals.noaa.gov, December 2009 n-propanol compatibility.
- Cardoso, Domingos, Oliveira, Passos, "Chemical Composition and Physical Properties of Black Liquors and Their Effects on Liquor Recovery Operation in Brazilian Pulp Mills," *Fuel* **88**, 756–763 (2009) Lignin liquids partial properties.
- Chao, Rossini, "Heats of Combustion, Formation, and Isomerization of Nineteen Alkanols," *Journal of Chemical Engineering Data* **10,** 374–379 (1965) Propanol and higher C alcohols partial properties.
- Chisti, Yusuf, "Biodiesel from Microalgae," *Biotechnology Advances* **25,** 294–306 (2007) Algae biodiesel compatibility.

- CHOREN Industries, "Biomass-to-Liquid Fuels (BtL)—Made by CHOREN process, Environmental Impact, and Latest Developments," Automobile and Environment at Belgrade EAEC Congress, May 2005 FT diesel compatibility.
- Cirad-Foret, "MSDS: Bio-Oil," May 2006 Pyrolysis oils compatibility.
- CITGO, *No. 2 Diesel, MSDS*, May 2006, http://www.martineagle.com/MSDS/CitgoLowSulfurDiesel.pdf Diesel properties.
- Colonial Pipeline Co., www.colpipe.com, December 2009 Pipeline map/shipping information.
- Coltrain, David, "Biodiesel: Is It Worth Considering?," Risk and Profit Conference, Kansas State University, August 2002 FAME production facility costs.
- Columbia Engineered Rubber, Inc., www.columbiaerd.com, 2010 Vehicle materials information.
- ConocoPhillips Pipeline LP, www.conocophillipspipeline.com, December 2009 Pipeline map/shipping information.
- Diebold, *A Review of the Toxicity of Biomass Pyrolysis Liquids Formed at Low Temperatures*, NREL/TP-430-22739, National Renewable Energy Laboratory, 1997 Pyrolysis oils partial properties.
- Dominguez, Miguel, Arjona, Millan, "The Effects of Ethanol-Diesel Blended Fuels on the Performance and Emissions of Unmodified Diesel Engines," 14th European Biomass Conference and Exhibition: Biomass for Energy, Industry and Climate Protection, Paris, October 2005 Ethanol-Diesel blend partial properties.
- Dow Chemicals, "Dow n-Propanol Product Safety Assessment," www.dow.com, June 18, 2009 n-propanol compatibility.
- Ekbom, T., "High Efficiency Motor Fuel Production from Biomass via Black Liquor Gasification," ISAF XV International Symposium on Alcohol Fuels, September 2005 Lignin liquids compatibility.
- Elliott, Douglas C., Staff Scientist, U.S. Department of Energy, Pacific Northwest National Laboratory, Richland, WA, "Hydroprocessing of Pyrolysis Bio-oil to Fuels and Chemicals," Bioenergy & Wood Products, Smallwood, May 14, 2008 Pyrolysis oils partial properties.
- Enterprise Products Partners LP, www.epplp.com, December 2009 Pipeline map/shipping information.
- EPUK, "Biogas as a Road Transport Fuel, National Society for Clean Air and Environmental Protection," www.environmentalprotection.org/uk, June 2006 Methane partial properties and compatibility.
- European Biofuels Technology Platform, funded by the EC under Grant Agreement 241269, last updated Feb. 23, 2010, http://www.biofuelstp.eu/hydrogen.html
- European Industrial Gases Association, *Carbon Monoxide and Syngas Pipeline Systems*, IGC Doc. 120/04/E Syngas partial properties and compatibility.
- European Project BioDME, "Production of DME from Biomass and Utilization as Fuel for Transport and for Industrial Use," 7th Framework Program, 2009 Syngas compatibility.
- ExxonMobil Chemical, "Isoprene Product Safety Summary," www.exxonmobilchemical.com, June 2009 Isoprene compatibility.
- ExxonMobil Pipeline Co., www.exxonmobilpipeline.com, December 2009 Pipeline map/shipping information.
- Fanick, "Fuel and Fuel Additive Registration Testing of Ethanol-Diesel Blend for O2Diesel, Inc.," National Renewable Energy Laboratory, www.nrel.gov, February 2004 Ethanol-diesel blend partial properties.
- Farrell, Alexander E., and Sperling, Daniel, "A Low-Carbon Fuel Standard for California," August 2007 State policy drivers for increased biofuels usage.
- Ferguson, Straub, Richards, Robey, "Impact of Fuel Variability on Dynamic Instabilities in Gas Turbine Combustion," 5th US Combustion Meeting, organized by the Western States Section of the

- Combustion Institute and hosted by the University of San Diego, Mar. 25–28, 2007. LFG, natural gas, and syngas partial properties.
- Ferro Fine Chemicals, "Product Data Sheet, Diglyme," http://www.d-orland.com/pdf/Diglyme.pdf Glyme partial properties.
- Fisher Scientific, "MSDS, 3-Methyl-1Butanol," Sept. 30, 2002, https://fscimage.fishersci.com/msds/00798.htm – Higher C alcohols partial properties and compatibility.
- Fisher Scientific, "MSDS, DL-2-Methyl-1Butanol, 98%," https://fscimage.fishersci.com/msds/52450.htm, Nov. 20, 2008 Higher C alcohols partial properties and compatibility.
- Fisher, Kein-Marcuschamer, Stephanopoulos, "Selection and Optimization of Microbial Hosts for Biofuels Production," *Metabolic Engineering* **10**, 295–304 (2008) Terpene information.
- Fortenbery, Randall T., "Biodiesel Feasibility Study: An Evaluation of Biodiesel Feasibility in Wisconsin," University of Wisconsin Staff Paper No. 481, March 2005 FAME production facility costs.
- Gautam, Martin, "Combustion Characteristics of Higher Alcohol/Gasoline Blends," *Proceedings of the Institution of Mechanical Engineers; Part A; Journal of Power and Energy* **214,** 497 (2000) Butanol and propanol partial properties.
- Georgia Forestry Commission, "Summary of State Incentives and Legislation for Renewable Energy Production," September 2007 State policy drivers for increased biofuels usage.
- Gillette and Kolpa, "Overview of Interstate Hydrogen Pipeline Systems," Argonne National Laboratory, www.corridoreis.anl.gov, November 2007 Hydrogen compatibility.
- Gurbuz, Kunkes, Simonetti, West, Serrano-Ruiz, Gaertner, Dumesic, "Catalytic Production and Upgrading of Biomass Derived Monofunctional Hydrocarbons," *Proceedings of the American Institute of Chemical Engineers Annual Meeting*, Nashville, TN, November 2009 Sugars and alcohols information.
- Hawkins, Eriksen, "Physical and Thermodynamic Properties of Terpenes. II. The Heats of Combustion of Some Terpene Hydrocarbons," *Journal of the American Chemical Society* **76**, 2669–2671 (1954) Terpene partial properties.
- Hawley's Condensed Chemical Dictionary: 11th Ed., 1987 Methanol compatibility.
- Helwani, Othman, Aziz, Fernando, Kim, "Technologies for Production of Biodiesel Focusing on Green Catalytic Techniques: A Review," *Fuel Processing Technology*, **90**, 1502–1514 (2009) Green diesel information.
- Hess, "Material Data Safety Sheet No. 9909, Diesel Fuel," Oct. 18, 2006, http://www.hess.com/ehs/msds/9909DieselFuelAllTypes.pdf – Diesel partial properties.
- Hess, Boehman, Tijm, Waller, Experimental Studies of the Impact of CETANER on Diesel Combustion and Emissions, SAE Technical Paper 2000-01-2886 Diesel partial properties.
- Hess, Howard, "Effect of Oxygenated Cetane Improver on Diesel Engine Combustion and Emissions," http://www.ems.psu.edu/~boehman/altfuels.html Glyme partial properties.
- Honeywell Burdick and Jackson, "Material Safety Data Sheet," http://www51.honeywell.com/sm/rlss/bandj/common/documents/2.4.67\_msds.pdf - Glyme partial properties.
- Hubbard, C. R., Peascoe, R. A., Keiser, J. R., "Pulp and Paper Plant Materials Issues Addressed by X-Ray and Neutron Diffraction Methods," *International Center for Diffraction Data, Advances in X-Ray Analysis* **46** (2003) Syngas compatibility.

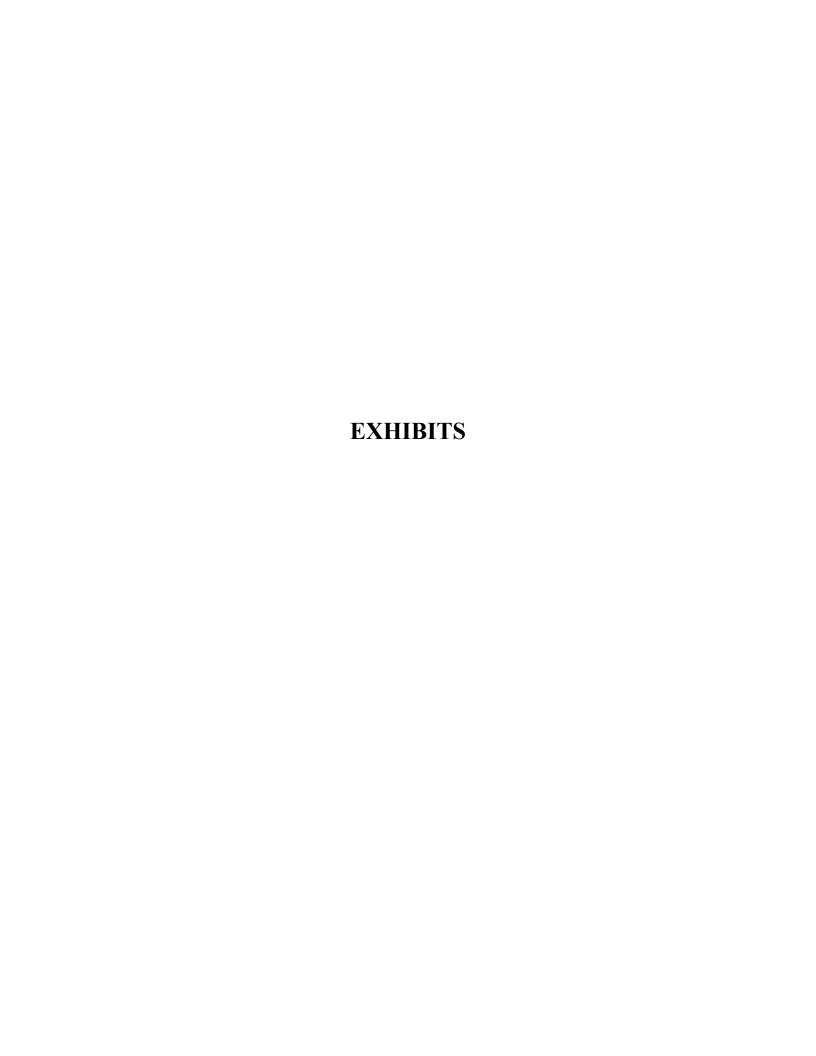
- Institute for the Analysis of Global Security, "Sources of Methanol," www.iags.org, 2004 Methanol production capacity.
- $Intelligent\ Energy\ Europe,\ "Fischer-Tropsch\ Diesel,"\ www.refuel.eu,\ 2010-FT\ diesel\ compatibility.$
- International Program on Chemical Samety, "INCHEM, 1-Propanol,"
  - http://www.inchem.org/documents/ehc/ehc/lo2.htm#SectionNumber:1.3 Propanol partial properties.
- iSOC Technology, "MSDS: Methane," www.isocinfo.com, December 2009 Methane compatibility.
- Jaaskelainen, Hannu, "Biodiesel Fuel Standards," http://www.dieselnet.com/tech/fuel\_biodiesel\_std.html FAME partial properties.
- JT Baker, "MSDS, 1-Propanol," http://www.jtbaker.com/msds/englishhtml/P6390.htm Propanol partial properties.
- JT Baker, "MSDS, Gasoline," Oct. 14, 2008, http://www.docs.citgo.com/msds\_pi/UNLEAD.pdf Gasoline and MTBE partial properties.
- Kalnes, Marker, Shonnard, Koers, "Green Diesel and Biodiesel a Technoeconomic and Life Cycle Comparison," 1st Alternative Fuels Technology Conference, February 2008, Prague, Czechoslovakia Green diesel information.
- Kamara, Coetzee, "Overview of High-Temperature Fischer-Tropsch Gasoline and Diesel Quality," *Energy & Fuels* **23**, 2242–2247 (2009) – FT gasoline partial properties and compatibility and FT diesel compatibility.
- Katikaneni, Sai P. R., Bakhshi, Narendra N., and Huffman, Don, "The New Bio-Crude: A Renewable Substitute for Petroleum?" Energy Conversion and Engineering Conference, August 1996 Pyrolysis oil production facility costs.
- Kinder Morgan, www.kne.com, February 2010 Pipeline map/shipping information.
- Kourtchev et al., *Atmospheric Environment* **43**, 3182 (2009) Sesquiterpene (farnasene) partial properties.
- Kreame, N., Gross, C., "University of Minnesota Biofuels Database, Branched Chain Alcohol Pathway," https://www.biofuelsdatabase.org/wiki/index.php5/Branched-Chain\_Alcohol\_Pathway Higher C alcohols information.
- Kunkes, Simonetti, West, Serrano-Ruiz, Gartner, Dumesic, "Catalytic Conversion of Biomass to Monofunctional Hydrocarbons and Targeted Liquid-Fuel Classes," *Science* **322**, 417–421 (2008) Sugars and alcohols information.
- Lantmänen Ecobränsle AB, Sweden, "MSDS," www.ecobransle.se FAME partial properties.
- LeBlanc, Richard J., "Black Liquor Gasification Can Help Sustain Forests, Generate Ultra-Clean Biofuels," *Biomass Magazine* (July 2009) Syngas compatibility.
- Lindhjem and Pollack, "Impact of Biodiesel Fuels on Air Quality and Human Health: Task 1 Report," National Renewable Energy Laboratory, www.nrel.gov, May 2003 FAME partial properties.
- Magellan Pipeline Company LLC, www.magellanlp.com, December 2009 Pipeline map/shipping information.
- Mariano, Tomasella, Martino, Filho, Seleghim, Contiero, deFranceschi de Angeles, "Aerobic Biodegradation of Butanol and Gasoline Blends," *Biomass and Bioenergy* **33**, 1175-1181 (2009) Biobutanol partial properties.
- McElroy, Anduin Kirkbride, "Pipeline Potential," *Biodiesel Magazine* (February 2007) Petroleum fuel distribution chain information.
- Merck Index, 11th Edition, 3148 Glyme partial properties.
- Methanex, "MSDS, Methanol," http://www.methanex.com/products/documents/MSDS\_USenglish.pdf, Oct. 13, 2005 Methanol partial properties.

- Methanex, "Technical Information and Safe Handling Guide for Methanol: Version 3.0," September 2006 Methanol compatibility.
- Miao, Wu, "Biodiesel Production from Heterotrophic Microalgal Oil," *Bioresource Technology* **97,** 841–846 (2006) Algae biodiesel compatibility.
- Miltner, Makaruk, Bala, Harasek, "Biogas upgrading for transportation purposes Operational Experiences with Austria's first Bio-CNG fuelling station," Chem. Eng. Trans. (2009), http://www.aidic.it/pres09/webpapers/134Miltner.pdf Methane information.
- Mueller, Stefan, "Assessing the Climate Change Impact of Biofuels," BioCycle Conference on Renewable Energy from Organics Recycling, October 2007 Federal policy drivers for increased biofuels usage.
- NACS Online, http://www.nacsonline.com/NACS/News/Daily/Pages/ND0917097.aspx Hydrogen information.
- National Biodiesel Board, "Materials Compatibility," www.biodiesel.org, 2004 FAME compatibility.
- National Biodiesel Board, "NBB Member Plant Locations," www.biodiesel.org, Sept. 23, 2010.
- National Biodiesel Board, "US Biodiesel Production Capacity," www.biodiesel.org, June 22, 2009 FAME production capacity.
- National Institutes of Health, "Substance Profiles: Isoprene," www.ntp.niehs.nih.gov, 2000 Isoprene compatibility.
- National Renewable Energy Laboratory, *Biodiesel Handling and Use Guide: 4th Edition*, Revised January 2009 FAME compatibility.
- National Renewable Energy Laboratory, http://www.nrel.gov/hydrogen/proj\_production\_delivery.html#water – Hydrogen information.
- Netse Oil, "Press Release, June 18, 2008," www.nesteoil.com Green diesel compatibility.
- Ng, Biruduganti, Stork, *Comparing the Performance of SunDiesel and Conventional Diesel in a Light-Duty Vehicle and Heavy-Duty Engine*, SAE Technical Paper 2005-01-3776 FT diesel partial properties.
- NIST, "Chemistry WebBook," http://webbook.nist.gov/cgi/cbook.cgi?Name=farnesene&Units=SI Sesquiterpene (farnasene) partial properties.
- NuStar Logistics LP, www.nustarenergy.com, December 2009 Pipeline map/shipping information.
- Oasmaa, Peacocke, Gust, Meier, McLellan, "Norms and Standards for Pyrolysis Liquids. End-User Requirements and Specifications," *Energy and Fuels C*, http://www.combioproject.com/download/PDF/COMBIO\_WP2\_specification.pdf Pyrolysis oils partial properties.
- Oil & Gas Journal, "Special Report: Natural Gas Pipeline Profits Surge; Oil Flat," Sept. 1, 2008 Pipeline map/daily production information.
- Pacific Northwest National Laboratory, Hydrogen Analysis Resource Center: Lower and Higher Heating Values of Hydrogen and Fuels,
  - $http://hydrogen.pnl.gov/filedownloads/hydrogen/datasheets/lower\_and\_higher\_heating\_values.xls-Butanol\ partial\ properties.$
- Paisley, Farris, Black, Irving, Overend, *Preliminary Operating Results from the Battelle/FERCO Gasification Demonstration Plant in Burlington, Vermont, U.S.A.*, http://www.silvagas.com/downloads/seville.pdf Syngas partial properties.
- PDM, Inc., "MSDS d-Limonene," http://www.pdmchemicals.com/MSDS/MSDS-d-Limonene.doc Terpene partial properties.
- Pipeline Research Council International, "Stress Corrosion Cracking," July 2006 Ethanol corrosion.
- Plains All-American Pipeline LP, www.paalp.com, December 2009 Pipeline map/shipping information.

- Praxair, "Dimethyl Ether MSDS," www.praxair.com, Oct. 15, 2007 DME partial properties.
- Problem Solving Products Inc., www.pspglobal.com, December 2009 DME compatibility
- Purushothaman, Nagarajan, "Experimental Investigation on a C.I. Engine Using Orange Oil and Orange Oil with DEE," *Fuel* **88**, 1732–1740 (2009) Terpene information.
- Qiang, Lu, Wen-Zhi, Li, Xi-Feng, Zhu, "Overview of Fuel Properties of Biomass Fast Pyrolysis Oils," Journal of Energy Conversion and Management **50** (2009) – Pyrolysis oils partial properties and compatibility.
- Rantanen, Linnaila, *NExBTL—Biodiesel Fuel of the Second Generation*, SAE Technical Paper 2005-01-3771, 2005 Green diesel partial properties and compatibility.
- *Refiner*, a daily newsletter from www.platts.com, providing information on news, pricing, and analysis for the refining market.
- Ren, Huang, Miao, Jiang, Liu, Wang, "Effect of the Addition of Diglyme in Diesel Fuel on Combustion and Emissions in a Compression-Ignition Engine," *Energy and Fuels* **21,** 2573–2583 (2007) Methanol partial properties and glyme compatibility.
- Renewable Fuels Association, 2010 Ethanol Industry Outlook, Climate of Opportunity, February 2010. Available from www.ethanolrfa.org.
- Ringer, M., Putsche, V., and Scahill, J., *Large Scale Pyrolysis Oil Production: A Technology Assessment and Economic Analysis*, NREL Technical Report TP-510-37779, November 2006 Pyrolysis oil production facility costs.
- Rude, Schirmer, "New Microbial Fuels: A Biotech Perspective," *Current Opinion in Microbiology* **12**, 274–281 (2009) Sesquiterpene (farnasene) partial properties.
- Sax and Lewis, Dangerous Properties of Industrial Materials: 9th Ed., 1995 Methanol compatibility.
- Science Lab, "MSDS, 1-Butanol," http://www.sciencelab.com/xMSDS-1\_Butanol-9927115, Nov. 6, 2008 Biobutanol partial properties.
- Science Lab, "MSDS, d-Limonene," Nov. 6, 2008, http://www.sciencelab.com/xMSDS-DLimonene-9924496 Terpene partial properties.
- Sevon, Cooper, "Modeling Combustion Efficiency in a Circulating Fluid Bed Liquid Incinerator," *Chemical Engineering Science* **46**, 2983–2996 (1991) Propanol partial properties.
- Sharkey, "The Future of Isoprene Research," *Bulletin of the Georgian National Academy of Sciences* **3**(3) (2009) Isoprene partial properties.
- Sharp, Christopher A., *Emissions and Lubricity Evaluation of Rapeseed Derived Biodiesel Fuels*, SwRI 7507, Southwest Research Institute, November 1996 FAME partial properties.
- Shihadeh, Hochgreb, *Energy and Fuels* **16**, 552–561 (2002) Pyrolysis oils partial properties.
- Sigma-Aldrich, "MSDS, Product Number W383902" Sesquiterpene (farnasene) partial properties.
- Snare, Maki-Arvela, Simakova, Myllyoja, Murzin, "Overview of Catalytic Methods for Production of Next Generation Biodiesel from Natural Oils and Fats," *Russian Journal of Physical Chemistry B* **3**, 3–17 (2009) Green diesel information.
- Spectrum Chemical, "Fact Sheet," http://www.speclab.com/compound/c64175.htm Diesel and ethanol partial properties.
- Stull, D. R., "Vapor Pressure of Pure Substances Organic Compounds," *Ind. Eng. Chem.* **39,** 517–540 (1947) Glyme partial properties.
- Sunoco Pipeline Co., www.sunocologistics.com, December 2009. Five documents were selected to be representative of typical crude oil shipping requirements: Sunoco Pipeline L.P. Rules and Regulations Governing the Transportation of Crude Petroleum, Texas R.R.C. No. 11 and F.E.R.C. No. 3, Sunoco Pipeline L.P. Local Proportional Pipeline Tarriff, Texas R.R.C. No. 11 and F.E.R.C. No. 142, and Sunoco Pipeline L.P. Viscosity Table. Pipeline map/shipping information.

- Sunsoil Inc., "Poultry Fat, B100," Midwest Laboratories Report Number 09-334-2203, Nov. 30, 2009 Poultry fat-derived biodiesel properties.
- Swanson, Satrio, Brown, Platon, "Techno-Economic Analysis of Biomass-to-Liquids Production Based on Gasification Scenarios," accepted to *Fuel* in February 2010 FT production facility costs.
- T2 Laboratories Inc., "Information Bulletin: Material Compatibility with Terpene Chemicals," www.t2labs.com, 1995 Terpene compatibility.
- TEPPCO Partners LP, www.teppco.com, December 2009 Pipeline map/shipping information.
- The Good Scents Company, http://www.thegoodscentscompany.com/data/rw1044061.html Sesquiterpene (farnasene) partial properties.
- Transport 4: Petroleum Logistics Solutions, www.transport4.com, December 2009 Pipeline map information.
- Union Gas Limited, "Chemical Composition of Natural Gas," http://www.uniongas.com/aboutus/aboutng/composition.asp, February 2010 – Natural gas partial properties.
- University of California, *Low Carbon Fuel Standard—Final Report 1*, http://www.energy.ca.gov/low\_carbon\_fuel\_standard/UC\_LCFS\_study\_Part\_1-FINAL.pdf – Butanol partial properties.
- UOP, "UOP/Eni Ecofining Process for Green Diesel Fuel," www.uop.com, 2007 Green diesel compatibility.
- U.S. Department of Energy, DOE Fuel Cell Technologies Program Hydrogen information.
- U.S. Department of Energy, "Handbook for Handling, Storing, and Dispensing E85," July 2006 Ethanol compatibility.
- U.S. Department of Energy, Office of Energy Efficiency and Renewable Energy, http://www1.eere.energy.gov/hydrogenandfuelcells/storage/hydro\_storage.html Hydrogen information.
- U.S. Department of Energy and North Carolina Solar Center, "Database of State Incentives for Renewables & Efficiency," www.dsireusa.org, 2009 State policy drivers for increased biofuels usage.
- U.S. Department of Transportation, "Title 49, Subtitle B, Chapter 1, Subchapter C—Hazardous Materials Regulations," www.goaccess.gov, Dec. 8, 2009 DOT Hazmat Transport Regulations.
- U.S. Energy Information Administration, "Biofuels in the U.S. Transportation Sector," February 2007 Federal policy drivers for increased biofuels usage.
- US EPA (Environmental Protection Agency), "Chemical Fact Sheet," http://www.epa.gov/opptintr/chemfact/s\_mtbe.txt - MTBE partial properties.
- US EPA, "Diglyme robust summary," EPA 201-15023, http://www.epa.gov/hpv/pubs/summaries/diglyme/c15023rs.pdf – Glyme partial properties.
- US EPA, "High Production Volume Information System, Butanol Detailed Chemical Results," http://iaspub.epa.gov/oppthpv/quicksearch.display?pChem=101066 Butanol partial properties.
- US EPA, "High Production Volume Information System, DME Detailed Chemical Results," http://iaspub.epa.gov/oppthpv/quicksearch.display?pChem=100157 DME partial properties.
- US EPA, "High Production Volume Information System, Ethanol Detailed Chemical Results," http://iaspub.epa.gov/oppthpv/quicksearch.display?pChem=100220 Ethanol partial properties.
- US EPA, "High Production Volume Information System, Methanol Detailed Chemical Results," http://iaspub.epa.gov/oppthpv/quicksearch.display?pChem=100296 – Methanol partial properties.

- US EPA, "Methodology for Deriving Ambient Water Quality Criteria for the Protection of Human Health," 2000, http://www.epa.gov/waterscience/criteria/humanhealth/method/tsdvol2.pdf Glyme environmental/partial properties.
- US EPA, "RFS2," www.epa.gov, January 2009 Federal policy drivers for increased biofuels usage.
- US EPA, "Summary of Workshop on Biodegradation of MTBE," February 2001, http://www.epa.gov/nrmrl/pubs/625r01001/625r01001.pdf MTBE partial properties.
- Wackett, L. P., "Biofuels (Butanol-Ethanol Production)," p. 2805 in *Handbook of Hydrocarbon and Lipid Microbiology*, Editor: K. N. Timmis, Springer, 2010 Higher C alcohols information.
- Wallace, W. J.; Mathews, A. L., "Density, Refractive Indices, Molar Refractions, and Viscosities of Diethylene Glycol Dimethyl Ether-Water Solutions at 25°C," *J. Chem. Eng. Data* **9,** 267–268 (1964) DME partial properties.
- Williams Energy Partners LP, "E Grade DN Fuel Ethanol Specifications," April 2003 Pipeline map/shipping information.
- Wright, Mark M., and Brown, Robert C., "Comparative Economics of Biorefineries Based on the Biochemical and Thermochemical Platforms," Center for Sustainable Environmental Technologies Iowa State University, *Biofuels, Bioproducts, and Biorefining* 1, 49–56 (2007) Ethanol, methanol, hydrogen, and FT production facility costs.
- Wright, Satrio, Brown, Daugaard, "Techno-Economic Analysis of Biomass Fast Pyrolysis to Transportation Fuels," accepted to *Fuel* in February 2010 Pyrolysis oil production facility costs.
- www.pipeline101, a public information website maintained by American Petroleum Institute (API) and Association of Oil Pipe Lines (AOPL).
- Xu, Miao, Wu, "High Quality Biodiesel Production from a Microalga Chlorella Protothecoides by Heterotrophic Growth Fermenters," *J. Biotechnol.* **126,** 499–507 (2006) Green diesel partial properties.
- Yacobucci, Brent D., *Biofuels Incentives: A Summary of Federal Programs*, Congressional Research Service Report for Congress, July 29, 2008 Federal policy drivers for increased biofuels usage.



# Oil Pipelines E.1. Products of the Largest U.S. Interstate Oil Pipeline Companies

Largest U.S. Interstate Oil Pipeline Companies	Ethanol	Biodiesel	Butane	Iso-Butane	Ethane	Demethanized NGI	L Propan	e Propyle	ne crude	Unleaded Gasoli	ine Gasoline Blendsto	ck Jet Fuel	Diesel	Kerosene	Natural Gasoline	e Fuel Oil	Biodiesel Fuel Oil
Magellan Plains All-American	E grade DN*	prohibited#, freeze/cloud point resitrictions	H grade	I grade	no	no	L grade	no	no yes	yes*	yes*	yes	yes	no	W grade	Y grade	ZB grade
ConocoPhillips	prohibited^	freeze/cloud point restrictions	dedicated lin	ne dedicated lin	ne dedicated li	ine dedicated line	dedicat	ed I dedicate	dlyes	yes*^		yes	yes	no	no	yes	no
Colonial	prohibited^	prohibited	no	no	no	no	no	no		yes*^	yes*	no	yes	Grade 51, 53-5	57	yes	no
Sunoco	prohibited	prohibited	yes	no	no	no	no	no	yes	yes*	yes*	yes	yes	yes	no	yes	no
Enterprise	yes"	freeze/cloud point restrictions	yes	yes	yes	dedicated line	yes	yes	yes	yes*		yes	yes		yes		
ExxonMobil	prohibited^		dedicated lin	ne dedicated lin	ne dedicated li	ine	dedicat	ed I dedicate	dlyes	yes^					dedicated line		
NuStar Logistics			yes			yes	yes		yes	yes	yes	yes	yes				
Buckeye Partners	prohibited^	prohibited	yes			yes	yes			yes*^	yes	yes	yes	yes		yes	no
Kinder Morgan	dedicated lines	A alloweds								vee*∆	voe*	VOC	voe				

Notes:

\*oxygen content restrictions
\*Autombols and ethers prohibited as blending components in gasoline at origin
\*Corocalor inhibitor required, max 1.00 voffs waits
\*Autombols and ethers prohibitor required, max 1.00 voffs waits
\*Autombols of the second of the

E grade ethanol specs include:

1) min 98 vol% ethanol content

2) only allowable denaturants are unleaded gasoline and natural gasoline 3) 0.5 mass% water max

references:

Buckeye Partners LP, www.buckeye.com, 12/09
Colonial Pipelline Co., www.colpipe.com, 12/09
Conco-Phillips Pipeline LP, www.colpipe.com, 12/09
Enterprise Products Partners LP, www.epip.com, 12/09
ExxonMobil Pipeline Co., www.exormorbilipspileine.com, 12/09
Magellan Pipeline Company LLC, www.magellanp.com, 12/09
NuStar Logistics LP, www.nustarenergy.com, 12/09
NuStar Logistics LP, www.nustarenergy.com, 12/09
NuStar Logistics LP, www.nustarenergy.com, 12/09
Sunco Pipeline CP, www.pasip.com, 12/09
Plains All-American Pipeline LP, www.pasip.com, 12/09
TEPPCO Partners LP, www.teppco.com, 12/09
TEPPCO Partners LP, www.teppco.com, 12/09
Nilliams Energy Partners LP, E grade DN fuel ethanol specifications, 4/2003
Kinder Morgan, www.kne.com, 2/10

# **Oil Piplines**

Notes:

# E.2. Pipeline Descriptions of the Largest U.S. Interstate Oil Pipeline Companies

Largest U.S. Interstate Oil Pipeline Cos.	Mileage*	Pipelines	Location
Magellan	9500 refined/1100 ammonia	refined, ammonia	Pipeline in midwest, from Texas to Wisonsin, with inland terminals in the southeast and marine terminals in the gulf
Plains All-American	8387*, 3 mil bpd	refined, crude, LPG, 3rd party	Pipeline from midwest to western Canada, with crude/refined/LPG/natural gas storage facilities across US
ConocoPhillips	11000	refined, crude, LPG	Pipeline from Texas to northwest and Chicago, with product terminals across US
Colonial	5591*, 2.3 mil bpd	refined	Pipeline from gulf to northeast
Sunoco	2200 refined/3350 crude	refined, crude	Pipeline from Texas to Chicago and northeast/Philadelphia metro area, with additional crude pipeline in northwest
Enterprise	48000	refined, crude, natural gas, NGL, petrochemicals	Pipeline partners from gulf up through midwest, northwest, and northeast, with some pipeline in southeast
ExxonMobil	4559*	refined, crude, LPG, NGL, petrochemicals	Pipeline from gulf to Michigan, northeast, southeast, southwest and California, with trans-Alaskan pipeline
NuStar Logistics	8147, 824K bpd	refined, crude, ammonia	Pipeline from gulf to Texas and midwest, terminals and storage facilities across country
Buckeye Partners	5400	refined, LPG, NGL, petrochemicals	Pipeline network from Chicago to Philadelphia metro areas, with smaller pipelines in Florida, Texas, and midwest
Kinder Morgan	8000+, 2 mil bpd	refined, NGL	Pipeline network in Southeast, Southwest and California, NGL pipeline in Great Lakes region north through Canada

references: Buckeye Partners, www.buckeye.com, 12/09

Colonial Pipeline Co., www.colpipe.com, 12/09

ConocoPhillips Pipeline LP, www.conocophillipspipeline.com, 12/09 Enterprise Products Partners LP, www.epplp.com, 12/09 ExxonMobil Pipeline Co., www.exxonmobilipipeline.com, 12/09 Magellan Pipeline Company LLC, www.magellanlp.com, 12/09

all other mileage and daily production data from company websites 12/4/2009

NuStar Logistics LP, www.nustarenergy.com, 12/09

Oil & Gas Journal, "Special Report: Natural Gas Pipeline Profits Surge; Oil Flat", 9/1/2008

\*2007 mileage from "Special Report: Natural Gas Pipeline Profits Surge; Oil Flat", Oil & Gas Journal, 9/1/2008,

Plains All-American Pipeline LP, www.paalp.com, 12/09 Sunoco Pipeline Co., www.sunocologistics.com, 12/09 TEPPCO Partners LP, www.teppco.com, 12/09

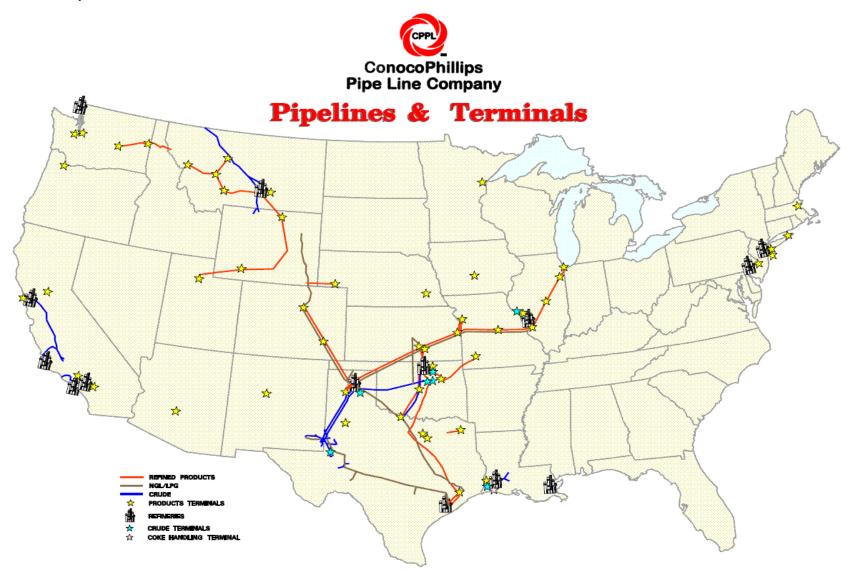
Transport 4: Petroleum Logistics Solutions, www.transport4.com, 12/09

Kinder Morgan, www.kne.com, 2/10

# **Oil Pipelines**

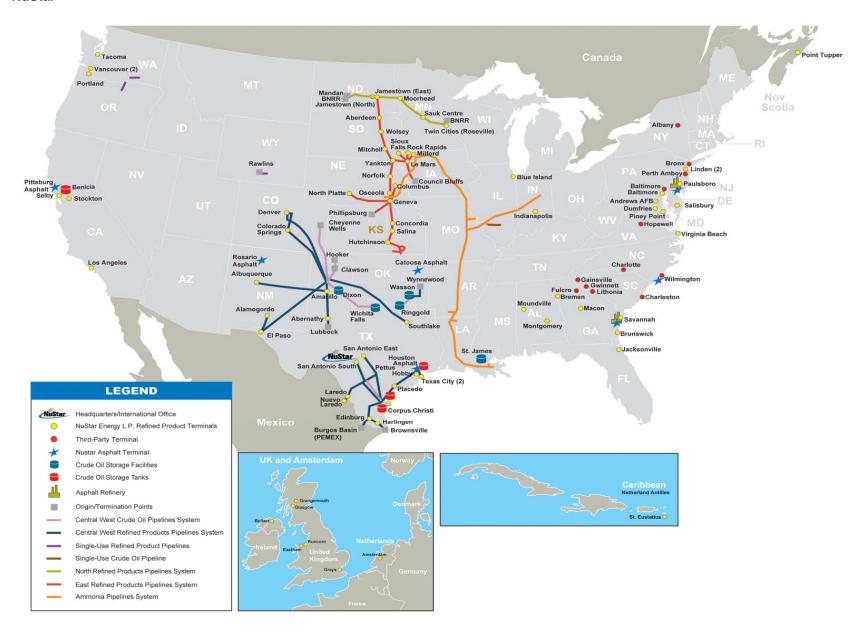
E.3. Maps of the Pipelines and Terminals of the Largest U.S. Interstate Oil Pipeline Companies

# ConocoPhillips



# **Oil Pipelines**

# E.3. Maps of the Pipelines and Terminals of the Largest U.S. Interstate Oil Pipeline Companies NuStar



# Oil Pipelines

E.3. Maps of the Pipelines and Terminals of the Largest U.S. Interstate Oil Pipeline Companies



Oil Pipelines							
E.3. Maps of the Pipelines and Terminals of the Largest U.S. Interstate Oil Pipeline Companies							
references:	Buckeye Partners, www.buckeye.com, 12/09 ConocoPhillips Pipeline LP, www.conocophillipspipeline.com, 12/09 NuStar Logistics LP, www.nustarenergy.com, 12/09						

Hazardous Materials Transport E.4. Transportation Options for Hazardous Fuels

Hazardous materials descriptions and proper shipping		Quantity lin				
names -	Hazard Class	Passenger aircraft/rail	Cargo aircraft only	Rail	Vessel	Public Highway
Butanols	3	60 L	220 L	private track	yes	yes
Coal gas, compressed Coal tar distillates,	2.3	Forbidden	Forbidden	yes private	yes	yes
flammable	3	60 L	220 L	track private	yes	yes
Diesel fuel	3	60 L	220 L	track	yes	yes
Dimethyl ether	2.1	Forbidden	150 kg	yes private	on-deck only	yes
Esters, n.o.s. Ethanol and gasoline	3	60 L	220 L	track	yes	yes
mixture or Ethanol and motor spirit mixture or Ethanol and petrol mixture, with more than 10%				private		
ethanol	3	5 L	60 L	track	yes	yes
Ethanol <i>or</i> Ethyl alcohol <i>or</i> Ethanol solutions <i>or</i> Ethyl alcohol solutions	3	60 L	220 L	private track	yes	yes
Gasohol gasoline mixed with ethyl alcohol, with not more than 10% alcohol	3	5 L	60 L	private track	yes	yes
Gasoline includes gasoline mixed with ethyl alcohol, with not more than 10%	ÿ	3.1	33 L	private	, 50	, 30
alcohol	3	5 L	60 L	track	yes	yes
Hydrocarbons, liquid, n.o.s.	3	60 L	220 L	private track	yes	yes

Hazardous materials descriptions and proper shipping		Quantity lin	nitations			
names -	Hazard Class	Passenger aircraft/rail	Cargo aircraft only	Rail	Vessel	Public Highway
Hydrogen,					on-deck	
compressed	2.1	Forbidden	150 kg	yes	only	no tunnels
Isobutane see also						
Petroleum gases,					on-deck	
liquefied	2.1	Forbidden	150 kg	yes	only	yes
Isobutanol or Isobutyl				private		
alcohol	3	60 L	220 L	track	yes	yes
				private		
Isoprene, stabilized	3	1 L	30 L	track	yes	yes
				private		
Kerosene	3	60 L	220 L	track	yes	yes
Methane, compressed or Natural gas, compressed (with						
high methane					on-deck	
content)	2.1	Forbidden	150 kg	yes	only	yes
Methane, refrigerated liquid (cryogenic liquid) or Natural gas, refrigerated liquid (cryogenic liquid),				,,,,		7.5
with high methane					on-deck	
content)	2.1	Forbidden	Forbidden	yes	only	no tunnels
				private		
Methanol	3	1 L	60 L	track	yes	yes
				private		
Petroleum crude oil	3	60 L	220 L	track	yes	yes
Petroleum distillates,						
n.o.s. or Petroleum				private		
products, n.o.s.	3	60 L	220 L	track	yes	yes
Petroleum gases, liquefied or Liquefied					on-deck	
petroleum gas	2.1	Forbidden	150 kg	yes	only	yes

Hazardous Materials Transport E.4. Transportation Options for Hazardous Fuels

Hazardous materials descriptions and proper shipping		Quantity lin	nitations			
names	Hazard Class	Passenger aircraft/rail	Cargo aircraft only	Rail	Vessel	Public Highway
				private		
Petroleum oil	3	60 L	220 L	track	yes	yes
Propane see also						
Petroleum gases,					on-deck	
liquefied	2.1	Forbidden	150 kg	yes	only	yes
n-Propanol or Propyl				private		
alcohol, normal	3	60 L	220 L	track	yes	yes
				private		
Shale oil	3	60 L	220 L	track	yes	yes
Terpene	_			private		
hydrocarbons, n.o.s.	3	60 L	220 L	track	yes	yes

Hazard Class: 2.1 - flammable gas

2.3 - poisonous gas

3 - flammable and combustible liquid

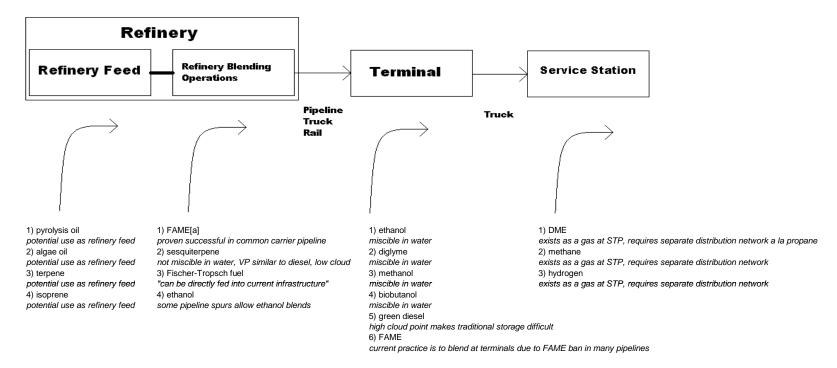
Department of Transportation, "Title 49, Subtitle B, Chapter 1, references:

Subchapter C - Hazardous Materials Regulations", www.goaccess.gov, 12/8/09

## **Distribution Chain**

# E.5. Inserting Biofuels into the Current Distribution Chain

#### Inserting biofuels into the current distribution chain



#### Notes:

High barrier for gaseous fuels due to current refinery-terminal-service station system's accommodation of liquid fuels only. Gaseous fuels necessitate separate distribution network, such as the one currently in place for propane.

Limited studies concerning entering FAME and ethanol in current oil pipelines. In addition, FAME and ethanol are currently expressly banned in most pipelines.

references: please see individual fuel property and compatibility worksheets for appropriate references [a] McElroy, Anduin Kirkbride, "Pipeline Potential", Biodiesel Magazine, 2/2007

E.6. Projected Capital and Operating Costs for FAME, Pyrolysis Oil, Ethanol, Methanol, Hydrogen, and Fischer-Tropsch

#### **Projected Capital and Operating Costs:**

#### FAME

Capital costs for 4 million gal/yr (260 bpd) facility: \$6,627,540.00 Capital costs for 10 million gal/yr (650 bpd) facility: \$8,820,760.00

Operating costs for 4 million gal/yr facility using yellow grease feedstock: \$8,042,396.00 Operating costs for 4 million gal/yr facility using soybean oil feedstock: \$12,502,396.00

Operating costs for 10 million gal/yr facility using yellow grease feedstock: \$18,041,034.00 Operating costs for 10 million gal/yr facility using soybean oil feedstock: \$29,191,034.00

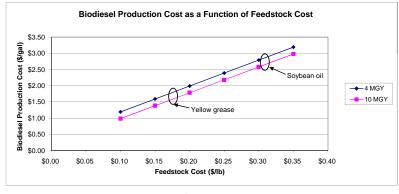
#### Notes:

Operating costs include gains made by selling by-products, including glycerin priced at \$0.26 per lb

Study assumes feedstock costs per lb. are \$0.17 for yellow grease and \$0.31 for soybean oil

Feedstock is approximately 80% of total operating cost

Feedstock cost (\$/lb)	Biodiesel pr	oduction cost (\$/g	gal
	4 MGY	10 MGY	
\$0.10	\$1.19	\$0.98	
\$0.15	\$1.59	\$1.38	
\$0.20	\$1.99	\$1.78	
\$0.25	\$2.39	\$2.18	
\$0.30	\$2.79	\$2.58	
\$0.35	\$3.19	\$2.98	



references: Fortenbery, Randall T., "Biodiesel Feasibility Study: An Evaluation of Biodiesel Feasibility in Wisconsin", University of Wisconsin Staff Paper No. 481, 3/2005 Coltrain, David, "Biodiesel: Is It Worth Considering?", Risk and Profit Conference, Kansas State University, 8/2002

# E.6. Projected Capital and Operating Costs for FAME, Pyrolysis Oil, Ethanol, Methanol, Hydrogen, and Fischer-Tropsch

Pyrolysis Oil Capital costs: \$48,291,646.00
Operating costs: \$9,600,000.00
Notes: Facility uses fast pyrolysis process
Facility produces 16,091 kg/hr of bio-crude (on the order of 30 million gal/yr, 1950 bpd)[a]
Assumes wood chip feedstock price of \$30/dry ton
Operating costs include annual revenue of \$210,000.00 due to annual net electricity export of 4.7 MM kWh
references: Ringer, M., Putsche, V., and Scahill, J., "Large Scale Pyrolysis Oil Production: A Technology Assessment and Economic Analysis", NREL Technical Report TP-510-37779, 11/2006 [a] Katikaneni, Sai P. R., Bakhshi, Narendra N., and Huffman, Don, "The New Bio-Crude: A Renewable Substitute for Petroleum?", Energy Conversion and Engineering Conference, 8/1996
Capital costs: \$200-280 million
Product Value (PV): \$2 - \$3 per gallon gasoline equivalent (GGE)
Notes: Analysis for nth facility
PV = production cost of fuel, including 10% return on investments
Corn stover feedstock cost = \$75 per short ton
Feedstock capacity = 2000 dry tonne (Mg) stover per day
Process involves production of pyrolysis oil and then hydroprocessing to diesel/gasoline-range fuel
Equipment, chemical, and labor prices in 2007 dollars
references: Anex, Aden, Kazi, Fortman, Swanson, Wright, Satrio, Brown, Daugaard, Platon, Kothandaraman, Hsu, Dutta, "Techno-Economic Comparison of Biomass-to-Transportation Fuels Via Pyrolysis, Gasification, and Biochemical Pathways", accepted to Fuel 2/10
Capital costs: \$200-287 million
Product Value (PV): \$2.11 - \$3.09 per gallon gasoline equivalent (GGE)
Notes: Analysis for nth facility
PV = production cost of fuel, including 10% return on investments

Equipment, chemical, and labor prices in 2007 dollars

Corn stover feedstock cost = \$75 per short ton

Feedstock capacity = 2000 dry tonne (Mg) stover per day

Production = 134 - 220 million L/year

references: Wright, Satrio, Brown, Daugaard, "Techno-Economic Analysis of Biomass Fast Pyrolysis to Transportation Fuels", accepted to Fuel 2/10

E.6. Projected Capital and Operating Costs for FAME, Pyrolysis Oil, Ethanol, Methanol, Hydrogen, and Fischer-Tropsch

#### Ethanol

Capital costs for 25 MMGPY (1630 bpd) grain ethanol facility: \$27,900,000.00

Capital costs for 50 MMGPY (3260 bpd) cellulosic ethanol facility: \$294,000,000.00

Operating costs for 25 MMGPY grain ethanol facility: \$22,000,000.00

Operating costs for 50 MMGPY cellulosic ethanol facility: \$76,000,000.00

Notes:

25 MMGPY grain ethanol in 1999 prices, 50 MMGPY cellulosic ethanol in 2005 prices

references: Wright, Mark M. and Brown, Robert C., "Comparative Economics of Biorefineries Based on the Biochemical Platforms", Center for Sustainable Environmental Technologies - Iowa State University, Biofuels, Bioproducts, and Biorefining 1:49-56, 2007

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Capital costs: \$380-390 million

Product Value (PV): \$5 - \$5.50 per gallon gasoline equivalent (GGE)

Notes.

Analysis for nth facility

PV = production cost of fuel, including 10% return on investments

Corn stover feedstock cost = \$75 per short ton

Feedstock capacity = 2000 dry tonne (Mg) stover per day

Equipment, chemical, and labor prices in 2007 dollars

references: Anex, Aden, Kazi, Fortman, Swanson, Wright, Satrio, Brown, Daugaard, Platon, Kothandaraman, Hsu, Dutta, "Techno-Economic Comparison of Biomass-to-Transportation Fuels Via Pyrolysis, Gasification, and Biochemical Pathways", accepted to Fuel 2/10

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Capital costs: \$327-501 million

Product Value (PV): \$5.13 - \$6.50 per gallon gasoline equivalent (GGE)

Notes:

Analysis for nth facility

PV = production cost of fuel, including 10% return on investments

Corn stover feedstock cost = \$83 per short ton

Feedstock capacity = 2000 dry tonne (Mg) stover per day

Ethanol production = 124-210 million L/year

Equipment, chemical, and labor prices in 2007 dollars

references: Anex, Aden, Kazi, Fortman, Kothandaraman, Hsu, Dutta, "Techno-Economic Comparison of Process Technologies for Biochemical Ethanol Production from Corn Stover", Fuel 2010

E.6. Projected Capital and Operating Costs for FAME, Pyrolysis Oil, Ethanol, Methanol, Hydrogen, and Fischer-Tropsch

#### Methanol

Capital costs for 87 MMGPY (5675 bpd) methanol facility: \$254,000,000.00

Operating costs for 87 MMGPY methanol facility: \$56,500,000.00

Notes:

87 MMGPY methanol in 2002 prices

Methanol produced from syngas from unspecified biomass feedstock

references: Wright, Mark M. and Brown, Robert C., "Comparative Economics of Biorefineries Based on the Biochemical and Thermochemical Platforms", Center for Sustainable Environmental Technologies - Iowa State University, Biofuels, Bioproducts, and Biorefining 1:49-56, 2007

#### Hydroge

Capital costs for 182 MMGPY (11870 bpd) hydrogen facility: \$244,000,000.00

Operating costs for 182 MMGPY hydrogen facility: \$53,500,000.00

Notes

182 MMGPY hydrogen in 2002 prices

Hydrogen produced from syngas from unspecified biomass feedstock

references: Wright, Mark M. and Brown, Robert C., "Comparative Economics of Biorefineries Based on the Biochemical and Thermochemical Platforms", Center for Sustainable Environmental Technologies - Iowa State University, Biofuels, Bioproducts, and Biorefining 1:49-56, 2007

E.6. Projected Capital and Operating Costs for FAME, Pyrolysis Oil, Ethanol, Methanol, Hydrogen, and Fischer-Tropsch

#### Fischer-Tropsch

Capital costs for 35 MMGPY (2280 bpd) F-T facility: \$341,000,000.00

Operating costs for 35 MMGPY F-T facility: \$87,500,000.00

Notes:

35 MMGPY F-T in 2002 prices

F-T produced from syngas from unspecified biomass feedstock

references: Wright, Mark M. and Brown, Robert C., "Comparative Economics of Biorefineries Based on the Biochemical and Thermochemical Platforms", Center for Sustainable Environmental Technologies - Iowa State University, Biofuels, Bioproducts, and Biorefining 1:49-56, 2007

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Capital costs: \$500-610 million

Product Value (PV): \$4.50 - \$5 per gallon gasoline equivalent (GGE)

Notes:

Analysis for nth facility

PV = production cost of fuel, including 10% return on investments

Corn stover feedstock cost = \$75 per short ton

Feedstock capacity = 2000 dry tonne (Mg) stover per day

Process involves gasification of corn stover, FT processing, and then hydroprocessing to diesel/gasoline-range fuel

Equipment, chemical, and labor prices in 2007 dollars

references: Anex, Aden, Kazi, Fortman, Swanson, Wright, Satrio, Brown, Daugaard, Platon, Kothandaraman, Hsu, Dutta, "Techno-Economic Comparison of Biomass-to-Transportation Fuels Via Pyrolysis, Gasification, and Biochemical Pathways", accepted to Fuel 2/10

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Capital costs: \$500-600 million

Product Value (PV): \$4 - \$5 per gallon gasoline equivalent (GGE)

Notes:

Analysis for nth facility

PV = production cost of fuel, including 10% return on investments

Corn stover feedstock cost = \$75 per short ton

Feedstock capacity = 2000 dry tonne (Mg) stover per day

Process involves gasification of corn stover, FT processing, and then hydroprocessing to diesel/gasoline-range fuel

Equipment, chemical, and labor prices in 2007 dollars

references: Swanson, Satrio, Brown, Platon, "Techno-Economic Analysis of Biomass-to-Liquids Production Based on Gasification Scenarios", accepted to Fuel 2/10

E.7. Cost Summary for Several Biofuels

PRODUCT	VOL	UME	CAPITAL COSTS	YEARLY OPERATING COSTS	FEED	FEED COSTS	OPERATING + FEED COSTS
	MMGPY	BPD	мм\$	мм\$			\$ per gallon
pyrolysis oil	30	1950	48	9.6	wood chips	\$0.30/dry ton	\$0.32
ethanol	25	1630	27.9	22	grain		\$0.88
ethanol	50	3260	294	76	cellulosic		\$1.52
methanol	87	5675	254	56.5	biomass syngas		\$0.65
FT fuel	35	2283	341	87.5	biomass syngas		\$2.50
FAME	4	260	6.6	8	yellow grease	\$0.17/lb	\$2.00
FAME	4	260	6.6	12.5	soy oil	\$0.31/lb	\$3.13
FAME	10	650	8.8	18	yellow grease	\$0.17/lb	\$1.80
FAME	10	650	8.8	29.2	soy oil	\$0.31/lb	\$2.97

# **Policy Drivers**

E.8. Policy Drivers for Increased Biofuels Use

#### Policy Drivers for Increased Biofuels Usage

#### Omnibus Budget Reconcilliation Act of 1990 - IRS, Customs

Tax credit for small ethanol producers. Tariff on most imported ethanol.

#### 1998 ammendment to 1992 Energy Policy Act - EPA, DOE

Portion of new vehicle purchases by some fleets (including federal and many state govs) must be alternative fuel vehicles. 1998 ammendment includes biodiesel as alternative fuel.

#### Biomass Research and Development Act of 2000 - DOE, USDA

Provides grants for biomass research and demonstration projects.

#### 2001 Value-Added Producer Grants Program - USDA

Provides grants for independent producers of value-added agricultural activities, e.g. biofuel production. Scheduled to end FY2007, extended.

#### Farm Security and Rural Investment Act of 2002 - USDA

Provides grants and loans for renewable energy projects and energy efficiency improvements, e.g. construction of biofuel plants.

#### Commodity Credit Corporation's Bioenergy Program - USDA

Payments for alternative fuel producers, feedstocks included animal fats and recycled oils. Ended June 2006.

#### 2004 American Jobs Creation Act - IRS

Incentives to biofuel producers (feedstocks include animal fats, vegetable oils, recycled oils). Biodiesel must meet ASTM D6751 standard.

#### 2005 Energy Policy Act - IRS, DOE

Provides tax incentives for small biodiesel producers, expired in 2008. Establishes Renewable Fuels Standard.

Also provides loan guarantees for construction of facilities that produce ethanol from cellulose, MSW, or sugar cane.

#### Renewable Fuels Standard - EPA

Mandates 7.5 billion gallons of biofuels used by 2012. Mandates widespread blending of biofuels into petroleum fuels.

Provides additional incentives for cellulosic ethanol producers.

#### Tax Relief and Healthcare Act of 2006 - IRS

Depreciation allowance for cellulosic ethanol plant property owners.

#### 2007 Energy Independence and Security Act (proposed expansion of Renewable Fuels Standard [RFS2]) - EPA

Mandates increased biofuels production from 9 billion gal/yr in 2008 to 36 billion gal/yr in 2022.

Includes cellulosic (advanced, i.e. non-corn feedstock) biofuel, biodiesel, and non-road biofuel requirements.

# **Policy Drivers**

E.8. Policy Drivers for Increased Biofuels Use

Year		Mandated E	Biofuels Usage (billion gallons)
	2008	9	
	2009	11.1	
	2010	12.95	
	2011	13.95	
	2012	15.2	
	2013	16.55	
	2014	18.15	
	2015	20.5	
	2016	22.25	
	2017	24	
	2018	26	
	2019	28	
	2020	30	
	2021	33	
	2022	36	

#### 2008 Farm Bill - USDA

Establishes tax credits for cellulosic ethanol use, among other biofuels incentives that are yet to be funded.

#### Food, Conservation, and Energy Act of 2008 - IRS, USDA

Tax credits for cellulosic ethanol producers and incentives for biorefineries.

#### State Initiatives

Low Carbon Fuel Standard - mandates at least 10% reduction in 2007 carbon intensity in transportation fuels by 2020, carbon intensity based on life-cycle global warming intensity.

Fuel providers must track and reduce the life-cycle global warming intensity of their products.

Mandated by the state of California, 11 other states considering adopting similar proposals.

Every state and the District of Columbia have incentives and/or mandates designed to encourage the production and use of renewable energy sources, including biofuels.

These measures include, but are not limited to, the following:

- ~ tax exemptions
- ~ fueling infrastructure grants
- ~ payments for production
- ~ state tax credits
- ~ renewable fuel usage mandates
- ~ state fleet requirements

references: Yacobucci, Brent D., "Biofuels Incentives: A Summary of Federal Programs", Congressional Research Service Report for Congress, 7/29/2008

Database of State Incentives for Renewables & Efficiency, US Department of Energy and North Carolina Solar Center, www.dsireusa.org, 2009

U.S. Energy Information Administration, "Biofuels in the U.S. Transportation Sector", 2/2007

Georgia Forestry Commission, "Summary of State Incentives and Legislation for Renewable Energy Production", 9/2007

Farrell, Alexander E. and Sperling, Daniel, "A Low-Carbon Fuel Standard for California", 8/2007

Mueller, Stefan, "Assessing the Climate Change Impact of Biofuels", BioCycle Conference on Renewable Energy from Organics Recycling, 10/2007 Environmental Protection Agency, RFS2, www.epa.gov, 1/2009

references (FAME specification):

# E.9. FAME (Fatty Acid Methyl Esters)--Properties

Properties							
	Soybean	Rapeseed	Poultry Fat		US FAME Specifications	EU FAME Specifications	
	Methyl Ester	Methyl Ester	Methyl Ester	No. 2	ASTM D6751-06a	EN 14214: 2003	Comments
Molecular Formula	C18 to C19	C18 to C19		C8 to C25			
Molecular Weight (g/mol)	300 (approx)	300 (approx)		200 (approx)			
Elemental Composition (mass%)							
Carbon	78	81		84-87			
Hydrogen	11	12		13-16			
Oxygen	11	7		0			
Density (g/cm3) at 15deg C	0.87	0.88		0.81-0.89		0.86-0.9	
Vapor Pressure kPa at 38 degC	<1	<1		<1			
Boiling Point		350	342 [d]	188-343			
Flash Point (degC)		179	143 [d]	74	min 120	min 130	Higher flashpoint of FAME influenced by alcohol content from production process
Pour Point (degC)	-3	-15	[-]	-23			FAME low temperature issues
Cloud Point (degC)	Ü	-6 [a]	6.5 [d]	-15 [a]	Report		Trunz lon temperature located
High Heating Value (MJ/L)		٥ [۵]	0.0 [4]	.o [a]	порон		
Low Heating Value (MJ/L)	~32	~37		35-37			SME lower energy density
Water solubility in fuel (ppm)	52	850		<50			OWE lower chargy density
Water content in fuel (mg/kg)		850		230		500 max	
Fuel Miscibility						Joo Illax	
Solvation Potential		High		Low			
Flammability Limits (Vol%)		nigii		LOW			
Lower				1			
Lower Higher				6			
Acid Number			0.00 [-1]	ь			
	50	60	0.39 [d]	40.55	47 :	54 i	EAME annually kinker autom
Cetane Number	52	62		40-55	47 min	51 min	FAME generally higher cetane
Viscosity (mPa-s)	3.0-6.0	3.0-6.0	40011	2.6-4.1	4000	0.5.5.0	
Kinematic viscosity (mm^2/s)		4407.1	4.39 [d]	10511	1.9-6.0	3.5-5.0	1515 B : 5 B: T : 200 : 5 : 111:3
Lubricity (um) *		140 [a]		405 [a]			High Frequency Reciprocating Rig Test wear scar < 380 um indicates good lubricity
+ · · ·							RME better lubricity than No. 2 Diesel
Toxicity							
Acute: Rodent Inhalation LC50 (g/m3)		5000 # 1		10000 17500 [ ]			
Acute: Rat oral LD50 (mg/kg)		> 5000 [b]		12000-17500 [c]			
Acute:Fish LC50 and bacteria EC50 (mg/L)		> 100 [b]		070/			
Subchronic: Rabbit dermal 8 ml/kg applied for 14 days				67% mortality [c]			
Chronic: Mouse dermal 0.05 ml/kg applied 3 X per week for 62 wks				extreme irritation [c]			
Mutagenicity: Salmonella typhimurium Modified Ames Asssay				Negative [c]			
Partition coefficient (Kow)							
Log Kow at 25 degC							
Bioconcentration factor (L/kg) [j]	No	bioconcentration expected [b]					
Soil adsorption				Strongly adsorb [c]			
Half-life in water at typical env. conditions							
Half-life in atmosphere							
Biodegradation		Readily biodegradable [b]					
Appearance		Yellowish liquid [b]		clear to yellow [c]			
Odor		Mild [b]		Mild [b]			
Odor threshold (mg/m3)							
CAS Number				68334-30-5			
references (FAME and No. 2):		, Alternative Fuels Guidebook: Prop				-180, 1997	
		r A., Emissions and Lubricity Evalu		ed Biodiesel Fuels, SwRI 7	507, November 1996		
	b) Lantmänen Ecobränsle AB, Sweden, MSDS, www.ecobransle.se						
	c) CITIGO No. 2 Diesel, MSDS, May 2006, http://www.martineagle.com/MSDS/CitgoLowSulfurDiesel.pdf						
	d) Sunsoil Inc., Poultry Fat, B100, Midwest Laboratories Report Number 09-334-2203, 11/30/09						

Hannu Jaaskelainen, Biodiesel Fuel Standards, http://www.dieselnet.com/tech/fuel\_biodiesel\_std.html

# E.10. FAME--Compatibility and Environmental Issues

#### **Incompatible Materials**

<u>elastomers</u> <u>metals</u>

nitrile lead
natural rubbers tin
polyurethane brass
bronze
zinc

galvanized metals

#### **Compatible Materials**

<u>elastomers</u> <u>metals</u>

Teflon aluminum
Viton stainless steel
fluorinated plastics carbon steel

nylon

most fiberglass

### **Vehicle Compatibility**

Not compatible with terne-coated steel, commonly used for fuel tanks

Nitrile and natural rubber hoses must be replaced with Viton

Compatible with Viton, typically used for most seals and gaskets

Rapeseed Methyl Ester cloud point higher than No. 2 diesel (-6 degC vs. -12 degC), leading to potential issues in cold climates

#### Advantages

Can be blended with diesel in any combination

Biodiesel does not separate from blends if kept above cloud point

Non-toxic

Biodegrades quicker than diesel

Requires little or no modification for use in existing engines

#### Disadvantages

Cleaning Effect, whereby accumulated sediments in storage tanks dissolve in FAME fuels, potentially plugging filters and causing injector deposits Stability can be an issue with certain feedstocks

E.10. FAME--Compatibility and Environmental Issues

#### **Transporting precautions**

Trucks/railcars must be constructed of aluminum, carbon steel, or stainless steel Proper inspection or washout before loading Generally only diesel or biodiesel are acceptable residuals No residual water allowed

Hoses and seals must be made from compatible materials Heating/insulation may be needed to keep above cloud point

#### **Environmental/Health concerns**

Non-toxic

Biodegrades quicker than diesel

#### Compatibility/Fungibility issues

Expressly prohibited in many oil pipelines

Freeze/cloud point restrictions on diesel/blends serve as a defacto biodiesel ban in many oil pipelines

Cleaning effect leads to deposits and plugged filters both in transport and in engines

Ability to biodegrade quicker than diesel means biodiesel cannot be stored as long as diesel

Relatively high freeze and cloud points mean potential biodiesel transport may require insulation/heating

Transport by rail: requires additional private track or existing diesel transport tracks

#### **Current production**

2008 US biodiesel production: 700 million gallons

2008 US biodiesel production capacity: 2.69 billion gallons

references: Lindhjem and Pollack, National Renewable Energy Laboratory, "Impact of Biodiesel Fuels on Air Quality and Human Health: Task 1 Report", www.nrel.gov, 5/2003

National Biodiesel Board, "US Biodiesel Production Capacity", www.biodiesel.org, 6/22/2009

National Renewable Energy Laboratory, "Biodiesel Handling and Use Guide: 4th Edition", Revised 1/2009

National Biodiesel Board, "Materials Compatibility", www.biodiesel.org, 2004

Columbia Engineered Rubber, Inc., www.columbiaerd.com, 2010

Alvarado, Peter J., "Steel vs. Plastics: The Competition for Light-Vehicle Fuel Tanks", JOM 48 (7) pp. 22-25, 1996

# E.11. Green Diesel--Properties

"The advantages of hydrotreating [green diesel] over transesterification [biodiesel] are that the former is compatible with the current infrastructure, the process leads to a deoxygenated and thus stable product that is fully compatible with petroleum-derived diesel fuels, the product exhibits high cetane number and low sulfur content."

Helwani, Othman, Aziz, Fernando, Kim (2009) Technologies for Production of Biodiesel Focusing on Green Catalytic Techniques: A Review, Fuel Processing Technology, Vol. 90, 1502 - 1514.

UOP green diesel and Neste Oil NExBTL diesel are produced by hydrogen saturation and deoxygenation of vegetable oils through catalytic refining.

Snare, Maki-Arvela, Simakova, Myllyoja, Murzin (2009) Overview of Catalytic Methods for Production of Next Generation Biodiesel from Natural

Oils and Fats, Russian Journal of Physical Chemistry B, Vol. 3, pp. 3-17.

Kalnes, Marker, Shonnard, Koers, *Green Diesel and Biodiesel a Technoeconomic and Life Cycle Comparison*, 1st Alternative Fuels Technology Conference, February 2008, Prague, Czechoslovakia

#### **Properties**

	UOP*	Neste Oil**	No. 2	
	Green Diesel	NExBTL Diesel	<u>Diesel</u>	
Molecular Formula			C8 to C25	
Molecular Weight (g/mol)			200 (approx)	
Elemental Composition (mass%)			04.07	
Carbon			84-87	
Hydrogen	0	0	13-16	M=
Oxygen	0 0.78	0 0.775 - 0.785	0 0.81-0.89	No oxygen
Density (g/cm3) at 15deg C	0.78	0.775 - 0.765		
Vapor Pressure kPa at 38 degC			<1 188-343	
Boiling Point Flash Point (degC)			188-343 74	
			-23	
Pour Point (degC) Cloud Point (degC)	-10 to +5	-5 to -30	-23 -15 [a]	
	-10 10 +5	-5 10 -30	-15 [a]	
High Heating Value (MJ/L)	34	~ 34	35-37	Cimilar anaray contant
Low Heating Value (MJ/L) Water Solubility at 21 degC	34	~ 34	33-37	Similar energy content
Water in fuel (ppm)			<50	
Water content in fuel (mg/kg)			<50	
Fuel Miscibility				
Solvation Potential			Low	
Flammability Limits (Vol%)			LOW	
Lower			1	
Higher			6	
Acid Number			U	
Cetane Number	70 to 90	84 - 99	40-55	Higher cetane
Viscosity (mPa-s)	70 10 30	64 - 99	2.6-4.1	riigher cetarie
Kinematic viscosity (mm^2/s)		2.9 - 3.5	2.5-4.1	
Lubricity (um)		2.0 - 3.0	405 [a]	
Editions (diff)			400 [a]	

# E.11. Green Diesel--Properties

Toxicity Acute: Rat oral LD50 (ml/kg) Acute: Rabbit dermal LD50 (ml/kg) Acute:LC50 for freshwater fish (Juven. Am. Shad) (ppm) Acute:LC50 for saltwater fish (Menhaden) (ppm) Acute:LC50 for aquatic invertebrate (shrimp) (ppm) Acute: Aquatic plants - No observable effect concentration (mg/L) Subchronic: Rabbit dermal 8 ml/kg applied for 14 days Chronic: Mouse dermal 0.05 ml/kg applied 3 X per week for 62 wks Mutagenicity: Salmonella typhimurium Modified Ames Asssay Teratogenicity: Mouse oral Lowest observable effect conc. (% calories) Partition coefficient (Kow) Log Kow at 25 degC Bioconcentration factor (L/kg) Transport between Environmental Compartments Air, water, soil, sediment (% mass distribution) Half-life in water at typical env. conditions Half-life in atmosphere Photodegradation half-life in air Biodegradation in water/sediment for 30 days Appearance Odor Odor Threshold (mg/L) CAS number \* UOP LLC, a Honeywell Company

clear to yellow [c] Mild [b]

9 [c]

> 5 [c]

2400 [c]

10 [c]

10 [c]

67% mortality [c] extreme irritation [c]

Negative [c]

68334-30-5

\*\* Neste Oil Oyj, Espoo, Finland

references (UOP Green Diesel):

Kalnes, Marker, Shonnard, Koers, Green Diesel and Biodiesel a Technoeconomic and Life Cycle Comparison, 1st Alternative Fuels Technology Conference, February 2008, Prague, Czechoslovakia

references (Neste NExBTL Diesel):

Rantanen, Linnaila (2005) NExBTL - Biodiesel Fuel of the Second Generation, SAE Technical Paper 2005-01-3771

references (No. 2):

Bechtold, Richard L., Alternative Fuels Guidebook: Properties, Storage, Dispensing, and Vehicle Facility Modifications, SAE Order Number R-180, 1997

a) Sharp, Christopher A., Emissions and Lubricity Evaluation of Rapeseed Derived Biodiesel Fuels, SwRI 7507, November 1996

b) Hess Material Data Safety Sheet No. 9909, Diesel Fuel, 10/18/2006, http://www.hess.com/ehs/msds/9909DieselFuelAllTypes.pdf

c) CITIGO No. 2 Diesel, MSDS, May 2006, http://www.martineagle.com/MSDS/CitgoLowSulfurDiesel.pdf

E.12. Green Diesel--Compatibility and Environmental Issues

# **Advantages**

Higher cetane number than both petroleum diesel and FAME
Higher energy content than biodiesel
Similar properties to petroleum diesel due to lack of oxygen
Requires little or no modification to run in existing diesel engines
Low cloud point - suitable for use in cold weather
Can be blended with petroleum diesel

references: UOP, UOP/Eni Ecofining Process for Green Diesel Fuel, www.uop.com, 2007

Netse Oil, Press Release 6/18/08, www.nesteoil.com, 2008

Rantanen, Linnaila (2005) NExBTL - Biodiesel Fuel of the Second Generation, SAE Technical Paper 2005-01-3771

# E.13. F-T (Fischer-Tropsch Fuel)--Properties

<u>Properties</u>		ExxonMobil F-T Diesel		
	SunDiesel*	from Natural Gas Feedstock	No. 2	
Molecular Formula			C8 to C25	
Molecular Weight (g/mol)			200 (approx)	
Elemental Composition (mass%)				
Carbon	85.79		84-87	
Hydrogen	15.54		13-16	
Oxygen			0	
Sulfur (ppm)	0.3	0	311 [c]	Lower sulfur content
Density (g/cm3)	0.7612	0.774	0.81-0.89 at 15 deg C	
Vapor Pressure kPa			<1 at 38 degC	
Boiling Point (degC)			188-343	
Flash Point (degC)		60	74	
Pour Point (degC)	-20.5		-23	
Cloud Point (degC)	-15.5		-15 [a]	
High Heating Value (MJ/kg)	47.2		54 [b]	
Low Heating Value (MJ/kg)	44.6		41-44	Similar energy content for LHV
Water Content (mass%)			negligible	
Water Solubility at 21 degC				
Water in fuel (ppm)			<50	
Fuel Miscibility				
Solvation Potential			Low	
Flammability Limits (Vol%)				
Lower			1	
Higher			6	
pH			8 - 9	
Cetane Number	80	74	40-55	Higher cetane number
Viscosity (mPa-s)	1.180	2.059	2.6-4.1	Lower viscosity
Lubricity (um)			405 [d]	

# E.13. F-T (Fischer-Tropsch Fuel)--Properties

Toxicity Acute: Rat oral LD50 (ml/kg) 9 [e] Acute: Rabbit dermal LD50 (ml/kg) > 5 [e] Acute:LC50 for freshwater fish (Juven. Am. Shad) (ppm) 2400 [e] Acute:LC50 for saltwater fish (Menhaden) (ppm) 10 [e] Acute:LC50 for aquatic invertebrate (shrimp) (ppm) 10 [e] Acute:Aquatic plants - No observable effect concentration (mg/L) Subchronic: Rabbit dermal 8 ml/kg applied for 14 days 67% mortality [e] Chronic: Mouse dermal 0.05 ml/kg applied 3 X per week for 62 wks extreme irritation [e] Mutagenicity: Salmonella typhimurium Modified Ames Asssay Negative [e] Teratogenicity: Mouse oral Lowest observable effect conc. Partition coefficient (Kow) Log Kow at 25 degC Bioconcentration factor (L/kg) Transport between Environmental Compartments Air, water, soil, sediment (% mass distribution) Half-life in water at typical env. conditions Half-life in atmosphere Photodegradation half-life in air Biodegradation in water/sediment for 30 days Appearance clear to yellow [e] Odor Mild [f] Odor Threshold (mg/L) CAS number 68334-30-5

\* SunDiesel is a biomass to liquid fuel, which is manufactured using a Fischer-Tropsch process and produced by CHOREN Industries GmbH of Germany

references (SunDiesel):

Ng, Biruduganti, Stork, Comparing the Performance of SunDiesel and Conventional Diesel in a Light-Duty Vehicle and Heavy-Duty Engine, SAE Technical Paper 2005-01-3776

references (ExxonMobil F-T Diesel):

Alleman, McCormick, Fischer-Tropsch Diesel Fuels - Properties and Exhaust Emissions: A Literature Review, SAE Technical Paper 2003-01-0763

references (No. 2):

Bechtold, Richard L., Alternative Fuels Guidebook: Properties, Storage, Dispensing, and Vehicle Facility Modifications, SAE Order Number R-180, 1997

- a) Sharp, Christopher A., Emissions and Lubricity Evaluation of Rapeseed Derived Biodiesel Fuels, SwRI 7507, November 1996
- b) Hess, Boehman, Tijm, Waller, Experimental Studies of the Impact of CETANER on Diesel Combustion and Emissions, SAE Technical Paper 2000-01-2886
- c) Bertola, Boulouchos, Oxygenated Fuels for Particulate Emissions Reduction in Heavy-Duty Di-Diesel Engines with Common-Rail Fuel Injection, SAE Technical Paper 2000-01-2885
- d) Sharp, Christopher A., Emissions and Lubricity Evaluation of Rapeseed Derived Biodiesel Fuels, SwRI 7507, November 1996
- e) CITIGO No. 2 Diesel, MSDS, May 2006, http://www.martineagle.com/MSDS/CitgoLowSulfurDiesel.pdf
- f) Hess Material Data Safety Sheet No. 9909, Diesel Fuel, 10/18/2006, http://www.hess.com/ehs/msds/9909DieselFuelAllTypes.pdf

E.14. F-T--Compatibility and Environmental Issues

#### **Vehicle Compatibility**

Cloud point comparable to No. 2 diesel, suitable for use in cold climates

"Requires little or no modification for use in current diesel engines" according to the CHOREN group

## Advantages

"Requires little or no modification for use in current diesel engines" according to the CHOREN group produces lower NOx and PM emissions than diesel in engines due to low aromatic content "can be directly fed into the infrastructure of existing distribution channels" according to the CHOREN group high energy content Higher cetane number than diesel

references:

CHOREN Industries, "Biomass-to-Liquid Fuels (BtL) - Made by CHOREN process, Environmental Impact, and Latest Developments", Automobile and Environment at Belgrade EAEC Congress, May 2005 Intelligent Energy Europe, Fischer-Tropsch Diesel, www.refuel.eu, 2010

Kamara, Coetzee, Overview of High-Temperature Fischer-Tropsch Gasline and Diesel Quality, Energy & Fuels, 2009, 23, 2242-2247.

# E.15. Algae Biodiesel--Properties

<u>Properties</u>					
	Microalgal		US FAME Specifications	EU FAME Specifications	
	<u>Biodiesel</u>	No. 2	ASTM D6751-06a	EN 14214: 2003	
Molecular Formula		C8 to C25			
Molecular Weight (g/mol)		200 (approx)			
Elemental Composition (mass%)					
Carbon		84-87			
Hydrogen		13-16			
Oxygen		0			
Density (g/cm3) at 15deg C	0.864	0.81-0.89		0.86-0.9	
Vapor Pressure kPa at 38 degC		<1			
Boiling Point		188-343			
Flash Point (degC)	115	74	min 120	min 130	Higher flash point
Pour Point (degC)		-23			3 ,
Cloud Point (degC)		-15 [a]	Report		
High Heating Value (MJ/L)	35 [a]	36-40 [b]			Similar energy content
Low Heating Value (MJ/L)		35-37			3,
Water Solubility at 21 degC					
Water in fuel (ppm)		<50			
Water content in fuel (mg/kg)				500 max	
Fuel Miscibility					
Solvation Potential		Low			
Flammability Limits (Vol%)		20			
Lower		1			
Higher		6			
Acid Value (mg KOH /g)	0.374 [a]	Max 0.5 [b]	Max 0.5 [a]		
Cetane Number	0.074 [u]	40 - 55	47 min	51 min	
Viscosity (mPa-s)		2.6 - 4.1		0	
Kinematic viscosity (mm^2/s)	5.2	3.2 - 4.6	1.9-6.0	3.5-5.0	Higher kinematic viscosity
Lubricity (um)	J.L	405 [a]	0.0	0.0 0.0	geeado vidoodky
200110117 (01117)		.55 [4]			

# E.15. Algae Biodiesel--Properties

Toxicity Acute: Rat oral LD50 (ml/kg) Acute: Rabbit dermal LD50 (ml/kg) Acute:LC50 for freshwater fish (Juven. Am. Shad) (ppm) Acute:LC50 for saltwater fish (Menhaden) (ppm) Acute:LC50 for aquatic invertebrate (shrimp) (ppm) Acute: Aquatic plants - No observable effect concentration (mg/L) Subchronic: Rabbit dermal 8 ml/kg applied for 14 days Chronic: Mouse dermal 0.05 ml/kg applied 3 X per week for 62 wks Mutagenicity: Salmonella typhimurium Modified Ames Asssay Teratogenicity: Mouse oral Lowest observable effect conc. (% calories) Partition coefficient (Kow) Log Kow at 25 degC Bioconcentration factor (L/kg) Transport between Environmental Compartments Air, water, soil, sediment (% mass distribution) Half-life in water at typical env. conditions Half-life in atmosphere Photodegradation half-life in air Biodegradation in water/sediment for 30 days Appearance Odor Odor Threshold (mg/L) CAS number

clear to yellow [c] Mild [d]

9 [c]

> 5 [c]

2400 [c]

10 [c]

10 [c]

67% mortality [c]

extreme irritation [c]

Negative [c]

68334-30-5

references (FAME specification):

references (No. 2):

Hannu Jaaskelainen, Biodiesel Fuel Standards, http://www.dieselnet.com/tech/fuel\_biodiesel\_std.html

a) Xu, Miao, Wu, High Quality Biodiesel Production from a Microalga Chlorella Protothecides by Heterotrophic Growth Fermenters, 2006, 126, 499-507.

Bechtold, Richard L., Alternative Fuels Guidebook: Properties, Storage, Dispensing, and Vehicle Facility Modifications, SAE Order Number R-180, 1997 a) Sharp, Christopher A., Emissions and Lubricity Evaluation of Rapeseed Derived Biodiesel Fuels, SwRI 7507, November 1996

- b) Xu, Miao, Wu, High Quality Biodiesel Production from a Microalga Chlorella Protothecides by Heterotrophic Growth Fermenters, 2006, 126, 499-507.
- c) CITIGO No. 2 Diesel, MSDS, May 2006, http://www.martineagle.com/MSDS/CitgoLowSulfurDiesel.pdf
- d) Hess Material Data Safety Sheet No. 9909, Diesel Fuel, 10/18/2006, http://www.hess.com/ehs/msds/9909DieselFuelAllTypes.pdf

E.16. Algae Biodiesel--Compatibility and Environmental Issues

# **Advantages**

Comparable heating value to diesel, higher than FAME Low cold filter plugging point indicates good cold weather performance

# Disadvantages

High viscosity means increased pumping work required for transport Rich in unsaturated fats, leading to oxidation susceptibility, will not comply with Euro biodiesel regulations unless further processed

references: Miao, Wu, Biodiesel Production from Heterotrophic Microalgal Oil, Bioresource Technology, 2006, 97, 841-846

Chisti, Yusuf, Biodiesel from Microalgae, Biotechnology Advances, 2007, 25, 294-306

# E.17. DME (Dimethyl Ether)--Properties

<u>Properties</u>			
	<u>Dimethyl ether</u>	No. 2	<u>Comments</u>
Molecular Formula	CH3-O-CH3	C8 to C25	
Molecular Weight (g/mol)	46.1	200 (approx)	
Elemental Composition (mass%)			
Carbon	52	84-87	
Hydrogen	13	13-16	
Oxygen	35	0	
Density (g/cm3) at 20deg C	1.91E-03	0.81-0.89	
Vapor Pressure kPa at 25 degC	593	<1	DME gaseous
Boiling Point (degC)	-24.8	188-343	
Flash Point (degC)	-5.5	74	
Pour Point (degC)		-23	
Cloud Point*		-15	
High Heating Value (MJ/L)			
Low Heating Value (MJ/L)		35-37	
Water Solubility at 25 degC (g/L)	35.3		
Fuel Miscibility			
Solvation Potential		Low	
Flammability Limits (Vol%)			
Lower	3.4	1	
Higher	18	6	DME highly flammable
Acid Number			3 ,
Cetane Number		40-55	
Viscosity (mPa-s)		2.6-4.1	
Lubricity (um) *		405	
Toxicity			
Acute: Rat inhalation (ppm)	164000		
Acute:Freshwater Fish - No observable effect concentration (mg/L)	> 4000		
Acute:Daphnia - No observable effect concentration (mg/L)	> 4000		
Acute: Algae	Predicted to be nontoxic		
Chronic: Rat - No observable effect concentration (ppm)	2000 ppm		
Genotoxicity - Bacteria, DME 0-75%	None		
Teratogenicity - Rat, DME 0-20,000 ppm	None		
Partition coefficient (Kow)	octanol-water		
Log Kow at 25 degC	0.1		
Bioconcentration factor (L/kg) [i]	0.7		Low potential for bioconcentration in aquatic organisms
Photodegradation half-life in water	2.2 years		aquallo organionio
Photodegradation half-life in air	5.4 days		
Biodegradation - 2 mg/L in activated sludge for 28 days	5% degredation		
Appearance	Colorless gas [a]		
Odor	Slightly ethereal [a]		
	- 3)[]		

DME references:

US EPA High Production Volume Information System, DME Detailed Chemical Results, http://iaspub.epa.gov/oppthpv/quicksearch.display?pChem=100157

a) Praxair Material Safety Data Sheet, Dimethyl Ether, P-4589-D, May 2009

\*Emissions and Lubricity Evaluation of Rapeseed Derived Biodiesel Fuels

SwRI 7507, November 1996 Christopher A. Sharp

No. 2 Diesel references:

### E.18. DME--Compatibility and Environmental Issues

#### **Incompatible Materials**

<u>elastomers</u> <u>metals</u>

Viton lithium aluminum hydride silicon rubber aluminum hyrdide

natural rubber butyl rubber neoprene

#### **Compatible Materials**

 elastomers
 metals

 Teflon
 Carbon Steel

 Buna N
 Stainless Steel

Aluminum Brass Copper

### **Vehicle Compatibility**

Not compatible with Viton and natural rubber, commonly used materials for gaskets, seals, and hoses Exists as a gas at STP, must be compressed for use as engine fuel

#### Advantages

Only minor modification needed to run in existing engines Short carbon chain compound leads to low PM, NOx, and CO emissions

#### Disadvantages

Exists as gas under normal operating conditions Highly flammable Soluble in water

#### **Transporting Precautions**

Must be compressed to a liquid for ease of transport

#### **Environmental/Health concerns**

No known adverse ecological effects

Highly flammable

#### Compatibility/Fungibility issues

Only minor modification needed to run in existing engines Must be compressed to a liquid for ease of transport

references: Air Liquide, www.airliquide.com, 12/2009

Avantec Performance Chemicals, www.inventec.dehon.com, 12/2009 Praxair, "Dimethyl Ether MSDS", www.praxair.com, 10/15/2007 Problem Solving Products Inc., www.pspglobal.com, 12/2009 Columbia Engineered Rubber, Inc., www.columbiaerd.com, 2010

Alvarado, Peter J., "Steel vs. Plastics: The Competition for Light-Vehicle Fuel Tanks", JOM 48 (7) pp. 22-25, 1996

### E.19. Glyme--Properties

Air Products and Chemicals, Inc. developed a process for the production of diglyme and triglyme from coal-derived synthesis gas. This could be adapted for biomass derived synthesis gas. However issues related to the toxicity of glymes may have prevented further development.

"A series of literature searches was conducted regarding the health hazards associated with 1,2-dimethoxyethane (monoglyme), diglyme, and triglyme. The literature implies that glymes are teratogens and reproductive toxins."

Reference:

Air Products and Chemicals, Inc. (1998) Alternative Fuels and Chemicals from Synthesis Gas, Quarterly Report, DOE contract number DE-FC22-95PC93052.

#### **Properties**

	<u>Diglyme</u>	No. 2	<u>Comments</u>
Molecular Formula	C6H14O3	C8 to C25	
Molecular Weight (g/mol)	134.2	200 (approx)	
Elemental Composition (mass%)			
Carbon	53.7%	84-87	
Hydrogen	10.4%	13-16	
Oxygen	35.8%	0	
Density (g/cm3)	0.938 at 25 degC	0.81-0.89 at 15 deg C	
Vapor Pressure kPa	0.395 at 25 degC [i]	<1 at 38 degC	Low vapor pressure for an organic solvent
Boiling Point (degC)	161.85	188-343	
Flash Point (degC)	57 [b]	74	
Pour Point (degC)		-23	
Cloud Point (degC)	< -17 [f]	-15 [a]	
High Heating Value (MJ/L)	26 [d]	46 [b]	Lower energy content
Low Heating Value (MJ/L)	23 [c]	35-37	
Water Solubility in fuel at 21degC (ppm)	Complete	<50	Water is soluble in diglyme
Fuel Miscibility	at least 45 vol% completely miscable in diesel fuel [e]		
Solvation Potential	High for organics [h]	Low	Excellent organic solvent
Flammability Limits (Vol%)			
Lower	1.5	1	
Higher	17.4	6	Wider flammability range
Acid Number			
Cetane Number	126 [c]	40-55	
Viscosity (mPa-s)	0.989	2.6-4.1	
Lubricity (um)	783 [g]	265 [c]	High Frequency Reciprocating Rig Test wear scar < 380 um indicates good lubricity No. 2 Diesel better lubricity than diglyme
			110. 2 Diodoi bottoi lubilotty than digiyino

### E.19. Glyme--Properties

Toxicity
Acute: Rat inhalation (ppm)
Acute:LC50 for fish, daphnia and algae
Chronic: Mouse oral (mg/Kg)
Partition coefficient (Kow)
Log Kow at 25 degC
Bioconcentration factor (L/kg) [j]
Soil adsorption

Half-life in water at typical env. conditions Half-life in atmosphere Photodegradation half-life in air Biodegradation Appearance Odor 1000 [b] 
> 1000 mg/L [k] 
Relativlely non-toxic for studied aquatic species

1250 - Teratogenic; 5 - Reproductive [b] 367- Lowest reported [d] octanol-water

- 0.36 [k] 
< 100 [i] 
Not expected to significantly bioaccumulate

When released into soil, largely evaporates,

Distributes primarily to water and secondarily to soil [k]

< 1 day [i]
7.33 hours [k]
Not readily biodegradable [k]
Clear, colorless liquid [i]
Slight aromatic odor [i]

moderately biodegrades, and can leach into groundwater [i]

> 1 year [k]

references (diglyme):

Wallace, W.J.; Mathews, A.L., Density, Refractive Indices, Molar Refractions, and Viscosities of Diethylene Glycol Dimethyl Ether-Water Solutions at 25 C, J. Chem. Eng. Data, 1964, 9, 267-268.

- a) Stull, D.R., Vapor Pressure of Pure Substances Organic Compounds, Ind. Eng. Chem., 1947, 39, 517-540
- b) Honeywell, Burdick and Jackson Material Safety Data Sheet, http://www51.honeywell.com/sm/rlss/bandi/common/documents/2.4.67 msds.pdf
- c) Ren, Huang, Miao, Jiang, Liu, Wang, Effect of the Addition of Diglyme in Diesel Fuel on Combustion and Emissions in a Compression-Ignition Engine, Energy and Fuels, 2007, 21, 2573-2583.
- d) Ferro Fine Chemicals, Product Data Sheet, diglyme, http://www.d-orland.com/pdf/Diglyme.pdf
- e) Air Products and Chemicals for DOE, Alternative Fuels and Chemicals From Synthesis Gas, Quarterly Report Jan1-March 31, 1998. http://www.osti.gov/bridge/purl.cover.jsp:jsessionid=98C35367D8BB64EC81F1D3F36F8998A0?purl=/2008-izPpak/webyiewable/

f) Howard Hess, Effect of Oxygenated Cetane Improver on Diesel Engine Combusiton and Emissions

http://www.ems.psu.edu/~boehman/altfuels.html

- g) Bertola, Boulouchos, Oxygenated Fuels for Particulate Emissions Reduction in Heavy-Duty Di-Diesel Engines with Common-Rail Fuel Injection, SAE Technical Paper 2000-01-2885
- h) Merck Index, 11th Edition, 3148
- i) J.T. Baker MSDS, http://www.jtbaker.com/msds/englishhtml/b3312.htm
- j) EPA Methodology for Deriving Ambient Water Quality Criteria for the Protection of Human Health (2000), http://www.epa.gov/waterscience/criteria/humanhealth/method/tsdvol2.pdf
- k) EPA 201-15023, Diglyme robust summary, http://www.epa.gov/hpv/pubs/summaries/diglyme/c15023rs.pdf

references (No. 2 diesel):

Bechtold, Alternative Fuels Guidebook: Properties, Storage, Dispensing, and Vehicle Facility Modifications, SAE Order Number R-180, 1997

- a) Sharp, Christopher A., Emissions and Lubricity Evaluation of Rapeseed Derived Biodiesel Fuels, SwRI 7507, November 1996
- b) Hess, Boehman, Tijm, Waller, Experimental Studies of the Impact of CETANER on Diesel Combustion and Emissions, SAE Technical Paper 2000-01-2886
- c) Bertola, Boulouchos, Oxygenated Fuels for Particulate Emissions Reduction in Heavy-Duty Di-Diesel Engines with Common-Rail Fuel Injection, SAE Technical Paper 2000-01-2885
- d) ChemCas, http://www.chemcas.com/msds/cas/msds57/68476-34-6.asp

### E.20. Glyme--Compatibility and Environmental Issues

#### **Incompatible Materials**

<u>elastomers</u> <u>metals</u>

PVC nitrile Viton

#### **Compatible Materials**

<u>elastomers</u> <u>metals</u> polyethylene <u>all metals</u>

#### **Vehicle Compatibility**

Compatible with fuel tank materials (polyethylene or metals)
Not compatible with typical gasket, seal, and hose materials (nitrile and Viton)
Low cloud point - suitable for use in cold climates

#### Environmental/Health concerns

Highly toxic

#### Compatibility/Fungibility issues

Necessitates o-ring and hose replacement for material compatibility

references: Bertola, Boulouchos, Oxygenated Fuels for Particulate Emissions Reduction in Heavy-Duty Di-Diesel Engines with Common-Rail Fuel Injection, SAE Technical Paper 2000-01-2885

Columbia Engineered Rubber, Inc., www.columbiaerd.com, 2010

Alvarado, Peter J., "Steel vs. Plastics: The Competition for Light-Vehicle Fuel Tanks", JOM 48 (7) pp. 22-25, 1996

### E.21. Ethanol--Properties

<u>Properties</u>						
	<u>Ethanol</u>	<u>E5</u>	<u>E10</u>	<u>E15</u>	<u>No. 2</u>	<u>Comments</u>
Molecular Formula	C2H5OH				C8 to C25	
Molecular Weight (g/mol)	46.07				200 (approx)	
Elemental Composition (mass%)						
Carbon	52.2				84-87	
Hydrogen	13.1				13-16	
Oxygen	34.7				0	
Density (g/cm3) at 15deg C	0.79	0.835 [b]	0.833 [b]	0.8315 [b]	0.8362 [b]	
Vapor Pressure kPa at 38 degC	15.9				<1	
Boiling Point	78				188-343	
Flash Point (degC)	13	< 40 [b]	< 40 [b]	< 40 [b]	63 [b]	
Pour Point (degC)	.0	1 10 [0]	1 .0 [0]	1.0[0]	-23	
Cloud Point (degC)		-1.2 [b]	-1.2 [b]	-0.1 [b]	-3.1 [b]	
Freezing Point (degC)	-114	1.2 [0]	1.2 [0]	0.1 [b]	-40 to -1	
High Heating Value (MJ/L)	23				37-40	
	23	25 [h]	24 [h]	22 E [h]		Louise anarmi contant
Low Heating Value (MJ/L)	21	35 [b]	34 [b]	33.5 [b]	36 [b]	Lower energy content
Water Solubility at 21 degC	400				NIU - U- I-	
Water in fuel (Vol%)	100				Negligible	
Fuel Miscibility						
Solvation Potential					Low	
Flammability Limits (Vol%)						
Lower	4.3				1	
Higher	19				6	
Acid Number						
Cetane Number		51.8 [b]	50 [b]	48.3 [b]	52.2 [b]	
Viscosity (mPa-s)	1.19				2.6-4.1	
Kinematic viscosity at 40 degC mm^2/s		2.88 [b]	2.45 [b]	2.47 [b]	2.88 [b]	Lower viscosity
Lubricity (um)					405 [c]	
Toxicity						
Acute: Mouse oral LD50 (mg/kg)	8300 [e]					
Acute:LC50 for freshwater fish (trout) (mg/L)	11200 [e]					
Acute:LC50 for aquatic invertebrate (daphnia) (vol%)	1.5[e]					
Acute:Aquatic plants - No observable effect concentration (mg/L)	< 500 [e]					
Chronic: Rat oral No observable effect conc. (mass% in food)	< 5 [e]					
Teratogenicity: Mouse oral Lowest observable effect conc. (% calories)	25% [e]					
Partition coefficient (Kow)	octanol-water					
Log Kow at 25 degC	-0.31 [e]					
Bioconcentration factor (L/kg)	Low based on Kow					
Transport between Environmental Compartments	Low based on Now					
Air, water, soil, sediment (% mass distribution)	13, 44.8, 42.1,0.039 [e]					
Half-life in water at typical env. conditions	10, 44.0, 42.1,0.009 [8]					
	6 days [d]					
Half-life in atmosphere	6 days [d]					
Photodegradation half-life in air	15.4 hrs [e]					
Biodegradation in water/sediment for 30 days	91% [e]					
Appearance	clear, water-like liquid					
Odor Threshold (mg/L)	0.1 air, 100 water [d]					
CAS number	64-17-5					

references:

Bechtold, Richard L., Alternative Fuels Guidebook: Properties, Storage, Dispensing, and Vehicle Facility Modifications, SAE Order Number R-180, 1997 NIST Chemistry WebBook

b) Dominguez, Miguel, Arjona, Millan, The Effects of Ethanol-Diesel Blended Fuels on the Performance and Emissions of Unmodified Diesel Engines, 14th European Biomass Conference and Exhibition: Biomass for Energy, Industry and Climate Protection, Paris, Oct.

c) Sharp, Christopher A., Emissions and Lubricity Evaluation of Rapeseed Derived Biodiesel Fuels, SwRI 7507, November 1996

d) Spectrum Chemical Fact Sheet, http://www.speclab.com/compound/c64175.htm

e) US EPA High Production Volume Information System, Ethanol Detailed Chemical Results, http://iaspub.epa.gov/oppthpv/quicksearch.display?pChem=100220

### E.22. Ethanol--Compatibility and Environmental Issues

### **Incompatible Materials**

 elastomers
 metals

 cork gasket material
 lead

 natural rubbers
 aluminum

 polyurethane
 brass

 PVC
 terne

 zinc

lead-based solder

#### **Compatible Materials**

<u>elastomers</u> <u>metals</u>
thermoset-reinforced fiberglass carbon steel
thermoplastic stainless steel
Buna N bronze
neoprene

neoprene Viton Teflon nitrile

polypropylene

#### **Vehicle Compatibility**

Incompatible with terne-coated steel, commonly used for fuel tanks Hoses constructed from natural rubbers must be replaced with Viton, nitrile, etc.

### Advantages

Requires little or no modification for use in exisitng engines Reduces PM, CO, NOx emissions

#### Disadvantages

Cleaning Effect Miscible with water Requires co-solvent

### E.22. Ethanol--Compatibility and Environmental Issues

#### **Trasnporting Precautions**

Vessels must be cleaned out to prevent contamination due to water and cleaning effect

#### Environmental/Health concerns

Toxic

Flammable

### Compatibility/Fungibility issues

Miscible with water

Cleaning effect leads to deposits and plugged filters both in transport and in engines Transport by rail: requires additional private track or existing gasoline transport tracks Stress corrosion cracking observed in pipelines due to ethanol

### **Current production**

2007 US ethanol production: 6.48 billion gallons 2007 US ethanol production capacity: 7.5 billion gallons 2008 projected US ethanol production capacity: 13.3 billion gallons

references: Biofuels Digest, "US Ethanol Production Capacity to Increase to 13.3 Billion Gallons in 2008", www.biofuelsdigest.com, 1/9/2008

Biofuels Journal, "Annual and Monthly US Ethanol Production", www.biofuelsjournal.com, 12/5/2006

Department of Energy, "Handbook for Handling, Storing, and Dispensing E85", 7/2006

Fanick, National Renewable Energy Laboratory, "Fuel and Fuel Additive Registration Testing of Ethanol-Diesel Blend for O2Diesel, Inc.", www.nrel.gov, 2/2004

Pipeline Research Council International, "Stress Corrosion Cracking", 7/2006

Columbia Engineered Rubber, Inc., www.columbiaerd.com, 2010

Alvarado, Peter J., "Steel vs. Plastics: The Competition for Light-Vehicle Fuel Tanks", JOM 48 (7) pp. 22-25, 1996

### E.23. Sesquiterpene (Farnesene)--Properties

"Sesquiterpenes and most fatty-acid-derived hydrocarbons are suitable for the production of diesel fuel and include farnesene, ethyl hexadecanoate, and pentadecane One advantage these molecules have over shortchain alcohols is their very low solubility in water."

Rude, Schirmer, New Microbial Fuels: A Biotech Perspective, Current Opinion in Microbiology, 2009, 12, 274-281

#### **Properties**

	ramesene	<u>INU. Z</u>	
Molecular Formula	C15H24	C8 to C25	
Molecular Weight (g/mol)	204.4	200 (approx)	
Elemental Composition (mass%)			
Carbon	88.24	84-87	
Hydrogen	11.76	13-16	
Oxygen		0	
Nitrogen		0	
Density (g/cm3)	0.844-0.8790 at 25 degC [a]	0.81-0.89 at 15 deg C	
Vapor Pressure kPa	0.001 at 20 degC [b]	<1 at 38 degC	
Boiling Point (degC)	260 [a]	188-343	
Flash Point (degC)	110 [a]	74	Higher flash point
Pour Point (degC)	***	-23	
Cloud Point (degC)		-15 [a]	
High Heating Value (MJ/kg)	47* [c]	54 [b]	
Low Heating Value (MJ/kg)		41-44	
Water Content (mass%)	negligible	negligible	
Water Solubility at 21 degC			
Water in fuel (ppm)	insoluble [a, c]	<50	Water insoluble
Fuel Miscibility			
Solvation Potential		Low	
Flammability Limits (Vol%)			
Lower		1	
Higher		6	
pH			
Cetane Number	Low** [c]	40-55	
Viscosity (mPa-s)		2.6-4.1	
Lubricity (um)		265 [c]	

Farnesene

No 2

Toxicity

Acute: Mouse oral LD50 (mg/kg)

Acute:LC50 for freshwater fish (trout) (mg/L)
Acute:LC50 for aquatic invertebrate (daphnia) (vol%)

Acute:Aquatic plants - No observable effect concentration (mg/L)

Chronic: Rat oral No observable effect conc. (mass% in food)

Teratogenicity: Mouse oral Lowest observable effect conc. (% calories)

Partition coefficient (Kow)

Log Kow at 25 degC Bioconcentration factor (L/kg) [j]

Transport between Environmental Compartments

Air, water, soil, sediment (% mass distribution) Half-life in water at typical env. conditions

Lifetime in atmosphere in presence of ozone

Photodegradation half-life in air

Biodegradation in water/sediment for 30 days

Appearance

Odor Odor Threshold (mg/L)

CAS number

Natural sources

1 hr [e]

Colorless to light yellow liquid [d]

Citrus, herbaceous [d]

502-61-4

Emitted to atm by plants and trees

references (farnesene):

NIST Chemistry WebBook, http://webbook.nist.gov/cgi/cbook.cgi?Name=farnesene&Units=SI

a) Sigma-Aldrich, MSDS, Product Number W383902

e) Kourtchev et al., Atmospheric Environment, Vol. 43, pg 3182, 2009.

references (No. 2)

Bechtold, Richard L., Alternative Fuels Guidebook: Properties, Storage, Dispensing, and Vehicle Facility Modifications, SAE Order Number R-180, 1997 Sharp, Christopher A., Emissions and Lubricity Evaluation of Rapeseed Derived Biodiesel Fuels, SwRI 7507, November 1996

Hess, Boehman, Tijm, Waller, Experimental Studies of the Impact of CETANER on Diesel Combustion and Emissions, SAE Technical Paper 2000-01-2886 Bertola, Boulouchos, Oxygenated Fuels for Particulate Emissions Reduction in Heavy-Duty Di-Diesel Engines with Common-Rail Fuel Injection SAE Technical Paper 2000-01-288

<sup>\*\*</sup> The cetane number for farnesene is low but it can be hyrogenated to farnesane such that the cetane number is 58 [c]

<sup>\*\*\*</sup> Cold flow properties improved by hydrogenation of farnesene to farnesane [c]

b) The Good Scents Company, http://www.thegoodscentscompany.com/data/rw1044061.html

c) Rude, Schirmer, New Microbial Fuels: A Biotech Perspective, Current Opinion in Microbiology, 2009, 12, 274-281

d) Bedoukian Research Inc, MSDS P3500-90, (e)-beta-farnesene, http://www.bedoukian.com/products/displayGraphic.asp?type=m&product=P3500-90, Aug. 3, 2007.

E.24. Sesquiterpene (Farnesene)--Complementary Information

Advantages Not soluble in water

### Disadvantages

Low cetane number Poor cold flow properties

references:

Bedoukian Research Inc, MSDS P3500-90, (e)-beta-farnesene, http://www.bedoukian.com/products/displayGraphic.asp?type=m&product=P3500-90, Aug. 3, 2007.

# **Gasoline Fuels** E.25. Green Gasoline--Properties

#### NO PUBLISHED DATA WAS FOUND FOR GREEN GASOLINE, BUT PERFORMANCE AND PROPERTIES ARE EXPECTED TO BE SIMILAR TO PETROLEUM DERIVED GASOLINE

#### Green Gasoline manufactured by upgrading pyrolysis oil is expected to be in production in 2014 (properties currently not published)

An announcement on January 12, 2010 on the Green Car Congress website:

"The US Department of Energy has selected UOP, a Honeywell company, for negotiation of a \$25 million award to build a demonstration unit in Hawaii to convert cellulosic biomass into renewable hydrocarbon transportation fuels. The demonstration unit will employ the RTP rapid thermal processing technology developed by Ensyn Corp. RTP rapidly heats biomass at ambient pressure to generate high yields of pourable, liquid pyrolysis oil. The pyrolysis oil— essentially a bio crude oil—will then be upgraded to green transport fuels using technology developed by UOP working with DOE, the DOE's National Renewable Energy Lab and Pacific Northwest National Laboratory (PNNL). The demonstration plant, which will be built at the Tesoro Corp. refinery in Kapolei, Hawaii, is expected to start up in 2014. In 2009, UOP and Ensyn Corp. launched a joint venture, Envergent Technologies, LLC, to offer technology and equipment to convert second-generation biomass into pyrolysis oil for power generation, heating fuel and for conversion into transportation fuels."

http://www.greencarcongress.com/2010/01/uop-rtp-20100112.html?utm\_source=feedburner&utm\_medium=feed&utm\_campaign=Feed%3A+greencarcongress%2FTrBK+%28Green+Car+Congress%29

From website of Envergent, which is a joint company by UOP and Ensyn (green diesel manufacturers) posted on January 25, 2010:

"UOP has been selected for negotiation of a \$25 million award from the U.S. Department of Energy (DOE) to build a demonstration-scale unit that will convert cellulosic biomass into green transportation fuels. It's a pilot test that will run as part of the DOE's effort to help reduce U.S. dependence on foreign oil, spur the creation of the domestic bio-industry and create new jobs.

The unit will include the RTP® rapid thermal processing technology to convert biomass to pyrolysis oil as well as a hydroprocessing unit to upgrade the pyrolysis oil to green transportation fuels – **primarily green gasoline.**" http://blog.envergenttech.com/

<b>Gasoline Fuels</b> E.26. Green GasolineCompatibility	y and Environmental Issues			
NO PUBLISHED DATA WAS FOUND FOR G	REEN GASOLINE, BUT COMPATIBILITY	AND ENVIRONMENTAL EFFECTS AF	RE EXPECTED TO BE SIMILAR TO I	PETROLEUM DERIVED GASOLINE

E.27. Fischer-Tropsch Fuel (FT)--Properties

From website of FT Diesel Manufacturer, CHOREN:

"Synthetic biofuel from CHOREN can at present only be used in diesel engines.

The light components generated in its production (naphtha) can be used in refineries as part of gasoline.

It is technically possible to produce pure fuel for gasoline engines, but it requires additional process stages and is not currently planned."

http://www.choren.com/en/faq/

Companies that produce FT gasoline from biomass were not found after an extensive literature search.

Information on companies which utilize the FT process in biomass to liquid production but do not produce gasoline can be found in the following references:

Hofer, R. Sustainable Solutions for Modern Economies, Royal Society of Chemistry, 2010.

See Chapter: Green Fuels - Sustainable Solutions for Transportation, pages 154-157.

Andrews, A. and Logan, J., "Fischer-Tropsch Fuels from Coal, Natural Gas, and Biomass: Background and Policy", CRS Report for Congress, 2008. See Section: Synthetic Fuel Plants, pages 7-15.

#### FT Gasoline derived from coal or natural gas produced by the South African Company, Sasol

Sasol FT gasoline properties published recently in 2009 article in journal, Energy & Fuels Properties

	Coal-derived	Natural Gas-derived	Conventional So. African
	FT Gasoline	FT Gasoline	<u>Gasoline</u>
density at 20 deg C (g/cm^3)	0.729	0.748	0.729
vapor pressure (kPa)	67	72	72
sulfur (ppm)	< 10	< 10	150
oxygen (mass %)	0.14		0.09
olefins (mass %)	30	8	~12
aromatics (total) (vol %)	29	37	27
octane	93	95	93

Reference: Kamara, Coetzee, Overview of High-Temperature Fischer-Tropsch Gasline and Diesel Quality, Energy & Fuels, 2009, 23, 2242-2247.

E.28. Fischer-Tropsch Fuel (FT)--Compatibility and Environmental Issues

### Advantages

Negligible sulfur content Some flexibility in adjusting certain fuel properties

### Disadvantages

Low octane

references: Kamara, Coetzee, Overview of High-Temperature Fischer-Tropsch Gasline and Diesel Quality, Energy & Fuels, 2009, 23, 2242-2247.

# E.29. Ethanol--Properties

<u>Properties</u>	F	F40	<b>500</b>	F.50	505	0 "	MEDS	
Molecular Formula Molecular Weight (g/mol) Elemental Composition (mass%)	Ethanol C2H5OH 46.07	<u>E10</u>	<u>E20</u>	<u>E50</u>	<u>E85</u>	Gasoline C4 to C12 100-105	<u>MTBE</u> C5H12O 88.15	<u>Comments</u>
Carbon Hydrogen Oxygen Density (g/cm3) at 15deg C Reid vapor pressure (psi) Boiling Point (degC)	52.2 13.1 34.7 0.794 [b] 2 78	0.737 [b] 10.5	0.744 [b] 10.3	0.763 [b] 9	56-58 13-14 29-30 0.786 [b] 5 49-80	85-88 12-15 0-4 0.733 [b] 11 27-225	68 14 18 0.7404 33 55.2	
Flash Point (degC) Pour Point (degC) Cloud Point	13				slightly higher than gasoline		-25	Higher flashpoint
Freezing Point (degC) High Heating Value (MJ/L) Low Heating Value (MJ/L) Water Solubility and Colored	-114 24 20 [b]	32 [b]	30 [b]	27 [b]	23 [b]	-40 35 33 [b]	51260	Lower energy content
Water Solubility at 21 degC Water in fuel (Vol%) Fuel Miscibility Solvation Potential	100				100	Negligible	51260	
Flammability Limits (Vol%) Lower Higher	4.3 19				Wider than gasoline	1.4 7.6	1.6 8.4	
Acid Number Research Octane Number Viscosity (mPa-s) at 20 degC Lubricity (um)	116 [b] 1.19	95 [b]	98 [b]	102 [b]	107 [b] 1.07-1.08	88 [b] 0.37-0.44		Higher octane
Toxicity Acute: Mouse oral LD50 (mg/kg) Acute: Mouse Inhalation LD50 (ppm)	8300 [e]					101200 [c]	1600-3900	
Acute:LC50 for freshwater fish (trout) (mg/L) Acute:LC50 for aquatic invertebrate (daphnia) (vol%) Acute:Aquatic plants - No observable effect concentration (mg/L) Chronic: Rat oral No observable effect conc. (mass% in food) Teratogenicity: Rat inhalation No observable effect conc. (ppm)	11200 [e] 1.5[e] < 500 [e] < 5 [e] 25% [e]					9000 [c]	> 100 mg/L	
Partition coefficient (Kow) Log Kow at 25 degC Bioconcentration factor (L/kg) Transport between Environmental Compartments Air, water, soil, sediment (% mass distribution)	octanol-water -0.31 [e] Low based on Kow 13, 44.8, 42.1,0.039 [e]					octanol-water 2.13 to 4.85 [c]	octanol-water 1.24 < 2	
Half-life in water at typical env. conditions Half-life in atmosphere Photodegradation half-life in air	6 days [d] 15.4 hrs [e]					0.8 to 16 days [c]	streams 2.5 hr, rivers 9.5 hr, lakes 137 days 3-6 days	
Biodegradation in water/sediment for 30 days Appearance Odor Threshold (mg/L) CAS number	91% [e] clear liquid [c] 0.1 air, 100 water [d] 64-17-5					Readily in aerobic cond. [c] clear to amber [c]	Slower than aromatic hydrocarbons [b] clear, water-like liquid [a] Detectable 0.05, Recognizable 0.13 [a]	
references:	Bechtold, Richard L., Alternative Fuels Guidebook: Properties, Storage, Dispensing, and Vehicle Facility Modifications, SAE Order Number R-180, 1997 a) NIST Chemistry WebBook b) Bailey, Russel SAE Technical Paper 81044 c) Fisher Scientific MSDS, http://fiscimage.fishersci.com/msds/89308.htm, March 2003 d) Spectrum Chemical Fact Sheet, http://www.speclab.com/compound/c64175.htm e) US EPA High Production Volume Information System, Ethanol Detailed Chemical Results, http://iaspub.epa.gov/oppthpv/quicksearch.display?pChem=100220							
references (MTBE)	EPA Chemical Fact Sheet, http://www.epa.gov/opptintr/chemfact/s_mtbe.txt a) Amerada Hess Corporation, Material Safety Data Sheet No. 9922, Methyl tert-Butyl Ether (MTBE), April 1998 b) EPA, Summary of Workshop on Biodegradation of MTBE, February 2001, http://www.epa.gov/nrmrl/pubs/625r01001/625r01001.pdf c) JT Baker MSDS, Gasoline, 10/14/2008, http://www.docs.citgo.com/msds_pi/UNLEAD.pdf							
Conversion Factors Bailey and Russel LHV in BTU/lb								
1900 1830 1750 1550 1300 1170	0 31.83233384   0 30.44075641   0 26.96181282   0 22.61313333	MJ/L MJ/L MJ/L MJ/L	E0 E10 E20 E50 E85 E100					

### E.30. Ethanol--Compatibility and Environmental Issues

#### Incompatible Materials

 elastomers
 metals

 cork gasket material
 lead

 natural rubbers
 aluminum

 polyurethane
 brass

 PVC
 terne

 zinc

lead-based solder

#### **Compatible Materials**

<u>elastomers</u> <u>metals</u>
thermoset-reinforced fiberglass carbon steel
thermoplastic stainless steel
Buna N bronze

neoprene Viton Teflon nitrile polypropylene

#### **Vehicle Compatibility**

Incompatible with terne-coated steel, commonly used for fuel tanks, especially in older vehicles Hoses constructed from natural rubbers must be replaced with Viton, nitrile, etc. Low freezing point, suitable for use in cold climates

#### Advantages

Can be blended with gasoline in any combination Requires little modification for use in exisitng engines

#### Disadvantages

Cleaning Effect Miscible with water

#### Trasnporting Precautions

Vessels must be cleaned out to prevent contamination due to water and cleaning effect

#### Environmental/Health concerns

Toxic

Flammable

#### Compatibility/Fungibility issues

Miscible with water

Cleaning effect leads to deposits and plugged filters both in transport and in engines Transport by rail: requires additional private track or existing gasoline transport tracks Stress corrosion cracking observed in pipelines due to ethanol

#### **Current production**

2007 US ethanol production: 6.48 billion gallons 2007 US ethanol production capacity: 7.5 billion gallons 2008 projected US ethanol production capacity: 13.3 billion gallons

references: Biofuels Digest, "US Ethanol Production Capacity to Increase to 13.3 Billion Gallons in 2008", www.biofuelsdigest.com, 1/9/2008

Biofuels Journal, "Annual and Monthly US Ethanol Production", www.biofuelsjournal.com, 12/5/2006

Department of Energy, "Handbook for Handling, Storing, and Dispensing E85", 7/2006

Pipeline Research Council International, "Stress Corrosion Cracking", 7/2006

Columbia Engineered Rubber, Inc., www.columbiaerd.com, 2010

Alvarado, Peter J., "Steel vs. Plastics: The Competition for Light-Vehicle Fuel Tanks", JOM 48 (7) pp. 22-25, 1996

### E.31. BioButanol--Properties

Propertie	<u>s</u>
Molecular	F

Properties			
	1-Butanol	<u>Isobutanol</u>	Gasoline <u>Comments</u>
Molecular Formula	C4H9OH	C4H9OH	C4 to C12
Molecular Weight (g/mol)	74.12	74.12	100-105
Elemental Composition (mass%)			
Carbon	16.2	16.2	85-88
Hydrogen	13.5	13.5	12-15
Oxygen	21.6	21.6	0-4
Density (g/cm3) at 15deg C	0.81	0.801	0.69-0.79
Vapor Pressure (kPa)	18.6 [j]	1.07	48-103 at 38C
Boiling Point (degC)	117.7	108	27-225
Flash Point (degC)	28.9	28	-43 Higher flashpoint
Freezing Point (degC)	-90 [c]	-108	-40
High Heating Value (MJ/L)	37.3 [h]	.00	35
Low Heating Value (MJ/L)	34.4 [h]		30-33
Water Solubility at 21 degC: Water in fuel (mg/L)	76700 [b]		Negligible
Fuel Miscibility	Complete [g]		regiigible
Dielectric constant ( > 15 indicates polar solvent)	17.8 [f]		
Flammability Limits (Vol%)	17.0 [1]		
Lower	1.4	1.7	1.4
Higher	11.2	10.6	7.6
Research Octane Number		10.6	7.6 88-100
	113 [e]		
Viscosity (mPa-s) at 20 degC	3 [d]	4	0.37-0.44
Toxicity	4000 5 3		
Acute: Rat oral LD50 (mg/kg)	4360 [b]	2460	
Acute: Rat Inhalation LD50 (ppm)		8000	101200 [a]
Acute:LC50 for freshwater fish (ppm)	1000 [b]		
Acute:Half max effective concentration for aquatic invertebrate (ppm)	1880 [b]		
Acute:Aquatic plants - Half max effective concentration (ppm)	500 [b]		
Chronic: Rat inhalation No observable effect conc. (mg/kg)	125 [b]		
Teratogenicity: Rat inhalation No observable effect conc. (ppm)	6000 [b]		9000 [a]
Partition coefficient (Kow)	octanol-water		octanol-water
Log Kow at 25 degC	0.84 [b]		2.13 to 4.85 [a]
Bioconcentration factor (L/kg)	< 3 (estimated) [c]		
Transport between Environmental Compartments			
Air/Soil	Slow to moderate volatilization [c]		
Water/Soil	May adsorb to clay, but leaches into water [c]		
Photodegradation half-life in air	2.2 days [c]		
Biodegradation in soil in 20 days	67% [c]		
Biodegradation in water in 24 hrs (Chemical oxygen demand method)	82% [c]		0.8 to 16 days [a]
Appearance	clear liquid		Readily in aerobic cond. [a]
Odor	Wine-like [c]		clear to amber [a]
Odor Threshold (ppm)	7.1 ppm (in water); 0.83 ppm (in air) [c]	1.6 ppm	6.1
Odor of incomplete combustion product, butyric acid	extremely strong and unpleasant [i]	• •	
CAS number	71-36-3	78-83-1	

#### references (butanol):

Science Lab MSDS, 1-Butanol, http://www.sciencelab.com/xMSDS-1\_Butanol-9927115, Nov. 6, 2008

- a) Argonne National Laboratory, Biobutanol Properties, http://www.greencarcongress.com/2008/08/argonne-investi.html
- b) US EPA High Production Volume Information System, Butanol Detailed Chemical Results, http://iaspub.epa.gov/oppthpv/quicksearch.display?pChem=101066
- c) EPA Chemical Fact Sheet, 1-Butanol, http://www.epa.gov/chemfact/s\_butano.txt
- d) California Air Resources Board Solvents Database, Butanol, http://www.arb.ca.gov/db/solvents/solvent\_pages/alcohols-html/butanol.htm
- e) Alasfour, Butanol A Single Cylinder Engine Study: Engine Performance, International Journal of Energy Research, 1997, 21, 21-30.
- f) American Chemical Society, Organic Chemistry Division, Common Organic Solvents Table of Properties, http://organicdivision.org/organic\_solvents.html
- g) Mariano, Tomasella, Martino, Filho, Seleghim, Contiero, deFranceschi de Angeles, Aerobic Biodegradation of Butanol and Gasoline Blends Biomass and Bioenergy, 2009, 33, 1175-1181.
- h) Pacific Northwest National Laboratory, Hydrogen Analysis Resource
- http://hydrogen.pnl.gov/filedownloads/hydrogen/datasheets/lower\_and\_higher\_heating\_values.xls
- i) University of California, Low Carbon Fuel Standard-Final Report 1, http://www.energy.ca.gov/low\_carbon\_fuel\_standard/UC\_LCFS\_study\_Part\_1-FINAL.pdf
- j) Gautam, Martin, Combustion Characteristics of Higher Alchohol/Gasoline Blends, Proceedings of the Institution of Mechanical Engineers; Part A; Journal of Power and Energy, 2000, vol. 214, pg. 497.

#### references (gasoline):

Alternative Fuels Guidebook: Properties, Storage, Dispensing, and Vehicle Facility Modifications SAE Order Number R-180, 1997

Richard L. Bechtold

a) JT Baker MSDS, Gasoline, 10/14/2008, http://www.docs.citgo.com/msds\_pi/UNLEAD.pdf

E.32. BioButanol--Compatibility and Environmental Issues

### **Incompatible Materials**

<u>elastomers</u> <u>metals</u>

aluminum copper

### **Compatible Materials**

<u>elastomers</u> <u>metals</u>

steel

### **Advantages**

Can be run in existing gasoline engines as blend or pure with little or no modification Biodegrades easily in soil and water Energy content closer to gasoline than ethanol according to BP "can be transported through pipelines...can be blended at refineries" "a commercial fuels trial confimed the compatibility of butanol with existing fuel infrastructure"

### **Disadvantages**

Highly flammable miscible with water

#### **Environmental/Health concerns**

Biodegrades easily in soil and water Flammable

### Compatibility/Fungibility issues

Miscible with water

Requires private track for transport by rail

Can be run in existing gasoline engines as blend or pure with little or no modification

references: Acros Organics, "1-Butanol Material Data Safety Sheet", www.acros.com, 12/09

BP, "Biobutanol Fact Sheet", www.bp.com, 2009

### E.33. Methanol--Properties

<u>Properties</u>	Methanol	M85	Gasoline	Comments
Molecular Formula	CH3OH	<u>IVIOS</u>	C4 to C12	Comments
Molecular Weight (g/mol)	32.04		100-105	
Elemental Composition (mass%)				
Carbon	37.5	43-45	85-88	
Hydrogen	12.6	40160.0	12-15	
Oxygen	49.9	43-44	0-4	
Density (g/cm3) at 15deg C	0.796	0.79-0.80	0.69-0.79	
Vapor Pressure at 38 degC (kPa)	32	48-103	48-103	
Boiling Point (degC)	65	49-66	27-225	
Flash Point (degC)	11	slightly higher than gasoline	-43	Higher flashpoint
Pour Point (degC)		0,0		,
Cloud Point				
Freezing Point (degC)	-97.5		-40	
High Heating Value (MJ/L)	18 [a]		35	
Low Heating Value (MJ/L)	15.8	17.9-18.3	30-33	Lower energy content
Water Solubility at 21 degC				
Water in fuel (Vol%)	100	100	Negligible	
Fuel Miscibility				
Solvation Potential				
Flammability Limits (Vol%)				
Lower	7.3	wider than	1.4	
Higher	36	gasoline	7.6	
Acid Number				
Research Octane Number	109	108	88-100	
Viscosity (mPa-s) at 20 degC	0.57 [d]	1.07-1.08	0.37-0.44	
Lubricity (um)				
Toxicity				
Acute: Mouse oral LD50 (mg/kg)	5628 [b]			
Acute: Mouse Inhalation LD50 (ppm)			101200 [a]	
Acute:LC50 for freshwater fish (Lepomis macrochirus) (mg/L)	15400 [b]			
Acute:Half max effective concentration for aquatic invertebrate (daphnia) (mg/L)	10000 [b]			
Acute:Aquatic plants - Half max effective concentration (mg/L)	28440 [b]			
Chronic: Rat inhalation Lowest observable effect conc. (ppm)	5000 [b]			
Teratogenicity: Rat inhalation Lowest (Gaso:No) observable effect conc. (ppm)	2000 [b]		9000 [a]	
Partition coefficient (Kow)	octanol-water		octanol-water	
Log Kow at 25 degC	-0.77 [b]		2.13 to 4.85 [a]	
Bioconcentration factor (L/kg)	Low based on Kow			
Transport between Environmental Compartments				
Soil/Water Environment - low organic carbon in soil	Preferentially in water [b]			
Soil/Water Environment - 10% organic carbon in soil	Equal amounts in soil & water [b]			
Half-life in water at typical env. conditions	2.6 days to volatilize from a pond [b]			
Half-life in atmosphere	47.0 1 11.1		0.01-10.1	
Photodegradation half-life in air	17.8 days [b]		0.8 to 16 days [a]	
Biodegradation in activated sludge for 6 days	80% [b]		Readily in aerobic cond. [a]	
Appearance	clear liquid		clear to amber [a]	
Odor Threshold (ppm) CAS number	160 detectable, 690 recognizable [c] 67-56-1			
CAO HUHIDEI	1-00-10			

Alternative Fuels Guidebook: Properties, Storage, Dispensing, and Vehicle Facility Modifications References: Gasoline

SAE Order Number R-180, 1997

Richard L. Bechtold

a) JT Baker MSDS, Gasoline, 10/14/2008, http://www.docs.citgo.com/msds\_pi/UNLEAD.pdf

References: a) NIST Chemistry WebBook

Methanol b) US EPA High Production Volume Information System, Methanol Detailed Chemical Results, http://iaspub.epa.gov/oppthpv/quicksearch.display?pChem=100296

c) Methanex MSDS, Methanol, http://www.methanex.com/products/documents/MSDS\_USenglish.pdf, Oct. 13, 2005

d) Assael and Polimatidou, Measurements of the Viscosity of Alcohols in the Temperature Range 290-340 K at Pressures up to 30 Mpa, International Journal of Thermophysics, 1994, 15, 95-107.

c) Ren, Huang, Miao, Jiang, Liu, Wang, Effect of the Addition of Diglyme in Diesel Fuel on Combustion and Emissions in a Compression-Ignition Engine, Energy and Fuels, 2007, 21, 2573-2583.

E.34. Methanol--Compatibility and Environmental Issues

### **Incompatible Materials**

<u>elastomers</u> <u>metals</u>

lead magnesium platinum

oxidizing materials

#### **Compatible Materials**

elastomers

<u>metals</u>

mild steel

neoprene

ethylene propylene

Teflon

nitrile

natural rubber

#### **Vehicle Compatibility**

Incompatible with terne-coated steel, commonly used for fuel tanks in older vehicles Compatible with nitrile and natural rubber, commonly used for hoses Low freezing point, suitable for use in cold climates

#### Advantages

Can be converted to hydrogen at relatively low temps Widely distributed currently Biodegrades easily in soil and water

### Disadvantages

Highly flammable Miscible in water

Existing engines would require modification

#### Environmental/Health concerns

Biodegrades easily in soil and water

Flammable

Short term harmful effects on aquatic life in spill zone

#### Compatibility/Fungibility issues

Miscible with water

Requires private track for transport by rail Engine modification required for use in engines

### **Current production**

2004 US methanol production capacity: 2.6 billion gallons

references: Methanex, "Technical Information and Safe Handling Guide for Methanol: Version 3.0", 9/2006

Sax and Lewis, "Dangerous Properties of Industrial Materials: 9th Ed.", 1995

"Hawley's Condensed Chemical Dictionary: 11th Ed.", 1987

Institute for the Analysis of Global Security, "Sources of Methanol", www.iags.org, 2004

Columbia Engineered Rubber, Inc., www.columbiaerd.com, 2010

Alvarado, Peter J., "Steel vs. Plastics: The Competition for Light-Vehicle Fuel Tanks", JOM 48 (7) pp. 22-25, 1996

# E.35. Propanol--Properties

<u>Properties</u>			
	1-Propanol	Gasoline	Comments
Molecular Formula	C3H8O	C4 to C12	
Molecular Weight (g/mol)	60.095	100-105	
Elemental Composition (mass%) Carbon	59.96	85-88	
Hydrogen	13.42	12-15	
Oxygen	26.62	0-4	
Density (g/cm3)	0.8 at 25 deg C	0.69-0.79 at 15 deg C	
Reid Vapor Pressure (kPa)	9.0 at 25 deg C	48-103 at 38 deg C	
Boiling Point (degC)	82.2	27-225	
Flash Point (degC)	23	-43	Higher flashpoint
Pour Point (degC)			
Cloud Point			
Freezing Point (degC)	-126.1	-40	
High Heating Value (MJ/L)	27 [f]	35	
Low Heating Value (MJ/L)	24 [d]	30-33	Lower energy content
Water Solubility at 21 degC Water in fuel (Vol%)	100	Negligible	
Fuel Miscibility	100	Negligible	
Solvation Potential			
Flammability Limits (Vol%)			
Lower	2.2 [b]	1.4	
Higher	13.7 [b]	7.6	
Acid Number			
Research Octane Number	112 [a]	88-100	
Viscosity (mPa-s) at 25 degC	1.94	0.37-0.44	
Lubricity (um)			
Toxicity	4070 [-]		
Acute: Rat oral LD50 (mg/kg) Acute: Mouse Inhalation LD50 (ppm)	1870 [c] 18 [c]	101200 [a]	
Acute: Mouse initiation LD50 (ppm) Acute: Rabbit eye irritation (mg)	4 [c]	101200 [aj	
Acute: Rabbit dermal (mg)	580 [c]		
Acute:LC50 for fish 96-hour values(ppm)	0.3 to 3 [c]	2 to 8 [a]	
Acute:Half max effective concentration for aquatic invertebrate (daphnia) (mg/L)	0.0 to 0 [0]	2 10 0 [4]	
Acute:Aquatic plants - Half max effective concentration (mg/L)			
Chronic: Rat inhalation Lowest observable effect conc. (ppm)			
Teratogenicity: Rat inhalation No observable effect conc. (ppm)		9000 [a]	
Partition coefficient (Kow)	octanol-water	octanol-water	
Log Kow at 25 degC	0.32 [e]	2.13 to 4.85 [a]	
Bioconcentration factor (L/kg)	0.7 [e]		
Transport between Environmental Compartments Soil/Air	Evaporates [e]		
Soil/Water	Can leach into groundwater [c]		
Air/Water	Evaporates [e]		
Half-life in water at typical env. conditions	2.6 days to volatilize from a pond [b]		
Half-life in atmosphere	short-lived: reaction with hydroxyl [e]		
Photodegradation half-life in air	,,-[-]	0.8 to 16 days [a]	
Biodegradation	Readily biodegradable [e]	Readily in aerobic cond. [a]	
Appearance	clear liquid	clear to amber [a]	
Odor Threshold (ppm)	0.13 recognizable [b]		
CAS number	71-23-8		
references:	California Air Resources Board, Solven	nts Database 1-propagol http	o://www.arb.ca.gov/db/solvents/solvent_pages/Alcohols-HTML/propanol.htm
1-propanol			Sasoline Blends, Proceedings of the Institution of Mechanical Engineers; Part A; Journal of Power and Energy, 2000, vol. 214, pg. 497.
, FE			ds.nsf/MSDSNo/71-23-8?OpenDocument
	c) JT Baker MSDS, 1-Propanol, http://v		
			Fluid Bed Liquid Incinerator, Chemical Engineering Science, 1991, Vol. 46, pp. 2983-2996.
			ll, http://www.inchem.org/documents/ehc/ehc102.htm#SectionNumber:1.3
	f) Chao, Rossini, Heats of Combustion,	, Formation, and Isomerization	n of Nineteen Alkanols, Journal of Chemical Engineering Data, 1965, Vol. 10, pp. 374-379.
references	Alternative Evels Cuideback Berneti	a Ctaraga Diananaina	Valido Cosility Madifications
references: gasoline	Alternative Fuels Guidebook: Propertie SAE Order Number R-180, 1997	s, Storage, Dispensing, and \	verticle raciity intodifications
gasoniro	Richard L. Bechtold		
	a) JT Baker MSDS, Gasoline, 10/14/20	008. http://www.docs.citao.com	m/msds pi/LINLEAD.pdf
	_,		

E.36. Propanol--Compatibility and Environmental Issues

### **Incompatible Materials**

<u>elastomers</u> <u>metals</u>

alkali metals

### **Compatible Materials**

<u>elastomers</u> <u>metals</u>

steel

### Advantages

Biodegrades easily

### Disadvantages

Highly flammable

### **Environmental/Health concerns**

Biodegrades easily in soil and water Flammable

### Compatibility/Fungibility issues

Requires private track for transport by rail

references: Cameo Chemicals, "n-Propanol Chemical Data Sheet", www.cameochemicals.noaa.gov, 12/09

Dow Chemicals, "Dow n-Propanol Product Safety Assessment", www.dow.com, 6/18/09

### E.37. Higher Carbon Alcohols--Properties

Higher carbon alcohols have greater energy density, lower miscibility with water, and lower vapor pressure than lower carbon alcohols like ethanol and methanol. [a] Recent developments by Atsumi, Hanai, Liao (2008) enabled biosynthesis of branched higher alcohols (in table below) which are not natural fermenation products. [b] 2-methyl-1butanol and 3-methyl-1-butanol may be superior fuels to both ethanol and n-butanol. [c]

- a) Kreame, N., Gross, C., Univeristy of Minnesota Biofuels Database, Branched Chain Alcohol Pathway, https://www.biofuelsdatabase.org/wiki/index.php5/Branched-Chain\_Alcohol\_Pathway
- b) Atsumi, S., Hanai, T., Liao, J. C. (2008) Non-fermentative Pathways for Synthesis of Branched-Chain Higher Alcohols as Biofuels, Nature, Vol. 451, doi:10.1038/nature06450. c) Wackett, L.P. (2010) Biofuels (Butanol-Ethanol Production), page 2805, In: Handbook of Hydrocarbon and Lipid Microbiology, Editor: K. N. Timmis, Springer.

<u>Properties</u>				
	2-methyl-1-butanol	3-methyl-1-butanol	<u>Gasoline</u>	
Molecular Formula	C5H12O	C5H12O	C4 to C12	
Molecular Weight (g/mol)	88.15	88.15	100-105	
Elemental Composition (mass%)				
Carbon	13.72	13.72	85-88	
Hydrogen	68.13	68.13	12-15	
Oxygen	18.15	18.15	0-4	
Density (g/cm3)	0.815	0.8	0.69-0.79 at 15 deg C	
Vapor Pressure (kPa) Boiling Point (degC)	0.4 130	0.32	48-103 at 38 deg C 27-225	
Flash Point (degC)	43	43	-43	
Pour Point (degC)	43	43	-43	
Cloud Point				
Freezing Point (degC)	-70	-117	-40	
High Heating Value (MJ/L)	30.75 [a]	30.18 [a]	35	
Low Heating Value (MJ/L)			30-33	
Water Solubility				
Water in fuel (grams per 100 ml water)	3.6	2	Negligible	
Fuel Miscibility				
Solvation Potential				
Flammability Limits (Vol%)				
Lower	1.1	1.2	1.4	
Higher	9.3	9	7.6	
Acid Number				
Research Octane Number			88-100	
Viscosity (mPa-s) at 20 degC	5.1	4.37	0.37-0.44	
Lubricity (um)				
Toxicity				
Acute: Rat oral LD50 (mg/kg)		1300	404000 [-]	
Acute: Mouse Inhalation LD50 (ppm) Acute: Rabbit eye irritation (mg)		20	101200 [a]	
Acute: Rabbit eye imation (mg) Acute: Rabbit dermal LD50 (mL/kg)	3.54	3.97		
Acute: Rabbit dermar ED50 (mD/kg) Acute:Lethal for fish 82-hour values (ppm)	3.04	100		
Acute:Half max effective concentration for aquatic invertebrate (daphnia) (mg/L)		100		
Acute: Aquatic plants - Half max effective concentration (mg/L)				
Chronic: Rat inhalation Lowest observable effect conc. (ppm)				
Teratogenicity: Rat inhalation No observable effect conc. (ppm)			9000 [a]	
Partition coefficient (Kow)			octanol-water	
Log Kow at 25 degC			2.13 to 4.85 [a]	
Bioconcentration factor (L/kg)		Not expected to bioconcentrate	• • • • • • • • • • • • • • • • • • • •	
Transport between Environmental Compartments		•		
Soil/Air				
Soil/Water		Leaches into groundwater		
Air/Water		Volatilizes		
Half-life in water at typical env. conditions				
Half-life in atmosphere				
Photodegradation half-life in air		Rapid	0.8 to 16 days [a]	
Biodegradation	Clear, colorless, liquid	Readily biodegrades Clear, colorless, liquid	Readily in aerobic cond. [a]	
Appearance Odor	Stench		clear to amber [a]	
Odor Threshold (ppm)	Stench	Disagreeable		
CAS number	137-32-6	123-51-3		
C// O Hamber	101 02 0	120 01 0		
references:				
2-methyl-1-butanol	Fisher Scientific MSDS,	DL-2-Methyl-1Butanol, 98%, 11/2	20/2008, https://fscimage.fishersci.com/msds/52450.htm	
	<ul> <li>a) Chao, Rossini, Heats</li> </ul>	of Combustion, Formation, and I	Isomerization of Nineteen Alkanols, Journal of Chemical Engineering Data, 1965, Vol. 10, pp. 374-37	79.
references:				
3-methyl-1-butanol			https://fscimage.fishersci.com/msds/00798.htm	
	<ul> <li>a) Chao, Rossini, Heats</li> </ul>	of Combustion, Formation, and I	Isomerization of Nineteen Alkanols, Journal of Chemical Engineering Data, 1965, Vol. 10, pp. 374-37	9.
	Alternative Freds C 111		A STATE OF THE STA	
references:			nsing, and Vehicle Facility Modifications	
gasoline	SAE Order Number R-1 Richard L. Bechtold	00, 199/		
		coline 10/14/2008 http://www.do	cs.citgo.com/msds_pi/UNLEAD.pdf	
	a, JI Dakel NODO, Gas	omie, 10/14/2006, http://www.do	ca.citgo.com/mada_pi/UNLEAD.pui	

E.38. Higher Carbon Alcohols--Compatibility and Environmental Issues

# Advantages

Low freezing point

### Disadvantages

Moderate flammability
Moderate toxicity
High oxygen content
Low vapor pressure
Somewhat soluble in water

references:

Fisher Scientific MSDS, DL-2-Methyl-1Butanol, 98%, 11/20/2008, https://fscimage.fishersci.com/msds/52450.htm Fisher Scientific MSDS, 3-Methyl-1Butanol, 9/30/2002, https://fscimage.fishersci.com/msds/00798.htm

### E.39. Pyrolysis Oil--Properties

<u>Properties</u>	NREL Oil *	Ensyn Oil**	MFR Specifications***	Fast Pyrolysis Bio-oil	Hydrothermal <u>Bio-oil</u>	Heavy Petroleum Fuel	
Molecular Formula							
Molecular Weight (g/mol)	370	550					
Elemental Composition (mass%)							
Carbon	58.25	57.95		39.5 - 55.8	72.6 - 74.8	85.2	
Hydrogen	7.4	7.23		7.5 - 6.1	8.0	11.1	
Oxygen	32.83	33.19		37.9 - 52.6			
Nitrogen	1.52	1.64		< 0.1	< 0.1	0.3	
Sulfur	1.2	1.22		< 0.05	< 0.05	2.3	Lower sulfur content
Density (g/cm3)				1.23	1.1	0.94	
Vapor Pressure kPa							
Boiling Point (degC)							
Flash Point (degC)		55 [a]					
Pour Point (degC)		-25 [a]					
Cloud Point (degC)							
High Heating Value (MJ/kg)		17.6 [a]	min. 18 [a]	16.5 - 17.5		40	Lower energy content
Low Heating Value (MJ/kg)	17	16.3	min. 16 [a]				•
Water Content (mass%)	16.9	26.3	max. 26 [a]	15 - 25	3 - 5	0.1	
Water Solubility at 21 degC							
Water in fuel (ppm)							
Fuel Miscibility							
Solvation Potential							
Flammability Limits (Vol%)							
Lower							
Higher							
pH		2.5					
Cetane Number							
Viscosity (mPa-s)		59 [a]		10 - 150 at 50 degC	3000 - 17000 at 60 degC	180 at 50 degC	Lower viscosity
Lubricity (um)					3.		,
* National Renewable Energy Laboratory wood-derived	d flash pyrolysis oil produced by ablative y	ortex reactor					

<sup>\*</sup> National Renewable Energy Laboratory wood-derived flash pyrolysis oil produced by ablative vortex reactor
\*\* Ensyn Corporation wood-derived flash pyrolysis oil produced in a tubular transport reactor

#### Information below for various pyrolysis oils: not only NREL Oil

- 1	OXI	CIL	y	
			۸	

Acute: Animal Aerosol Inhalation LD50 (mg/m3)	3100 [b]
Acute: Rabbit Dermal No observable effect concentration (mg/kg)	2000 [b]
Acute: Rabbit Eye Corneal Damage (mL)	0.1 [b]
Acute: Oral (mg/kg)	700 [b]

Acute:Fish LC50 and bacteria EC50 (mg/L)

Chronic: Rat and Mouse oral (mg/m3)

Mutagenicity

Partition coefficient (Kow)

Log Kow at 25 degC Bioconcentration factor (L/kg) [j]

Soil adsorption Half-life in water at typical env. conditions

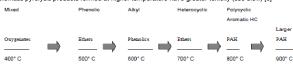
Half-life in atmosphere

Biodegradation: Aerobic in freshwater, 28 days

41% - 50% [d] Appearance Strong Smoky [c] Odor

Odor threshold (mg/m3) Odor threshold (ppm)

Biomass pyrolysis products formed at higher temperature have greater toxicity (see blow) [c]



#### References:

NREL oil, Ensyn oil, and MFR specifications

Shihadeh, Hochgreb, Energy and Fuels, 2002, 16, 552-561.

Conflicting studies [b]

- a) Oasmaa, Peacocke, Gust, Meier, McLellan, Norms and Standards for Pyrolysis Liquids. End-User Requirements and Specifications, Energy and Fuels C, http://www.combio-project.com/download/PDF/COMBIO\_WP2\_specification.pdf
- b) Diebold, A review of the toxicity of biomass pyrolysis liquids formed at low temperatures. National Renewable Energy Laboratory, NREL/TP-430-22739, 1997.
- c) Ringer, Putsche, Scahill, Large-Scale Pyrolysis Oil Production: A Technology Assessment and Economic Analysis, National Renewable Energy Laboratory, NREL/TP-510-37779, November 2006. d) Blin, Volle, Girard, Bridgwater, Meier, Biodegradability of biomass pyrolysis oils: Comparison to conventional petroleum fuels and alternatives fuels in current use, 2007, Fuel, 86, 2679-2686

<sup>\*\*\*</sup> Manufacturer Specifications Set by Ensyn (US/Canada), Wartsila (Finland), and Birka (Sweden) in the 1990s [a]

E.40. Pyrolysis Oil--Compatibility and Environmental Issues

#### **Incompatible Materials**

<u>elastomers</u> <u>metals</u>

aluminum mild steel nickel

impure copper

#### **Compatible Materials**

<u>elastomers</u> <u>metals</u>

polyethylene stainless steel

polypropylene cobalt polyester resins brass

### Advantages

Biodegrades quickly

Less toxic than petroleum fuels

#### Disadvantages

corrosive

high viscosity

instability

temperature sensitivity

high char and solids content

contains alkali metals, leading to deposits in filters, boilers, engines, etc.

suspended char particles can contribute to phase separation

#### **Environmental/Health Concerns**

Biodegrades quickly

Less toxic than petroleum fuels

#### Compatibility/Fungibility Issues

Generally not soluble in water

Can phase separate

High oxygen content leads to polarity, can cling to pipe/vessel walls

references: Hydroprocessing of Pyrolysis Bio-oil to Fuels and Chemicals, Bioenergy & Wood Products, Smallwood, May 14, 2008, http://www.forestprod.org/smallwood08powerpoints.html

Qiang, Lu, Wen-Zhi, Li, Xi-Feng, Zhu, Overview of Fuel Properties of Biomass Fast Pyrolysis Oils, Journal of Energy Conversion and Management vol 50, 2009

Cirad-Foret, "MSDS: Bio-Oil", 5/06

### E.41. Syngas--Properties

<u>Properties</u>				
	FERCO*	Coal-derived	Landfill	Typical
	Bio-Syngas	<u>Syngas</u>	<u>Gas</u>	Natural Gas
Molecular Formula				
Molecular Weight (g/mol)				
Gas Composition				
Hydrogen Molecule	26.2	45		Trace
Carbon Monoxide	38.2	49		
Carbon Dioxide	15.1	2.9	37.5	0.7
Nitrogen Molecule	2	2.2	7	1.3
Methane	14.9	0.9	54.5	95.2
Gaseous Compounds with more than two Carbon Atoms	4			3.6
Density (g/cm3)				0.58
Vapor Pressure kPa at 38 degC				
Boiling Point				
Flash Point (degC)				
Wobbe Index (BTU/scf)	499 [a]	450	639	1367 [a]
High Heating Value (MJ/m^3)	16.30			37.8
Low Heating Value (MJ/m^3)				
Water Solubility at 21 degC				
Water in fuel (%mass)				
Water content in fuel (mg/m^3)				16 to 32
Fuel Miscibility				
Solvation Potential				
Flammability Limits (Vol%)				4 to 16
Lower	4 [b]			
Higher	75 [b]			
Acid Number				
Cetane Number				
Viscosity (mPa-s)				
Kinematic viscosity (mm^2/s)				

#### Toxicity based on Carbon Monoxide Content [b]

i	Table of the effects of	of carbon monoxide on health and life
	Concentration in ppm	Consequences
	50	Limit of tolerance for long exposure
,	50 to 100	After some days ,chronic poisoning
1	200	Subacute poisoning
1	1000-1500	Headache,nausea, poisoning and fatal in case of prolonged
		exposure (more than 30 minutes)
1	2500	Rapid collapse , death in one or two hours
1	3760	LC50, one hour exposure
1	5000	Massive poisoning , death in less than one hour
1	10000	Death in 10 to 15 minutes
1	50000	Instantaneous poisoning , immediately fatal

Appearance

Odor

Odor threshold (mg/m3)

Odor threshold (ppm)

\*Future Energy Resources Company (FERCO), 950 E. Paces Ferry Road, NE, Suite 810, Atlanta, GA 30326

References: FERCO Bio-syngas Richard L. Bain, An Introduction to Biomass Thermochemical Conversion, DOE/NASLUGC Biomass and Solar Energy Workshops, August 3-4, 2004.

a) Paisley, Farris, Black, Irving, Overend, Preliminary Operating Results from the Battelle/FERCO Gasification Demonstration Plant in Burlington, Vermont, U.S.A., http://www.silvagas.com/downloads/seville.pdf

b) European Industrial Gases Association, Carbon Monoxide and Syngas Pipeline Systems, IGC Doc 120/04/E,

References: Natural Gas Union Gas Limited, Chemical Composition of Natural Gas, http://www.uniongas.com/aboutus/aboutng/composition.asp, February 2010.

a) Ferguson, Straub, Richards, Robey, Impact of Fuel Variability on Dynamic Instabilities in Gas Turbine Combustion, 5th US Combustion Meeting,

Organized by the Western States Section of the Combustion Institute and Hosted by the University of San Diego, March 25-28, 2007.

References:

Ferguson, Straub, Richards, Robey, Impact of Fuel Variability on Dynamic Instabilities in Gas Turbine Combustion, 5th US Combustion Meeting,

Coal-derived Syngas and Landfill Gas

Organized by the Western States Section of the Combustion Institute and Hosted by the University of San Diego, March 25-28, 2007.

E.42. Syngas--Compatibility and Environmental Issues

### **Incompatible Materials**

<u>elastomers</u> <u>metals</u>

Buna N some grades of carbon steel

Neoprene low-alloy steel
Natural rubber high strength steel
Butyl rubber stainless steel

nickel alloy

### **Compatible Materials**

<u>elastomers</u> <u>metals</u>

Viton low strength, high toughness carbon steel

Teflon microalloyed steel

### **Environmental/Health Concerns**

Flammable

CO component is highly toxic

### **Transportation Precautions**

Pipeline must be free of water to prevent serious corrosion when syngas is introduced H2 component highly prone to leaks

references: European Industrial Gases Association, Carbon Monoxide and Syngas Pipeline Systems, www.eiga.org, 2004

**Properties** 

### E.43. Lignin Liquids--Properties

- reported	Black Liquor Eucalyptus	Black Liquor Bamboo	Heavy Petroleum Fuel	
Molecular Formula				
Molecular Weight (g/mol)				
Elemental Composition (mass% per dry solids for liquor)				
Carbon	30.8	35.4	85.2	
Hydrogen	3.6	3.6	11.1	
Oxygen	0.0	0.0		
Nitrogen	0.01	0.3	0.3	
Sodium	21.8	13.3	0.5	High Group 1 metals
Potassium	1.8	3.3		riigir Group i metais
Sulfur	3.7	0.2	2.3	
Chlorine	4.5	1.3	2.3	
Silicon	0.1	3.8		
Lignin Concentration (% mass per mass dry solids)	42.3	45.3		
Density (g/cm3) at 26 - 30 degC for liquors	1.005	0.947	0.94	
Vapor Pressure kPa at 38 degC				
Boiling Point				
Flash Point (degC)				
Pour Point (degC)				
Cloud Point (degC)				
High Heating Value (MJ/L)	14.67	13.90	40	Lower energy content
Low Heating Value (MJ/L)				
Water Solubility at 21 degC				
Water in fuel (%mass)			0.1	
Water content in fuel (mg/kg)				
Fuel Miscibility				
Solvation Potential				
Flammability Limits (Vol%)				
Lower				
Higher				
Acid Number				
Cetane Number				
Viscosity (mPa-s)	30000*	50*	180 at 50 degC	Higher viscosity for Eucalyptus
Kinematic viscosity (mm^2/s)	00000	00	100 at 00 augu	riigiter viococity for Educatypiae
Lubricity (um)				
Edulicity (dill)				
Toxicity				
Acute: Animal Aerosol Inhalation LD50 (mg/m3)				
Acute: Rabbit Dermal No observable effect concentration (mg/kg)				
Acute: Rabbit Eye Corneal Damage (mL)				
Acute: Oral (mg/kg)				
Acute:Fish LC50 and bacteria EC50 (mg/L)				
Chronic: Rat and Mouse oral (mg/m3)				
Mutagenicity				
Partition coefficient (Kow)				
Log Kow at 25 degC				
Bioconcentration factor (L/kg) [j]				
Soil adsorption				
Half-life in water at typical env. conditions				
Half-life in atmosphere				
Biodegradation: Aerobic in freshwater, 28 days				
Appearance				
Odor				
Odor threshold (mg/m3)				
Odor threshold (ppm)				

<sup>\*</sup> The liquor viscosity depends on sheer rate, temperature and lignin concentration; the values reported are for 10/s sheer rate, ~40.5 % mass lignin per dry mass solids, and 30.1 - 31.5 degC (Cardoso et al., 2009).

Black Liquor References Cardoso, Domingos, Oliveira, Passos, Chemical Composition and Physical Properties of Black Liquors and Their Effects on Liquor Recovery Operation in Brazilian Pulp Mills, Fuel, 2009, 88, 756-763.

FAME Specification Reference Hannu Jaaskelainen, Biodiesel Fuel Standards, http://www.dieselnet.com/tech/fuel\_biodiesel\_std.html

Alternative Fuels Guidebook: Properties, Storage, Dispensing, and Vehicle Facility Modifications SAE Order Number R-180, 1997
Richard L. Bechtold Diesel References

a) Emissions and Lubricity Evaluation of Rapeseed Derived Biodiesel Fuels

SwRI 7507, November 1996 Christopher A. Sharp

b) Hess, Boehman, Tijm, Waller, Experimental Studies of the Impact of CETANER on Diesel Combustion and Emissions, SAE Technical Paper 2000-01-2886

E.44. Lignin Liquids--Compatibility and Environmental Issues

#### Advantages

Can be refined into a number of different fuels including DME, ethanol, methanol, FT diesel, and biogas Estimated US annual black liquor yield is 28 million tons
High land-use efficiency when processed to produce DME or methanol

#### Disadvantages

Low diesel yield compared to DME/methanol/etc. yields

Black liquor generation also produces highly corrosive Na2CO2 and Na2S smelts that can damage a recovery boiler

references: LeBlanc, Richard J., "Black Liquor Gasification Can Help Sustain Forests, Generate Ultra-Clean Biofuels", Biomass Magazine, 7/09

Ekbom, T., "High Efficienct Motor Fuel Production From Biomass Via Black Liquor Gasification", ISAF XV International Symposium on Alcohol Fuels, 9/05

Hubbard, C. R., Peascoe, R. A., Keiser, J. R., "Pulp and Paper Plant Materials Issues Addressed by X-Ray and Neutron Diffraction Methods", International Center for Diffraction Data, Advances in X-Ray Analysis Vol. 46, 2003

European Project BioDME, "Production of DME from Biomass and Utilisation as Fuel for Transport and for Industrial Use", 7th Framework Program, 2009

E.45. Sugar and Alcohols--Properties

NO PUBLISHED DATA WAS FOUND FOR PROPERTIES OR CHEMISTRY OF MIXED SUGAR AND CARBOHYDRATE FEEDSTOCKS FOR FUEL PRODUCTION ALCOHOL BASED FEEDSTOCKS WOULD BE EXPECTED TO HAVE SIMILAR PROPERTIES AND CHEMISTRY TO ALCOHOLS LISTED IN THE FUELS SECTIONS

### Fungible Fuels Composed of Gasoline- and Diesel-like Hydrocarbons Produced from Sugar and Alcohols

Process developed by group of J. A. Dumesic at the University of Wisconsin-Madison:

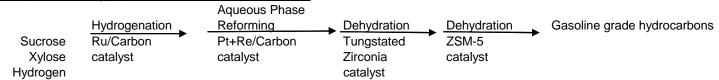
		C4-C6 hydrocarbons		
Biomass-derived carbohydrates	Carbon supported	Alcohols	C-C coupling	Deoxygenation over
Monosaccharides	<del></del>	Ketones	C7-C12 ketones	Diesel grade alkanes
Sugar Alcohols	Pt-Re catalyst	Carboxylic acids	Processes	Pt/NbOPO4 catalyst

#### References:

Gurbuz, Kunkes, Simonetti, West, Serrano-Ruiz, Gaertner, Dumesic (2009) Catalytic Production and Upgrading of Biomass Derived Monofunctional Hydrocarbons, Proceedings of the American Institute of Chemical Engineers Annual Meeting, November 2009, Nashville, TN.

Kunkes, Simonetti, West, Serrano-Ruiz, Gartner, Dumesic (2008) Catalytic Conversion of Biomass to Monofunctional Hydrocarbons and Targeted Liquid-fuel Classes, Science, Vol. 322, pp. 417-421.

### Process developed by Virent Energy Systems, Inc., Madison, Wisconsin.



Virent sugar-derived aviation fue			
	Limit		
1.1	25 max		
< 0.001	0.3 max		
.77584	0.7398		
< -70	-40 max		
240.7	300 max		
33	38 min		
44.21	42.8		
2.74	8 max		
	1.1 < 0.001 .77584 < -70 240.7 33 44.21		

E.46. Sugar and Alcohols--Compatibility and Environmental Issues

NO PUBLISHED DATA WAS FOUND FOR COMPATABILITY OR ENVIRONMENTAL INFORMATION RELATED TO MIXED SUGAR AND CARBOHYDRATE FEEDSTOCKS FOR FUEL PRODUCTION ALCOHOL BASED FEEDSTOCKS WOULD BE EXPECTED TO HAVE SIMILAR COMPATABILITY AND ENVIRONMENTAL CHARACTERISTICS TO ALCOHOLS LISTED IN THE FUELS SECTIONS

#### Fungible Fuels Composed of Gasoline- and Diesel-like Hydrocarbons Produced from Sugar and Alcohols

Process developed by group of J. A. Dumesic at the University of Wisconsin-Madison:

		C4-C6 hydrocarbons			
Biomass-derived carbohydrates	Carbon supported	Alcohols	C-C coupling	Deoxygenation over	
Monosaccharides	<del></del>	Ketones	C7-C12 ketones	<del></del>	Diesel grade alkanes
Sugar Alcohols	Pt-Re catalyst	Carboxylic acids	Processes	Pt/NbOPO4 catalyst	

#### References:

Gurbuz, Kunkes, Simonetti, West, Serrano-Ruiz, Gaertner, Dumesic (2009) Catalytic Production and Upgrading of Biomass Derived Monofunctional Hydrocarbons, Proceedings of the American Institute of Chemical Engineers Annual Meeting, November 2009, Nashville, TN.

Kunkes, Simonetti, West, Serrano-Ruiz, Gartner, Dumesic (2008) Catalytic Conversion of Biomass to Monofunctional Hydrocarbons and Targeted Liquid-fuel Classes, Science, Vol. 322, pp. 417-421.

### Process developed by Virent Energy Systems, Inc., Madison, Wisconsin.

		Aqueous Phase			
	Hydrogenation _	Reforming	Dehydration	Dehydration	Gasoline grade hydrocarbons
Sucrose	Ru/Carbon	Pt+Re/Carbon	Tungstated	ZSM-5	
Xylose	catalyst	catalyst	Zirconia	catalyst	
Hvdroaen			catalyst		

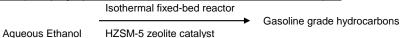
#### Virent sugar-derived aviation fuel

		Limit	
	1.1	25 max	
Aromatics (vol %)	< 0.001	0.3 max	
Sulfur	.77584	0.7398	
Density (g/cm3)	< -70	-40 max	
Freezing Point (deg C)	240.7	300 max	
Boiling Point	33	38 min	
Flash Point (degC)	44.21	42.8	
Specific Energy (MJ/kg)	2.74	8 max	
Viscosity at -20C (cSt)			

#### Reference:

Blommel, Cortright of Virent Energy Systems, Inc., Production of Conventional Liquid Fuels from Sugars, White Paper, August 25, 2008.

#### Process developed by Aguayo et al. (2002) at the Universidad del Pais Vasco, Spain



#### Reference:

Aguayo, Gayubo, Tarrio, Atutxa, Bilbao (2002) Study of Operating Variables in the Transformation of Aqueous Ethanol into Hydrocarbons on a HZSM-5 Zeolite, Journal of Chemical Technology and Biotechnology, Vol. 77, pp. 211-216.

### E.47. Terpenes--Properties

An advantage of terpenes is water insolubility, however, "Strains and processes capable of converting sugars to terpe-noids at yields similar to the ethanol process have not yet been reported in the scientific literature." Reference: Fisher, Kein-Marcuschamer, Stephanopoulos, Selection and Optimization of Microbial Hosts for Biofuels Production, Metabolic Engineering, 2008, Vol. 10, pp. 295-304.

"Orange oil is a biomass-derived fuel obtained from orange skin, which has ~90% D-limonene and can be used for many applications." "In addition, orange oil can also be used as an alternative to gasoline either partially in the form of a blend or as a total replacement. "India has a huge potential of producing orange peel oil of ~27,600 ton (based on 0.6% recovery of oil from 46 lakhs ton fruits -21,000 for (base) of 10 for 8 receively of oil min-14 datas to find its by cold press process) from the orange fruits. Presently, 2–3 tons of orange oil are produced for food and cosmetic industries. There is no other demand for orange oil."
Reference:

Purushothaman, Nagarajan (2009) Experimental Investigation on a C.I. Engine Using Orange Oil and Orange Oil with DEE, Fuel, Vol. 88, pp. 1732-1740.

#### Properties

	d-Limonene	Gasoline
Molecular Formula	C10H16	C4 to C12
Molecular Weight (g/mol)	136.23	100-105
Elemental Composition (mass%)		
Carbon	88	85-88
Hydrogen	12	12-15
Oxygen		0-4
Density (g/cm3)	0.8402	0.69-0.79 at 15 deg C
Vapor Pressure (kPa)	0.2	48-103 at 38 deg C
Boiling Point (degC)	175	27-225
Flash Point (degC)	45	-43
Pour Point (degC)		
Cloud Point		
Freezing Point (degC)	-40	-40
High Heating Value (MJ/L)	37.96 [a]	35
Low Heating Value (MJ/L)		30-33
Water Solubility at 21 degC		
Water in fuel (Vol%)	Negligible [b]	Negligible
Fuel Miscibility		
Solvation Potential		
Flammability Limits (Vol%)		
Lower	0.7	1.4
Higher	6.1	7.6
Acid Number		
Research Octane Number		88-100
Viscosity (mPa-s) at 25 degC	1.08 [b]	0.37-0.44
Lubricity (um)		
Toxicity	Sensitizer, skin & lung irritant	
Acute: Rat oral LD50 (mg/kg)	4400	
Acute: Mouse Inhalation LD50 (ppm)		101200 [a]
Acute: Rabbit eye irritation (mg)		
Acute: Rabbit dermal (mgkg)	> 5000	
Acute:LC50 for fish 96-hour values(ppm)		
Acute:Half max effective concentration for aquatic invertebrate (daphnia) (mg/L)		
Acute:Aquatic plants - Half max effective concentration (mg/L)		
Chronic: Rat inhalation Lowest observable effect conc. (ppm)		
Teratogenicity: Rat inhalation No observable effect conc. (ppm)	May cause birth defects	9000 [a]
Partition coefficient (Kow)		octanol-water
Log Kow at 25 degC		2.13 to 4.85 [a]
Bioconcentration factor (L/kg)		
Transport between Environmental Compartments		
Soil/Air		
Soil/Water		
Air/Water		
Half-life in water at typical env. conditions		
Half-life in atmosphere		
Photodegradation half-life in air	1 hour [b]	0.8 to 16 days [a]
Biodegradation	100% in 28 days	Readily in aerobic cond.
Appearance	clear, almost colorless	clear to amber [a]
Odor	citrus	
Odor Threshold (ppm)		
CAS number	5989-27-5	

references:

Science Lab MSDS, d-Limonene, 11/06/2008, http://www.sciencelab.com/xMSDS-DLimonene-9924496

Science Earl MISJO - Chilinoterie, 17 mol 2006, http://www.science@auchim/MisJOS-dimonteriersez-winneriersez-

Alternative Fuels Guidebook: Properties, Storage, Dispensing, and Vehicle Facility Modifications

references:

Alethnative Puels disubstook. Properties, Storage, Dispensing, and Venicle Facility industrials SAE Order Number R-180, 1997 Richard L. Bechtold J.J TBaker MSDS, Gasoline, 10/14/2008, http://www.docs.citgo.com/msds\_pi/UNLEAD.pdf

E.48. Terpenes--Compatibility and Environmental Issues

### **Incompatible Materials**

<u>elastomers</u> <u>metals</u>
PVC ferrous metals\*

nitrile silicone Tygon

natural rubber latex rubber neoprene

### **Compatible Materials**

elastomersmetalsTeflonnon-ferrous metals\*polypropylenestainless steel

epoxy Viton nylon

# **Vehicle Compatibility**

Compatible with terne-coated steel, commonly used for fuel tanks Hoses made of nitrile or natural rubber must be replaced with Viton, etc.

### **Advantages**

Negligibly miscible in water

## Disadvantages

notes: \*non-corrosive to metals but can

become discolored by rust from ferrous metals

references: T2 Laboratories Inc., "Information Bulletin: Material Compatability with Terpene Chemicals", www.t2labs.com, 1995

E.49. Isoprenes--Properties

"...ethanol has a lower energy density and must be distilled from the fermentation broth, requiring significant energy. Soprene could be made instead and collected from the gas phase of the ferment; eliminating the need for distillation. Isoprene has a higher energy density that enthanol and does not absorb water and so should be less corrosive when used in authorities. Isoprene has a higher energy density than extended to the state of th used to make ethanol. Starch from Zea may grain is currently a major starting point in the either hippic currently used to make ethanol. Starch from Zea may grain is currently a major starting point in the ethanol industry in the US and this is generally considered unsustainable. As alternate inputs are developed there is no reason that those inputs could not be converted to isoprene instead of ethanol. On the other hand, isoprene emission is closely associated with photosynthesis so photosynthesic organisms engineered to make high levels of closely associated with photosynthesis so photosynthesic organisms engineered to make high levels of the convergence of the isoprene can also be envisioned for the future."

Sharkey (2009) The Future of Isoprene Research, Bulletin of the Georgian National Academy of Sciences, Vol. 3, No. 3.

P	rn	pe	rti	io

Stoprene   Stoprene   Caseline   Care   Caseline   Care	Properties			
Molecular Weight (gmn0)				Comments
Elemental Composition (mass%)				
Carbon         88         85-88           Hydrogen         10         0-4           Oensity (glorna) at 20deg C         0.68         0.69-0.79           Reid Vapor Pressure (kPa)         103.4         48-103           Bolling Point (degC)         34.1         27-225           Flash Point (degC)         -54         43         Lower flashpoint           Pour Point (degC)         -54         43         Lower flashpoint           Preezing Point (degC)         -146		68.12	100-105	
Hydrogen				
Oxygen         0         0.4         Density (grons) at 20deg C         0.68 8         0.69-0.79         Reid Vapor Pressure (kPa)         48-103         48-103         Alender Control (Geg C)         34.1         27-225         Pressure (kPa)         48-103         Alender Control (Geg C)         48-103         Alender Control (Geg C)         48-103         Alender Control (Geg C)         49-10         4-146         48-10         Alender Control (Geg C)         4-146         48-10         48-10         Alender Control (Geg C)         4-146         48-10         30-33         35-33         30-33         30-33         30-33         30-33         30-33         35-10         48-10         49-10         <				
Density (g/cm/3) at 20deg C         0.68         0.89-0.79           Reil (Vapor Fressure (kPa)         103.4         48-103         Lower flashpoint           Boiling Point (degC)         34.1         27-225         Lower flashpoint           Flash Point (degC)         -54         -43         Lower flashpoint           Freezing Point (degC)         -146         -148 </td <td></td> <td></td> <td></td> <td></td>				
Reid Yapor Pressure (kPa)         103.4         48-103           Boiling Point (degC)         -54         -27.25           Flash Point (degC)         -54         -43         Lower flashpoint           Pour Point (degC)         -146         -7.25				
Boiling Point (degC)				
Flash Point (degC)				
Pour Point (degC)   Cloud Point   Freezing Point (degC)   -146   -146   Freezing Point (degC)   -146   Freezing Point (degC)   -146   -146   Freezing Point (degC)   -146   Freezing Poi				
Cloud Point   Freezing Point (degC)		-54	-43	Lower flashpoint
Freezing Point (degC)         -146           High Heating Value (MJ/L)         30         35           Low Heating Value (MJ/L)         30-33         30-33           Water in fuel (prm)         -50         -50           Fuel Misscibility         -50         -50           Solvation Potential         -1.5         1.4           Flammability Limits (Vol%)         -1.5         1.4           Lower         1.5         1.4           Higher         9.7         7.6           Acid Number         88-100         0.37-0.4           Research Octane Number         88-100         0.37-0.4           Viscosity (mPa-s)         1.5         1.4           Lubridity (um)         5240         0.37-0.4           Acute: Rat oral LD50 (mg/kg)         5240         1.0           Acute: Ratorial LD50 (mg/kg)         8900         1.0           Acute: Rabbit dermal (mgkg)         8900         8900           Acute: Rabbit dermal (mgkg)         8900         8900           Acute: Albit max effective concentration (mg/L)         1.0         1.0           Carcinogenicity         Rat inhalation No observable effect conc. (ppm)         2.13 to 4.85 [a]           Partition coefficient (Kow)         2.13 to 4.				
High Heating Value (MJL)         30         35           Low Heating Value (MJL)         30-33           Water Solubility at 21 degC         450           Fuel Miscibility         50           Solvation Potential         15           Flammability Limits (Vol%)         1.5         1.4           Lower         1.5         1.4           Higher         9.7         7.6           Acid Number         88-100         0.37-0.44           Viscosity (mPa-s)         1.5         1.4           Lubricity (urm)         7.6         3.81-100           Toxicity         88-100         0.37-0.44           Viscosity (mPa-s)         1.5         1.4           Lubricity (urm)         5240         1.01200 [a]           Acute: Rat oral LD50 (mg/kg)         8900         101200 [a]           Acute: Rabbit dermal (mgkg)         8900         8900           Acute: Rabbit dermal (mgkg)         8900         101200 [a]           Acute: Half max effective concentration for aquatic invertebrate (daphnia) (mg/L)         Carcinogenic         1000           Carcinogenicity         Carcinogenicity         2.13 to 4.85 [a]         1000           Teratogenicity         1000         1000         1000		440		
Low Heating Value (M.M.)         30-33           Water Solubility at 21 degC         -50           Water in tuel (ppm)         -50           Fuel Miscibility         -50           Solvation Potential         -50           Flammability Limits (Vol%)         -50           Lower         1.5         1.4           Higher         9.7         7.6           Acid Number         88-100           Research Octane Number         88-100           Viscosity (mPa-s)         0.37-0.44           Lubricity (um)         5240           Acute: Ratoral LD50 (mg/kg)         5240           Acute: Ratoral LD50 (pmg/kg)         5240           Acute: Ratoral LD50 (pmg/kg)         8900           Acute: Rabbit dermal (mgkg)         8900           Acute: LD50 for fish 96-hour values(ppm)         8900           Acute: LD50 for fish 96-hour values(ppm)         8900           Acute: Labit dermal (mgkg)         8900           Acute: LD50 for fish 96-hour values(ppm)         Carcinogenic           Carcinogenicity: Rat inhalation No observable effect conc. (ppm)         000           Carcinogenicity: Rat inhalation No observable effect conc. (ppm)         9000 [a           Partition coefficient (Kow)         2.13 to 4.85 [a]			05	
Water fue (ppm)         -50           Fuel Miscibility         -50           Fuel Miscibility         -50           Fuel Miscibility         -50           Flammability Limits (Vol%)         -50           Lower         1.5         1.4           Higher         9.7         7.6           Acid Number         88-100         37-0.44           Research Octane Number         88-100         3.7-0.44           Viscosity (mPa-s)         2240         3.7-0.44           Lubricity (um)         5240         3.578         101200 [a]           Acute: Rat oral LD50 (mg/kg)         35278         101200 [a]         1.5         1.4         1.5         1.5         1.4         1.5         1.5         1.5         1.5         1.5         1.5         1.5         1.5         1.5         1.5         1.5         1.6         1.0         1		30		
Value in fue (pom)			30-33	
Fuel Missibility Solvation Potential Flammability Limits (Vol%) Lower 1.5 1.5 1.4 Higher 9.7 7.6 Acid Number 8.8-100 Viscosity (mPa-s) Lubricity (um) Toxicity 8.1-10-10-10-10-10-10-10-10-10-10-10-10-10			×50	
Solvation Potential   Flammability Limits (Vol%)   Lower   1.5   1.4   1.5   1.4   1.5   1.4   1.5   1.4   1.5   1.4   1.5   1.4   1.5   1.4   1.5   1.4   1.5   1.4   1.5   1.4   1.5   1.5   1.4   1.5   1.5   1.4   1.5			230	
Flammability Limits (Vol%)   1.5				
Lower   1.5   1.4   1.5   1.4   1.5   1.4   1.5   1.4   1.5   1.4   1.5   1.4   1.5   1.5   1.4   1.5   1.5   1.4   1.5   1.				
Higher		1.5	1.4	
Acid Number         88-100           Research Octane Number         0.37-0.44           Viscosity (mPa-s)         (0.37-0.44           Lubricity (tum)         Risk damage eyes, respir.           Toxicity         Acute: Rat oral LD50 (mg/kg)           Acute: Nabit in LD50 (ppm)         35278         101200 [a]           Acute: Rabbit eye irritation (mg/kg)         8900           Acute: Rabbit dermal (mgkg)         8900           Acute: Aquatic Idermal fems effective concentration for aquatic invertebrate (daphnia) (mg/L)         Carcinogenic           Acute: Aquatic plants - Half max effective concentration (mg/L)         Carcinogenic           Carcinogenicity         Carcinogenic           Carcinogenicity         09000 [a]           Carcinogenicity         09000 [a]           Partition coefficient (Kow)         0000 [a]           Log Kow at 25 degC         2.13 to 4.85 [a]           Bioconcentration factor (L/kg)         2.13 to 4.85 [a]           Transport between Environmental Compartments         Soil/Air           Soil/Water         Air/Water           Half-life in water at typical env. conditions         Readily in aerobic cond. [a]           clair in atmosphere         Products of biodeg, toxic         Readily in aerobic cond. [a]           Cloer Toward Cond. [a] <t< td=""><td></td><td></td><td></td><td></td></t<>				
Research Octane Number Viscosity (mPa-s) Viscosity (mpa-sperice) Viscosity (mp		0.7	7.0	
Viscosity (mPa-s) Lubricity (urm) Toxicity Acute: Rat oral LD50 (mg/kg) Acute: Mouse Inhalation LD50 (ppm) Acute: Rabbit gever irratation (mg/kg) Acute: Rabbit dermal (mg/kg) Acute: LC50 for fish 96-hour values(ppm) Acute: Half max effective concentration for aquatic invertebrate (daphnia) (mg/L) Acute: Aquatic plants - Half max effective concentration (mg/L) Chronic: Rat inhalation Lowest observable effect conc. (ppm) Carcinogenicity Teratogenicity Rat inhalation No observable effect conc. (ppm) Carcinogenicity Rat inhalation No observable effect conc. (ppm) Partition coefficient (Kow) Log Kow at 25 degC Internation factor (L/kg) Transport between Environmental Compartments Soil/Water Air/Water Half-life in water at typical env. conditions Half-life in water at typical env. conditions Half-life in atmosphere Photodegradation half-life in air Biodegradation Appearance Odor Threshold (ppm)			88-100	
Lubricity (um)         Risk damage eyes, respir.           Toxicity         S240           Acute: Rat oral LD50 (mg/kg)         5240           Acute: Ratorial LD50 (ppm)         33278         101200 [a]           Acute: Ratorial veg irritation (mg)         8900           Acute: LC50 for fish 96-hour values(ppm)         8900           Acute-1.C41 for fish 96-hour values(ppm)         Acute-1.C41 for fish 96-hour values(ppm)           Acute-1.C41 firm ax effective concentration for aquatic invertebrate (daphnia) (mg/L)         Carcinogenic           Carcinogenicity         Carcinogenic           Carcinogenicity: Rat inhalation No observable effect conc. (ppm)         Carcinogenic           Carcinogenicity: Rat inhalation No observable effect conc. (ppm)         9000 [a]           Partition coefficient (Kow)         2.13 to 4.85 [a]           Bioconcentration factor (L/kg)         2.13 to 4.85 [a]           Transport between Environmental Compartments         Soil/Air           Soil/Water         Air/Water           Air/Water         Half-life in water at typical env. conditions           Half-life in atmosphere         0.8 to 16 days [a]           Photodegradation half-life in air         Readily in aerobic cond. [a]           Glodegradation half-life in air         Iquid           Coor         Liquid <td></td> <td></td> <td></td> <td></td>				
Acute: At rate ILD50 (mg/kg)				
Acute: At rate ILD50 (mg/kg)	Toxicity	Risk damage eyes, respir.		
Acute: Rabbit eye irritation (mg) Acute: Rabbit dermal (mgk) Acute: Rabbit	Acute: Rat oral LD50 (mg/kg)			
Acute: Rabbit dermal (mgkg) 8900 Acute:LS0 for fish 96-hour values(ppm) Acute:LS0 fish 96-hour values(ppm) Acute:LS0 fish 96-hour values(ppm) Carcinogenic Carcin	Acute: Mouse Inhalation LD50 (ppm)	35278	101200 [a]	
Acute:LC50 for fish 96-hour values(ppm) Acute:L30 for fish 96-hour values(ppm) Acute:Alquatic plants - Half max effective concentration (mg/L) Chronic: Rat inhalation Lowest observable effect conc. (ppm) Carcinogenicic Teratogenicity: Rat inhalation No observable effect conc. (ppm) Partition coefficient (Kow) Log Kow at 25 degC Silvant Silv	Acute: Rabbit eye irritation (mg)			
Acute-Alaff max effective concentration for aquatic invertebrate (daphnia) (mg/L) Acute-Aquatic plants - Half max effective concentration (mg/L) Chronic: Rat inhalation Lowest observable effect conc. (ppm) Carcinogenicity Carcinogenicity Carcinogenicity: Rat inhalation No observable effect conc. (ppm) Partition coefficient (Kow) Log Kow at 25 deg/C Bioconcentration factor (L/kg) Transport between Environmental Compartments Soil/Air Soil/Water Air/Water Air/Water Half-life in water at typical env. conditions Half-life in atmosphere Photodegradation half-life in air Biodegradation half-life in air Biodegradation Appearance Odor Threshold (ppm)	Acute: Rabbit dermal (mgkg)	8900		
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Carcinogenicity Carcinogenicit				
Teratogenicity' Rat inhalation No observable effect conc. (ppm)  Partition coefficient (Kow) Log Kow at 25 degC Bioconcentration factor (L/kg) Bioconcentra	Chronic: Rat inhalation Lowest observable effect conc. (ppm)			
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Log Kow at 25 degC 2.13 to 4.85 [a]  Bioconcentration factor (L/kg)  Transport between Environmental Compartments Soil/Water Soil/Water Air/Water Half-life in water at typical env. conditions Half-life in atmosphere Photodegradation half-life in air Biodegradation Self-life in air Biodegradation Self-life in air Codor Codor Threshold (ppm)  2.13 to 4.85 [a]  8.13 to 4.85 [a]  8.13 to 4.85 [a]  8.14 to 4.85 [a]  8.15 to 4.8				
Bioconcentration factor (L/kg) Transport between Environmental Compartments Soil/Air Soil/Water Air/Water Half-life in water at typical env. conditions Half-life in atmosphere Photodegradation half-life in air Biodegradation half-life in air Biodegradation Appearance Odor Odor Threshold (ppm)				
Transport between Environmental Compartments Soil/Air Soil/Water Air/Water Half-life in water at typical env. conditions Half-life in in atmosphere Photodegradation half-life in air Biodegradation Appearance Odor Odor Threshold (ppm)			2.13 to 4.85 [a]	
Soil/Mair Soil/Water Alir/Water Half-life in water at typical env. conditions Half-life in atmosphere Photodegradation half-life in air Biodegradation half-life in air Biodegradation Products of biodeg, toxic Appearance Odor Odor Threshold (ppm)    Odor Threshold (ppm)				
Soil/Water  Air/Water  Half-life in water at typical env. conditions  Half-life in atmosphere  Photodegradation half-life in air  Biodegradation  Products of biodeg. toxic Appearance  Odor  Odor  Odor Threshold (ppm)				
Air/Nater Half-life in water at typical env. conditions Half-life in in water at typical env. conditions Half-life in introsphere Photodegradation half-life in air Biodegradation Products of biodeg. toxic Appearance Iiquid Cdor Cdor Threshold (ppm)  0.8 to 16 days [a] Readliy in aerobic cond. [a] clear to amber [a]				
Half-life in water at typical env. conditions Half-life in atmosphere Photodegradation half-life in air Biodegradation half-life in air Products of biodeg. toxic Readily in aerobic cond. [a] Appearance Odor Odor Threshold (ppm)				
Half-life in atmosphere Photodegradation half-life in air Biodegradation Products of biodeg. toxic Appearance Odor Odor Odor Threshold (ppm)  0.8 to 16 days [a] Readily in aerobic cond. [a] clear to amber [a]				
Photodegradation half-life in air Biodegradation half-life in air Biodegradation Products of biodeg. toxic Appearance liquid Cdor Cdor Threshold (ppm)  0.8 to 16 days [a] Readlily in aerobic cond. [a] clear to amber [a]				
Biodegradation Products of biodeg. toxic Readily in aerobic cond. [a] Appearance liquid clear to amber [a] Odor Odor Threshold (ppm)			0.8 to 16 days [a]	
Appearance liquid clear to amber [a] Odor Odor Threshold (ppm)		Products of biodea toxic		
Odor Odor Threshold (ppm)				
Odor Threshold (ppm)		nquiu	sour to unibor [a]	
		7879-5		

Reference: isoprene

Science Lab MSDS, 11/06/2008, http://www.sciencelab.com/xMSDS-Isoprene-9924409

references: gasoline

Alternative Fuels Guidebook: Properties, Storage, Dispensing, and Vehicle Facility Modifications SAE Order Number R-180, 1997

a) JT Baker MSDS, Gasoline, 10/14/2008, http://www.docs.citgo.com/msds\_pi/UNLEAD.pdf

E.50. Isoprenes--Compatibility and Environmental Issues

# **Incompatible Materials**

<u>elastomers</u> <u>metals</u>

### **Compatible Materials**

<u>elastomers</u> <u>metals</u>

### **Advantages**

Water insoluble

### **Disadvantages**

Highly flammable Harmful to aquatic life in very low doses Highly volatile

### **Environmental/Health concerns**

Water insoluble Flammable Harmful to aquatic life in very low doses

### Compatibility/Fungibility issues

Requires private track for transport by rail

#### **Production**

1996 US isoprene production capacity: 598 million lbs.

references: Cameo Chemicals Inc., "Isoprene", www.cameochemicals.noaa.gov, 6/1999

ExxonMobil Chemical, "Isoprene Product Safety Summary", www.exxonmobilchemical.com, 6/2009

National Institute of Health, "Substance Profiles: Isoprene", www.ntp.niehs.nih.gov, 2000

### E.51. Methane--Properties

"When fitted according to approved standards, the use of biomethane in vehicles can be safer than petrol.

This is due to the higher flammability limits, higher diffusion coefficient and auto-ignition temperature of biomethane (Cenex, 2009)." Reference:

Renewable Energy, Landfill Gas and EfW: Now, Next and Future

K A Adu-Gyamfi, R Villa and F Coulon

http://www.geotech.co.uk/press\_releases/Geotech%20sponsored%20paper.pdf

#### Motor vehicle fuel standard in Sweden for biomethane

Property	Units	Requirement Type A	Requirement Type B	Test Method
Wobbe index (1)	MJ/m²	44./ - 46.4	43.9 – 47.3	SS-ISO 69/6
Methane (volume at 273 K, 101.3 kPa)	%	97±1	97±2	ISO 6974
Motor Octane Number (MON)		130	130	2)
Dewpoint at highest storage pressure	°C	t - 5	t - 5	ISO 6327
t = lowest monthly daily average temperature				
Water content	mg/m³	32	32	SS-EN ISO 10101- 1, -2,-3
CO <sub>2</sub> + O <sub>2</sub> + N <sub>2</sub> by volume, max.	%	4,0	5,0	ISO 6974
Of which O <sub>2</sub> , max	%	1.0	1.0	
Total sulphur	mg/m³	23	23	ISO 6326-1,-2,-4 SS-EN ISO -3,-5
Total nitrogen compounds calculated as NH₃	mg/m³	20	20	ISO 6974 <sup>5</sup>
Alcohol		6)	6)	

#### Reference:

EPUK (2006) Biogas as a Road Transport Fuel, National Society for Clean Air and

Environmental Protection (now Environmental Protection UK), June 2006.

http://www.environmentalprotection.org.uk/assets/library/documents/biogas as transport fuel june06.pdf

# Motor vehicle fuel standard in Austria (BGBL 417/04) and Europe (DIN 51624) for biomethane In comparison to upgraded biogas (methaPUR) and raw biogas

Table 1: Composition and properties of raw biogas produced in Margarethen/Mocs compared to methaPUR and CNG- quality defined by Austrian Law and DIN

Component	Raw	methaPUR	Austrian Law	DIN	
Component	Biogas	standard	BGBL 417/04	51624	Unit
Methane	49±10	>95	NR	>80	mol%
Carbon dioxide	$51 \pm 10$	<5	NR	S 15	mol%
Nitrogen	<0,3	<1,0	NR	Sum <15	mol%
Oxygen	<0.1	<1.0	NR	<3.0	mol%
Hydrogen sulphide	5 (<20)	<10	NR	<5*	ppmv
Water	saturated	"dried"	NR	<40	mg/kg
Particulate matter	techn. free	techn. free	techn. free	-	mg/kg
Relative density	1,05*	0,60*	0,55-0,7	0,56-0,70*	kWh/m3
Upper Calorific value	5,40*	>10,45	8,4-13,1	NR	kWh/m3
Wobbe Index	5,27*	>13,6	12,8-15,7	NR	kWh/m³

"In order to produce fuel for the Austrian market, the product has to fulfill the Austrian law "Kraftstoffverordnung" BGBL 417/04, while in Germany and many other European countries DIN 51624 is applicable. It is planned to merchandize upgraded biogas on several locations in Austria and abroad; therefore a new fuel brand called "methaPUR" has been established, unifying the numerous quality parameters in one standard. The definition of the methaPUR standard is compared to the composition of gaseous fuels (CNG – compressed natural gas) prescribed in the aforementioned laws and to the raw biogas in Table 1. It has to be mentioned, that the hydrogen sulphide content of the raw biogas is extremely low due to effective in-situ-desulphurization using commercially available liquid mixtures of metal salts and due to the favorable local substrate mixture (high content of energy crops together with liquid pig manure).

It can be easily seen that in order to upgrade biogas to accepted fuel qualities, several steps must be performed. The most important of them are the separation of malicious substances, drying and separation of carbon dioxide, nitrogen and oxygen, which results in the increase of the calorific value and the Wobbe Index."

\*... calculated NR... not regulated

#### Reference

Biogas upgrading for transportation purposes – Operational Experiences with Austria's first Bio-CNG fuelling station

Martin Miltner, Aleksander Makaruk, Harald Bala, Michael Harasek

http://www.aidic.it/pres09/webpapers/134Miltner.pdf

Chem Eng Trans, 2009

### E.52. Methane--Compatibility and Environmental Issues

Incompatibility

<u>elastomers</u> <u>metals</u>

Compatibility

elastomers metals

#### Advantages

Non-toxic

Can produce significant reductions in CO2, CO, NOx, and PM emissions

#### Disadvantages

Must be compressed to a liquid for ease of transport

Highly flammable

Can produce significant increases in HC emissions (20x that of gasoline vehicles in Sweden) Can produce significant increases in fuel consumption versus comparable diesel engines

#### Environmental/Health concerns

Non-toxic

Flammable

#### Compatibility/Fungibility issues

Must be compressed to a liquid for ease of transport Trucks carrying methane not permitted in tunnels

#### Motor vehicle fuel standard in Sweden for biomethane

Biogas produced to this standard is subject to a number of storage and handling requirements:

- It shall not include dirt, oil or other substances which can damage engine fuel systems;
- The potential for oil carry-over from gas compressors needs to be mitigated by the use of molecular oil filters downstream of the compressor;
- Alcohol may not be added to avoid freezing as this can cause corrosion in storage tanks;
- The gas shall be odorised to enable the detection of gas at up to a concentration of 20% of its flammability limit. The odorising medium shall not be harmful to health. It may also increase the sulphur content in the fuel.

Table 5.1: Summary	of Costs for the	Production of Bioga	s Used as a Ve	hicle Fuel

Process	Biogas (sewa	ge sludge)	Biogas (organic waste)		
	SEK/Nm³	p/Nm³	SEK/Nm³	p/Nm³	
Production	0 – 1.5	0 – 11	1.5 – 2.5	11 – 18	
Upgrading	1 – 2	7 – 15	1 – 2	7 – 15	
Compression	1	7	1	7	
Total	2.0 - 4.5	14 – 33	3.5 – 5.5	25 - 40	

references:

EPUK, "Biogas as a Road Transport Fuel, National Society for Clean Air and Environmental Protection", www.environmentalprotection.org/uk, 6/06 iSOC Technology, "MSDS: Methane", www.isocinfo.com, 12/09 Feasibility Study for a Large Scale Regional Anaerobic Digestion Facility", 2009

E.53. Hydrogen--Properties

#### **Properties**

Hydrogen is an asphyxiant and highly flammable.

#### Production of bio-hydrogen is in research phase

"Researchers at The National Renewable Energy Laboratory (NREL) are developing advanced processes to produce hydrogen economically from sustainable resources. These R&D efforts include: Fermentation

Biological Water Splitting
Photoelectrochemical Water Splitting
Conversion of Biomass and Wastes
Solar Thermal Water Splitting
Renewable Electrolysis."
Reference:

http://www.nrel.gov/hydrogen/proj\_production\_delivery.html#water

"Currently most hydrogen is produced from fossil fuels (e.g. steam reforming of natural gas). Prototype hydrogen vehicles have been developed, but there is currently no significant infrastructure for distributing hydrogen as a transport fuel, and in-vehicle storage capacity is still an issue. In addition, hydrogen fuel cells are expensive to produce and fragile, and have a relatively short service life."

# "Extensive research is being carried out on chemical storage of hydrogen" Reference:

European Biofuels Technology Platform, funded by the EC under Grant Agreement 241269, Last updated February 23, 2010 http://www.biofuelstp.eu/hydrogen.html

#### Chemical Hydrogen Storage R&D

"DOE's chemical hydrogen storage R&D is focused on developing low-cost energy-efficient regeneration systems for these irreversible hydrogen storage systems. Significant technical issues remain regarding the regeneration of the spent material and whether regeneration can be accomplished on-board. In addition, life cycle cost analysis is needed to assess the costs of regeneration. Currently, borohydride-water systems, magnesium-hydride slurries, and innovation beyond boron are under investigation."

"Research is carried out through DOE's Chemical Hydrogen Storage Center of Excellence

"Research is carried out through DOE's Chemical Hydrogen Storage Center of Excellence and Independent Projects overseen by the Fuel Cell Technologies Program."

Reference:

DOE Fuel Cell Technologies Program

http://www1.eere.energy.gov/hydrogenandfuelcells/storage/hydro\_storage.html

#### **Hydrogen Infrastructure**

"Germany to Launch Nationwide Hydrogen Fuel Network by 2015 Signs a memorandum of understanding with eight industrial partners, including Daimler, Shell, and Total."

Reference:

http://www.nacsonline.com/NACS/News/Daily/Pages/ND0917097.aspx

E.54. Hydrogen--Compatibility and Environmental Issues

#### **Incompatible Materials**

<u>elastomers</u> <u>metals\*</u>

cast iron nickel steel

**Compatible Materials** 

<u>elastomers</u> <u>metals\*</u>

stainless steel carbon steel aluminum copper titanium alloy

### Advantages

### Disadvantages

Highly flammable

Must be compressed to a liquid for ease of transport

#### Environmental/Health concerns

Flammable

#### Compatibility/Fungibility issues

Must be compressed to a liquid for ease of transport Trucks carrying hydrogen not permitted in tunnels

notes: \*high strength steels (above 100ksi) are more suscpetible to

hydrogen embrittlement, therefore low strength steels are

recommended for hydrogen pipelines

references: BOC Gases, "MSDS: Hydrogen", www.fergusongases.com, 6/7/1996

Gillette and Kolpa, Argonne National Laboratories, "Overview of Interstate Hydrogen Pipeline Systems", www.corridoreis.anl.gov, 11/07