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The Enterprise Derivative Application: Flexible Software for Optimizing Manufacturing Processes

November 2008

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The Enterprise Derivative Application: Flexible Software for Optimizing Manufacturing Processes

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Enterprise Derivative Application: Flexible Software for Optimizing Manufacturing Processes

ABSTRACT

The Enterprise Derivative Application (EDA) implements the enterprise-derivative analysis for optimization of an industrial process.¹ It is a tool to help industry planners choose the most productive way of manufacturing their products while minimizing their cost. Developed in Microsoft (MS) Access, the application allows users to input initial data ranging from raw material to variable costs and enables the tracking of specific information as material is passed from one process to another.

Energy-derivative analysis is based on calculation of sensitivity parameters. For the specific application to a steel production process these include: the cost to product sensitivity, the product to energy sensitivity, the energy to efficiency sensitivity, and the efficiency to cost sensitivity. Using the EDA for all processes, the user can display a particular sensitivity or all sensitivities can be compared for all processes.

Although energy-derivative analysis was originally designed for use by the steel industry, it is flexible enough to be applied to many other industrial processes. Examples of processes where energy-derivative analysis would prove useful are wireless monitoring of processes in the petroleum cracking industry and wireless monitoring of motor failure for determining the optimum time to replace motor parts.

One advantage of the MS Access-based application is its flexibility in defining the process flow and establishing the relationships between parent and child process and products resulting from a process. Due to the general design of the program, a process can be anything that occurs over time with resulting output (products). So the application can be easily modified to many different industrial and organizational environments. Another advantage is the flexibility of defining sensitivity parameters. Sensitivities can be determined between all possible variables in the process flow as a function of time. Thus the dynamic development of the process can be tracked over time and optimized. EDA is a uniquely flexible and efficient way for planners to choose the most productive way of optimizing production while minimizing costs.

The purpose of this document is to describe energy-derivative analysis and the operation of the application. The first section is an introduction of the concept, followed in Sect. 2 by a detailed description of the analysis approach. The third section provides a general overview of the operation of the application. The detailed description of the application is described in Sect. 4, using the steel mill operation as an example. Conclusions regarding the utility of the EDA and the effectiveness of the implementation follow in Sect. 5. Appendix A describes details of setting up the process flow model and App. B provides information on overcoming an error that occurred in using the application on a PC that did not have Visual Basic installed.

1. INTRODUCTION

In today's manufacturing environment, systems and equipment are being asked to perform at levels not thought possible a decade ago. The intent is to push process operations, product quality, and equipment reliability to unprecedented levels while pursuing cost reduction initiatives. Industries see a tremendous amount of uncertainty associated with calculating total process impact and fear the mysticism that may be required for such a venture. What is needed is a methodology and approach that takes the guesswork out of calculating the total cost/benefit for any new technology or innovation. The energy-derivative analysis provides a solution to this problem - a new tool for developing and managing investment strategies and risks.

Energy-derivative analysis mitigates risks by first identifying the potential benefits for all processes and sub-processes associated with new technologies or innovations. This is realized by calculating approximations to the first order sensitivity parameters (first derivatives) obtained from using a Taylor Series expansion about the system's operating point. These sensitivity parameters are invariant economic and operational indicators that quantify the impact of any proposed technology in terms of material throughput, efficiency changes, energy use, environmental effects, and costs. The model then develops a set of coupled equations from these parameters that links the entire enterprise system together, so that total impact can be calculated. The key to the model is the evaluation of the sensitivity parameters.

Energy-derivative analysis will have a major impact on business and engineering decisions to select and incorporate new technologies and innovations into processes. The metrics or measures of performance that are derived from the model are well defined and can be used to track technology impacts across the enterprise and over extended periods of operation.

The Enterprise Derivative Application (EDA) implements energy-derivative analysis for optimization of an industrial process. It is a tool to help industry planners choose the most productive way of making their products while minimizing their cost. Developed using Microsoft (MS) Access and Visual Basic, the application allows users to input initial data ranging from raw material to variable costs and enables the tracking of specific information as material is passed from one process to another.

In this paper we outline the energy-derivative analysis with specific application to the process flow in a mini-mill steel manufacturing². This example consists of twelve process producing five products. Screenshots of the MS-Access application will demonstrate how energy-derivative analysis has been implemented for this specific case.

Although energy-derivative analysis was originally designed for use by the steel industry, it is flexible enough to be applied to many other industrial processes. Examples of processes where energy-derivative analysis would prove useful are wireless monitoring of processes in the petroleum cracking industry and wireless monitoring of motor failure for determining the optimum time to replace motor parts.

One advantage of the MS Access-based EDA is its flexibility in defining the process flow and establishing the relationships between parent and child processes and products resulting from a process. Due to the general design of the program, a process can be anything that occurs over

time with resulting output (products). So the application can be easily modified to many different industrial and organizational environments. Another advantage is the flexibility of defining sensitivity parameters. Sensitivities can be determined between all possible variables in the process flow as a function of time. Thus the dynamic development of the process can be tracked over time and optimized. The EDA is a uniquely flexible and efficient way for planners to choose the most productive way of optimizing production while minimizing costs.

2. ENTERPRISE-DERIVATIVE ANALYSIS

The basis of EDA is the calculation of a set of enterprise-derivative sensitivity parameters that are used in a coupled set of equations to calculate the impacts on a process from a proposed technology or innovation. The assumption is that the proposed technology or innovations will not change the way manufacturing is made but will affect the operational efficiencies about is current operating point. Given this assumption, the process can then be modeled as a first-order Taylor Series expansion about the operating point with changes being influenced by the first differential of a derived benefit. Process gains (production, efficiency, energy, and quality) are estimated as incremental changes from the operating point. The mathematical formulation for any process gain, f, is

$$f(x) = f(\chi_0) + f'(\chi_0)(x - \chi_0) + \dots + \frac{f^n(\chi_0)(x - \chi_0)^n}{n!} + Rn,$$
(1)

where χ_0 is the current plant operating point and *Rn* is a remainder and is ignored in this formulation. In this expansion, we are only interested in the first term, $f'(x_0)$, which is the generalized differential approximation or enterprise-derivative sensitivity term.

The generalized differential approximation (sensitivity) is expanded in general terms as a linear combination of ratios of total differentials of the process changes due to technology innovations (i.e., product, energy, and efficiency). The total differential is:

$$\Delta f_{T_{ech}} = \frac{\partial E}{\partial \eta} \Delta \eta + \frac{\partial \eta}{\partial C} \Delta C + \frac{\partial C}{\partial P} \Delta P + \frac{\partial P}{\partial E} \Delta E + \varepsilon , \qquad (2)$$

where, E, η, C, P are the energy, efficiency, savings, and product, respectively and ε is the error associated with the approximation and is ignored in the EDA.

These sensitivity parameters are based on a total derivative calculation and are approximations to the first partial derivatives of a multiple variable function. The sensitivity parameters are defined below for reference.

 $\frac{\partial E}{\partial \eta}$ is the change in process energy per unit change in efficiency, $\frac{\partial \eta}{\partial C}$ is the change in process efficiency per unit change in costs, and $\frac{\partial C}{\partial P}$ is the change in process costs per unit change in product.

The remaining sensitivity parameter, $\frac{\partial P}{\partial E}$, can be calculated directly or derived as ratios of other sensitivity parameters.

Conducting an EDA involves the following four steps:

- 1. Develop the process flow.
- 2. Compute the sensitivity parameters of the enterprise.
- 3. Conduct a technology assessment and impact analysis.
- 4. Optimization (what-if strategies).

Each step will be described in detail for an example problem² in the following sections. The example problem is process flow in mini-mill steel manufacturing consisting of the twelve processes:

Electric Arc Furnace => Ladle Metallurgy Station => Caster => Tunnel Furnace => Hot strip Mill (HSM). At this point the process splits

HSM => Acid Pickling => Cold Mill Reduction A => Galvanized

HSM => Temper A.

Temper A then splits: Temper A => Cold Mill Reduction B or Temper A => Annealing => Temper B.

3. STEPS OF THE ENTERPRISE DERIVATIVE APPLICATION

3.1 DEVELOPING THE PROCESS FLOW

A requirement for conducting an EDA is to develop a complete understanding of the process: its product flow; material changes; and procedural steps used in the making the product. This understanding also includes identifying energy use, material residence time, and maintenance and operational procedures. This microscopic view of the process is needed to resolve balance of plant issues and to help understand energy, material, and time management as it applies to the current process. In the course of conducting the EDA, a detailed process flow diagram is developed. Roll-ups from these process flow diagrams are then developed along with energy and time management diagrams. Some of the process variables extracted from the diagrams are used in the calculation of the first order Enterprise-Derivative sensitivity parameters.

In the EDA, the user can interactively design the process flow by dragging the process icons into place (Fig. 1). Likewise the user drags the Product icons where desired (in this example there are products out of the TF, GAL, TEMP A, TEMP B and CRM B processes. Once the user has specified the number of processes *m* and products *n* and connected the processes, the user must create the parent-child relationships, name the processes, and save the process flow. Note that in this example there are twelve processes and five products. But there is also a "Process zero" which is the initial feed. The diagram represents the flow of material from the initial feed to successive processes with production of products P1 through P5.



Fig. 1. EDA form for creating the process flow. To develop the process flow, the user drags process icons into place and connects processes in desired manner (see Appendix A for description).

3.2 COMPUTING THE ENTERPRISE SENSITIVITY PARAMETERS

The next step is the computation of the sensitivity parameters. The user must first enter the Enterprise information for each process as shown in Fig. 2.



Fig. 2. On this form the user enters the Enterprise information consisting of required fields: energy, cost, maximum processing capacity, yield, and revenue.

This information includes costs, energy usage, and revenue for each product. Once this information is completed, the sensitivities are computed and displayed as shown in Fig. 3. This EDA Sensitivity form displays the sensitivity parameters for each associated process. The sensitivity parameters (and associated

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EU	APPLICATION SENSITIVITY FO	RM					
Cł	HART EXIT						
	PROCESS	DC/DP	DP/DE	DE/DN	DN/DC	DP/EC1	DE/DC2
	Electric Arc Furnace	37.000	0.0500000000	4000.00	0.00013514	0.05000000	0.00000000
	Ladle Metallurgy Furnace	55.755	0.0625000000	1568.00	0.00018302	0.12500000	0.12500000
	Caster	70.318	0.0454545455	4268.88	0.00007329	0.09090909	0.09090909
	Tunnel Furnace	83.753	0.0555555556	5134.30	0.00004186	0.11111111	0.11111111
	Hot Strip Mill	100.344	0.0454545455	7304.40	0.00003002	0.09090909	0.09090909
	Pickle/Oiler/Dryer	115.525	0.0666666667	2510.06	0.00005173	0.12500000	0.14285714
	Cold Reduction Mill	132.220	0.0476190476	3734.96	0.00004252	0.10000000	0.09090909
	Galvanized	150.717	0.0526315789	388.61	0.00032439	0.09090909	0.12500000
	Temper A	112.525	0.0476190476	3514.08	0.00005311	0.09090909	0.10000000
	Annealing	125.005	0.0588235294	2299.49	0.00005914	0.1000000	0.14285714
	Temper B	142.584	0.0476190476	3238.22	0.00004548	0.09090909	0.10000000
	Cold Reduction Inspection	124.005	0.0625000000	2337.36	0.00005520	0.12500000	0.12500000

Fig. 3. The sensitivity parameters are computed and displayed once the user has completed entering all the Enterprise information.

units) are the ones defined previously $\frac{\partial E}{\partial \eta}$ (kW-h), $\frac{\partial \eta}{\partial C}$ (\$^-1), $\frac{\partial C}{\partial P}$ (\$/ton), $\frac{\partial P}{\partial E}$ (ton/kW-h), and two additional sensitivities which break the energy utilization into both an electricity sensitivity parameter, $\frac{\partial P}{\partial EC1}$ (ton/kW-h), and a natural gas sensitivity parameter, $\frac{\partial P}{\partial EC2}$ (ton/kW-h).

The baseline operation can be expressed in an enterprise matrix (EM) which shows flow of material from one process to the next and of product produced. This matrix completely describes the baseline operation. The matrix can also be stated as ratios of material moved from one process from the next, in which case it is referred to as the R Matrix (RM).

The EM or RM represents the culmination of the enterprise-derivative computation. The EDA has all the information it needs to computer the *status quo* operation, the plant operating point. The user now moves on to conduct a technology assessment and impact analysis, where changes in technology are introduced and products produced by processes are increased or decreased and the impact analysis is made about the original plant operating point.

3.3 CREATING THE ENTERPRISE MATRIX

APPLICATION ENTER	RPRISE MA	TRIX												
VIEW MATERIAL RATI	10													
	FAF	T MT	CACUED	(B) 17	HCM	BICHIE	CBY	CAL	BEND 3	ANDUERT	TTO D	CBT	DROBHCE (EO)	TC N
	EHE	Little	CHOIER	11	пэн	PICKLE	CKM	GHL	IEMP R	HININEHLE	IEMP D	CKI	PRODUCT (TON	(3)
INITIAL	10000													-
EAF		9800												
LMF			9702											_
CASTER				9508										
TF					8300									92
HSM						2391			5578					
PICKLE							2223							
CRM								2045						
GAL													2	202
TEMP A										2705		1623	1	.08
ANNEAL											2570			
TEMP B													2	41
CRI													1	.47
TOTAL TONS	10000	9800	9702	9508	8300	2391	2223	2045	5578	2705	2570	1623	7	92
YIELD %	0.980	0.990	0.980	0.970	0.960	0.930	0.920	0.990	0.970	0.950	0.940	0.910		
ENERGY KW-H/TON	20	16	22	18	22	15	21	19	21	17	21	16		
ENERGY TONS/KW-H	200000	156800	213444	171143	182610	35858	46687	38861	117136	45990	53970	25971		
FIXED COST	7.000	10.000	10.000	4.000	8.000	4.000	5.000	5.000	3.000	6.000	9.000	4.000		
VARIABLE COST	5.000	8.000	4.000	8.000	6.000	7.000	3.000	2.000	5.000	3.000	2.000	4.000		
TOTAL COST	12.000	18.000	14.000	12.000	14.000	11.000	8.000	7.000	8.000	9.000	11.000	8.000		
ACCUMILATED COST	37.755	56.318	71.753	86.344	104.525	124.220	143.717	152.240	116.005	131.584	151.685	136.269		
4														

The user can select to display the Enterprise Matrix as shown in Fig. 4.

Fig. 4. Once the user has entered all the Enterprise information and the sensitivity parameters have been computed, the EM (products transferred from process to process in tons) or the RM (ratio of material moved from one process to the next) can be displayed. Here the EM is shown.

We see here that the EM is an overview of the enterprise-derivative analysis in matrix view. The top half of the screen shot shows the flow of material from one process to another while the bottom half shows the process parameters. At the right of the form, the product, revenue and profit are displayed. The user can select from this "Enterprise Matrix" view (for the EM), which shows transfer in terms of tons of material, to an "R Matrix" view (for the RM), in which the ratio of material moved from one process to another is displayed. To access this feature, the user clicks on the button in the lower right corner. This converts the top half of the form to reflect the material flow as a ratio.

3.2 CONDUCTING A TECHNOLOGY ASSESSMENT AND IMPACT ANALYSIS

Using the information extracted from the process flow diagrams, a technology assessment can be conducted for each manufacturer or company. Plant managers and technical representatives for each of the individual sub-processes are asked to sit in on a session to review the findings of the process flow activity. They are also asked to identify new technologies and needs (or innovations) that are considered important to enhancing their operational performance or increasing overall process efficiency. During the review, any proposed need or technology candidate is identified and listed along with its current operating profile, desired profile, and any figures of merit associated with its use. The amount of change in the product for this process for every specified technology modification is required by the program (Fig. 5). The identification of the operational impacts that these technologies will have on the enterprise/plant/process is included in this analysis. Other indicators of importance include: *variance* defined as labor, maintenance, or productivity; *impact* defined in terms of operations, throughput, or quality; and *priority ranking* defined in terms of high, medium, or low for the particular process step and numerical (1-10) as it would relate to the entire process. These additional indicators provide a measure of importance for each technology or innovation as determined by the plant and technology personnel.

PLICATION	MAIN FORM .	YOUR CURRE	NT PROCESS FLO	W IS DEMO 1_1						
ROCESS FLO	OW SET DEFAULT	T PROCESS FLOW	SET PERCENTAGES	SET INITAL VARIABLES	WORKSHEET	SENSITIVITIES 1	rechnologies e	NTERPRISE MATRIX	OPTIMIZATION	I EXIT
	TION TECHNO	LOGY FORM								
AVE ADD	A ROW DELETE P	ROW EXIT								
Select	Process									
Electr	ic Arc Furnad	ce 💌								
	PROCESS	ADDITIONAL	ANNUAL	THUESTMENT	COST	FNFDCY	FRETCIEN	CY RC1	RC	
	VARIABLE	PRODUCT	EXPENSE	INVESTIBAT	0001	BABROT	AFFICIEN		10	-
V	ariable l	5	\$900.00	\$18,500.00	\$1,887.0	0 10	0.25500	0000 1	.020 0.00	0000000
V	ariable 2	8	\$975.00	\$14,000.00	\$3,108.0	0 16	80 0.42000	0000 1	.680 0.00	000000
		1	41 050 00	617 500 00	¢1 999 0	0 10	0 22000	2000 1	000 0.00	000000
V	ariable 3	5	\$1,050.00	\$17,500.00	71,000.0	-	0.27000	10000	0.00	0000000

Fig. 5. Once the Enterprise has been defined, the user enters the desired technology improvements and their associated product increases (or decreases) for all technology modifications for each process. This form then displays the differential in the sensitivity parameters derived from the associated product change, using the previously computed sensitivity parameters.

The Technology Analysis form allows the user to add or delete new technologies, annual expenses, and investments for each process. After the new technologies and innovations have been identified along with their respective variance, impact, and priority ranking, their economic and process impacts are calculated for the enterprise system. These measures of performance will be in terms of cost saving or yield increases if it were deployed. During a typical study, usually one or the other is given.

Given these economic indicators, the model then calculates three additional parameters; energy, efficiency, and per-process cost savings. Energy savings are computed for electricity, natural gas, and for total energy. These parameters, along with other process data, are used in the subsequent analysis and comparison.

3.5 OPTIMIZING TECHNOLOGICAL CHANGES

The last element in conducting the EDA is selecting the optimal mix of technologies based on some stated criteria. The optimization scheme implemented (algorithm or heuristic) will use the economic and process impacts derived from the energy-derivative analysis coupled with the energy-derivative sensitivity parameters to search for an optimal solution in the value space for a given set of hard and soft constraints. The different optimization approaches include:

Risk Analysis: Risk analysis will determine the process and economic impact of a new operational strategy. If only one operational strategy is to be analyzed, the process and economic impact analysis becomes a straightforward activity using the coupled equations of the enterprise model if the product mix ratios are maintained.

If more than one operational strategy is to be analyzed concurrently, the optimization model uses the enterprise's coupled equations to estimate changes in f(x) assuming the same product mix ratios. As before, the EDA will also provide the parametric analysis figures for each operational strategy, and ultimately suggest the best implementation sequence for the given operational strategies.

Alternative Analysis: Alternative analysis deals with contrasting and comparing two or more operational strategies. The optimization module can calculate changes in f(x) for each operational strategy using the coupled equations, and provide a ranking based on production cost savings, additional throughput and energy savings assuming the product mix ratios are not changed.

Enterprise Analysis: Enterprise-derivative analysis will select the operational strategy or group of operational strategies that will maximize or minimize an objective function given a set of criteria. Since the sensitivity parameters are invariant for each process regardless of the operational strategies, the module can optimize the enterprise through a two-step procedure: 1) the optimization algorithm will select the process or processes that meet a set of multi-goal criteria based on the information contained in the sensitivity parameters and 2) select the operational strategy or group of operational strategies that maximize the benefits of the process(es) as reflected by f(x) and without violating the constraints.

The EDA presents the user with a form (Fig. 6) that shows the differences between the original process and sensitivity parameters and the optimized ones. Negative entries (colored red on the screen) signify a decrease in parameters and positive entries (colored blue on the screen) signify an increase in parameters.

The user can click on the ENTERPRISE MATRIX button on the Optimization form to view an optimized EM (Fig. 6) showing the difference in values due to optimization.

PPLICATION VIEW O	PTIMIZED E	INTERPRIS	E MATRIX												
*RED SIGNIFIES A DE	CREASE *	BLUE SIGN	VIFIES AN	INCREAS	E										
Please choose a gr:	id from be	low													
View Ontinized Rut	ernrise M	etriv				-									
			-	<u></u>											
	EAF	LMF	CASTER	TF	HSM	PICKLE	CRM	GAL	TEMP A	ANNEAL	TEMP B	CRI	PRODUCT (TONS)	REVENUE (\$/TON)	PROFIT (\$/TON)
INITIAL	10000				4.0						· · · · · ·		1		
EAF		9800													
LMF			9702												
CASTER				9508											
TF					8341								927	\$100.00	\$12,949.36
HSM						2415	1		5635						
PICKLE							2246		-						
CRM	8		-		£			2066				S	1-262-272		anner an
GAL													2045	\$165.00	\$28,012.91
TEMP A										2782		1669	1113	\$135.00	\$23,977.39
ANNEAL											2643				
TEMP B													2522	\$175.00	\$70,980.57
CRI													1519	\$145.00	\$17,519.38
TOTAL TONS	10000	9800	9702	9508	8341	2415	2246	2066	5635	2782	2643	1669	8126	\$720.00	\$153,439.61
AIETD #	0.980	0.990	0.980	0.975	0.965	0.930	0.920	0.990	0.988	0.950	0.954	0.910			1.111.111.111.11
ENERGY KW-H/TON	20	16	22	18	22	15	21	19	21	17	21	16	000000		ž
ENERGY TONS/KW-H	200000	156800	213444	171143	183501	36223	47162	39257	118328	47299	55507	26710	1295374		
FIXED COST	7.000	10.000	10.000	4.100	8.081	4.000	5.000	5.000	3.312	6.000	9.197	4.000			
VARIABLE COST	5.000	8.000	4.000	8.000	6.000	7.000	3.000	2.000	5.000	3.000	2.000	4.000			
TOTAL CUST	12.000	18.000	14.000	12.100	14.081	11.000	8.000	7.000	8.312	9.000	11.197	8.000			
RCCUMILATED COST	37.755	56.318	71.753	86.027	103.733	123.369	142.792	151.305	113.455	128.901	146.851	133.468			

Fig. 6. The EM showing the processes that increased product transfer between processes (shown using blue color font) with corresponding decreases in costs (shown using red font).

4. EDA: DETAILED SOFTWARE OVERVIEW

After starting the application, the **MAIN FORM** (Fig. 1) loads displaying a process flow diagram that represents the flow of material from one process to another and the product, if any, a particular process might have.

For the initial use of the EDA, there is a series of steps to follow in order to properly populate the data needed for the EDA calculations. The order is:

- 1. Populate the process names, acronyms, and parent-child relationships by clicking on the **BUILD PROCESS FLOW** button at the top of the form. Documentation for this is found in the document EDA_SetUp.doc
- 2. Assign material flow, material yield, product yield, and maximum processing capacity by clicking on the **SET PERCENTAGES** button at the top of the form.
- 3. Assign initial starting values such as material, cost, etc., by clicking on the **SET INITIAL VARIABLES** button at the top of the form.
- 4. Complete the worksheet for all processes (i.e., cost, energy, etc) by clicking on the **WORKSHEET** button at the top of the form.
- 5. Assign any process variables (technologies), additional products, annual expenses, and investments a particular technology might have by clicking the **TECHNOLOGIES** button at the top of the form.

Once these criteria have been completed, the user can view other parts of the application such as the sensitivities, the enterprise matrix, and the optimization.

After the user has completed step one by building their process flow, they must set the default process flow by clicking on the **SET DEFAULT PROCESS FLOW** button at the top of the form.

The second criterion requirement is to determine the material percentages. To open the **SET PERCENTAGES FORM**, click on the **SET PERCENTAGES** button on the **MAIN FORM**. The **SET PERCENTAGES FORM** is displayed in a data grid. The material flow is the percent of material flowing from one process to another. The default material flow for all processes is 100%. The only time a user should change the material ratio for a process is if it is a child in a split or if there is product for a process. For the example shown in Fig. 1, the **SET PERCENTAGES FORM** is seen below in Fig. 7. Process five is a parent of both process six and process nine. Process five (HSM) sends 30% of its material to Process six (PICKLE) and 70% to Process nine (TEMP A). NOTE: Percentages are entered as whole numbers instead of decimals. Processes that have <u>all</u> material going out to a product would have a material ratio equal to the material yield of that process. The material yield for a process is the material yield for that particular process. The product yield is the percent of material going to product. The Max Process Cap is the maximum cap in production of the process and is used in the optimization.

D APPLICATION M	AIN FORM	YOUR	CURRENT	F PROCESS FLOW	IS DEMO 1_1						
UILD PROCESS FLOW	SET DEFAULT P	PROCESS	FLOW SI	ET PERCENTAGES SE	T INITAL VARIABLES	WORKSHEET	SENSITIVITIES	TECHNOLOGIES	ENTERPRISE MATRIX	OPTIMIZATION	EXIT
		ED AP	PLICATIO	ON PERCENTAGE F	ORM	INITI	AL				
		SAVE	EXIT								
			Acrony	m Material Flo	w % Material Yi	eld % Produ	ct Yield %	Max Process	Cap		
			INITIA	L 100	100	0		0			
			EAF	100	98	0		10500			
			LMF	100	99	0		10000			
			CASTER	100	98	0		10000			
			TF	90	97	10		9750			
			HSM	100	96	0		8750			
			PICKLE	30	93	0		2450			
			CRM	100	92	0		2250			
			GAL	100	99	99		2250			
			TEMP A	70	97	20		6000			
			ANNEAL	50	95	0		3000			
			TEMP B	100	94	94		2750			
			CRI	30	91	91		1750			
					Product 2			Product 4	CRI Product 5		

Fig. 7. The form for setting the material flow percentages.

For the third criterion requirement, the user must open the **INITIAL VARIABLES FORM** (Fig. 8) by clicking **SET INITIAL VARIABLES** in the combo box on the **MAIN FORM** (Fig. 1). The initial cost is any cost associated with starting the flow of material and is NOT the same cost the user will see on the process worksheet form. The initial material is the beginning material that will be introduced into the first process. The other variables are self explanatory and are used in the optimization routine.

ED APPLICATION INIT	IAL VARIABLES FORM	
SAVE EXIT		
	-INITIAL RAW MATERIAL COST PER TON	1
	Fixed Cost:	25
	Variable Cost:	0
	Maintenance Cost:	0
	Total Initial Cost:	25
	Initial (Raw) Material:	10000 TONS
Time Horizo	on For Economic Analyis:	15 YEARS
Enterprise's Att	ractive Rate of Return:	12 %
Enterprise's Avail	able Investment Budget:	70000 \$

Fig. 8. Form for setting the initial variables.

The user then opens the **WORKSHEET FORM**. Two choices are provided for entering the worksheet information: individual or group. At this time, the only fields required are energy,

cost, yield, and revenue – revenue only if the process has product. If the process being worked on has a product, the user can enter revenue on that product in the revenue field. If the process being worked on does not have a product the user is prevented from entering a revenue amount. If selecting the *individual option* (under the **Worksheet tab**), the user must click on the **COST** and or **ENERGY** buttons to open appropriate forms to enter the cost and energy values as sown in Figs. 9-11. If the *group option* (under the **Worksheet tab**) is selected, the user must click on **VIEWS** and then select either **WORKSHEET**, **COST**, or **ENERGY** to enter the appropriate data as shown in Figs. 12, 13.

D APPLICATION WORKSHEET FORM		
5AVE EXIT		
Select Process:	Electric Arc Furna	ce 🔽
Temperature In:	66	DEG F
Temperature Out:	99	DEG F
Residence Time:	0	MIN
Tequilibrium:	0	DEG F
Utilization:	33	*
Process Speed:	0	FT/MIN
*Energy	20	KW-HR/TOK
*Cost	12	\$/TON
*Yield:	98	\$
*Material In:	10000.00	TONS/YR
*Material Out:	9800.00	TONS/YR
*Revenue:	0	\$/TON

Fig. 9. User has selected the *individual option* (under the Worksheet tab) to enter workshe data. In this case the user must click the Energy and Cost buttons to enter that information.

PLICATION WORKSHEET FORM	
EXIT	
Select Process:	Electric Arc Furnace
Temperature In:	66 DEC F
ENERGY FORM FOR ELE	CTRIC ARC FURNACE
SAVE EXIT	
and the second second second	and the second se
Electricity:	20 KW-HR/TON
Natural Gas:	0 RW-HR/TON
Total Energy:	20 RW-HR/TON
	11 \$710N
*Yield:	98 %
*Material In:	10000.00 TONS/YR
*Material Out:	9800.00 TONS/YR
+ Deveryone -	0.5 (70)

Fig. 10. User has selected the *individual option* (under the Worksheet tab) to enter worksheet data. This is the entry form for energy usage.

FXIT			
COST FOR	M FOR ELECTRIC AF	RC FURNACE	-
SAVE EXIT			
	Fixed:	2 \$/TON	
	Variable:	5 \$/TON	
Main	ntenance:	0 \$/TON	
Rej	pairable:	0 \$/TON	
Coz	nsumable:	0 \$/TON	
Tot	al Cost:	12 \$/TON	
		Tone) In	
*Ma	terial Out:	9800.00 TONS/YR	
	*Detremue ·	O \$ (TON	

Fig. 11. User has selected the *individual option* (under the Worksheet tab) to enter worksheet data. This is the entry form for the costs.

SAVE EXIT							
Process Name	Temperature In	Temperature Out	Residence Time	Teguilibrium	Vtilization	Process Speed	Revenue
Electric Arc Furnace	66	99	C		33		0 \$0.00
Ladle Metallurgy Furnace	0	0	C C		0 0	1	0 \$0.00
Caster	0	0	a a a a a a a a a a a a a a a a a a a) 0		0 \$0.00
Tunnel Furnace	0	2	11) 0		0 \$100.00
Hot Strip Mill	0	0	C C) 0	Ĩ	0 \$0.00
Pickle/Oiler/Dryer	0	0	a) 0		0 \$0.00
Cold Reduction Mill	0	0	a) 0		0 \$0.00
Galvanized	0	0	G		0 0		0 \$165.00
Temper A	0	0	C		0 0		0 \$135.00
Annealing	0	0	C C		0 0	1	0 \$0.00
Temper B	0	0	a		0 0		0 \$175.00
Cold Reduction Inspection	0	0	a		0 0		0 \$145.00

Fig. 12. User has selected the *group option* (under the Worksheet tab) to enter worksheet data. This is the entry form for costs.

) AP	PLICATION WORKSHEET FORM		ED APPLICATION WORKSHEET FORM								
TEWS	SAVE EXIT		VIEWS SAVE EVIT								
					SHITE ENTI						
	Busses News	Final Coat	Namishle Cost	Persinahla Cost	Concernable Cont	1			B V		Noterio 7 Con
	Electric Arc Furnace	Fixed cost	Variable cost	i 0	Consumable cost			•	Flectric Brc Furnace	Electricity 20	Natural Gas
Ľ	Ladle Metallurgy Furnace	10	1	3 0	0			-	Ladle Metallurgy Furnace	8	8
	Caster	10	4	. 0	0				Caster	11	11
	Tunnel Furnace	4		3 0	0				Tunnel Furnace	9	9
	Hot Strip Mill	8	e e	5 0	0				Hot Strip Mill	11	11
	Pickle/Oiler/Bryer	4	5	7 0	0				Pickle/Oiler/Dryer	8	7
	Cold Reduction Mill	5		3 0	0				Cold Reduction Mill	10	11
	Galvanized	5	2	2 0	0				Galvanized	11	. 8
	Temper A	3		5 0	0				Temper A	11	10
	Annealing			3 0	0				Annealing	10	7
	Temper B	5	· 2	2 0	0				Temper B	11	. 10
	Cold Reduction Inspection	4	4	L 0	0				Cold Reduction Inspection	8	8

Fig. 13. User has selected the *group option* (under the Worksheet tab) to enter worksheet data. This is the entry form for energy usage.

The final criterion requirement is to fill in the additional technologies on the **TECHNOLOGY ANALYSIS FORM**. To open the **TECHNOLOGY ANALYSIS FORM**, click the **TECHNOLOGIES** button on the **MAIN FORM**. When the form opens (Fig. 5), the first process's technologies, if any, are automatically shown.

This criterion requirement is essential for the optimization routine. To add a new process variable, click on the **ADD A ROW** button on the **TECHNOLOGY FORM**. A new row will appear and the user can enter the new process variable, additional product, annual expense and investment. The variables cost, energy, efficiency, EC1 (1/electricity) and EC2 (1/natural gas) are calculated automatically.

To view the sensitivity parameters, click on the **SENSITIVITIES** button on the **MAIN FORM** to open the **SENSITIVITIES FORM** (Fig. 3). The table displays the sensitivity parameters associated with each process, where the sensitivity parameters are defined as:

DC/DP (or
$$\frac{\partial C}{\partial P}$$
): cost to product sensitivity parameter (\$/ton).
DP/DE (or $\frac{\partial P}{\partial E}$): product to energy sensitivity parameter (ton/kW-h).

DE/Dn (or $\frac{\partial E}{\partial \eta}$): energy to efficiency sensitivity parameter (ton/kW-h). Dn/DC (or $\frac{\partial \eta}{\partial C}$): efficiency to cost sensitivity parameter (\$⁻¹). DP/EC1: product to electricity sensitivity parameter (ton/kW-h). DP/EC2: product to natural gas sensitivity parameter (ton/kW-h).

The user can choose to view a chart by choosing the desired sensitivity parameter by clicking the CHART button. Figure 14 below shows the chart for DC/DP for all process below the table of sensitivity values for all process.

DAPPLICATION SENSITIVITY FORM									
ART EXIT									
PROCESS	DC/DP	DP/DE	DE/DN	DN/DC	DP/EC1	DE/DC2			
Electric Arc Furnace	37.000	0.0500000000	4000.00	0.00013514	0.05000000	0.00000000			
Ladle Metallurgy Furnace	55.755	0.0625000000	1568.00	0.00018302	0.12500000	0.12500000			
Caster	70.318	0.0454545455	4268.88	0.00007329	0.09090909	0.09090909			
Tunnel Furnace	83.753	0.055555556	5134.30	0.00004186	0.11111111	0.11111111			
Hot Strip Mill	100.344	0.0454545455	7304.40	0.00003002	0.09090909	0.09090909			
Pickle/Oiler/Dryer	115.525	0.0666666667	2510.06	0.00005173	0.12500000	0.14285714			
Cold Reduction Mill	132.220	0.0476190476	3734.96	0.00004252	0.10000000	0.09090909			
Galvanized	150.717	0.0526315789	388.61	0.00032439	0.09090909	0.12500000			
Temper A	112.525	0.0476190476	3514.08	0.00005311	0.09090909	0.10000000			
Annealing	125.005	0.0588235294	2299.49	0.00005914	0.10000000	0.14285714			
Temper B	142.584	0.0476190476	3238.22	0.00004548	0.09090909	0.10000000			
Cold Reduction Inspection	124.005	0.0625000000	2337.36	0.00005520	0.12500000	0.12500000			
		Chart For	- DC/DP						
		Chart For	: DC/DP						
160		Chart For	: DC/DP		160				
160		Chart For	c DC/DP		160				
		Chart For	c DC/DP		160				
160 140 120		Chart Fo:	<pre>c DC/DP</pre>		160				
160 140 120 100		Chart For	: DC/DP						
160 140 120 100 80		Chart For	: DC/DP						
		Chart For			160 140 120 100 80	Process			
		Chart For	E DC/DP		160 140 120 100 80 60	Process			
		Chart For			160 140 120 100 80 60 40	Process			
		Chart For	: DC/DP		160 140 120 100 80 60 40 20	Process			
160 140 120 100 80 60 40 20		Chart For			160 140 120 100 80 60 40 40 20	Process			
		Chart For			160 140 120 100 80 60 40 20 20	Process			

Fig. 14. Sensitivity table and chart of DC/DP for all processes.

To view the enterprise matrix, click on the ENTERPRISE MATRIX button on the MAIN FORM to open the ENTERPRISE MATRIX FORM. An overview of the basic EDA application is displayed. The top half shows the flow of material from one process to another while the bottom half shows the process parameters. At the right of the form, the product, revenue, and profit are displayed. Use the horizontal scroll bar to view the entire matrix. To view the ratio of material from one process to another, click on the VIEW MATERIAL RATIO button and the top half of the form reflects the material flow as a ratio. Figure 6 shows the EM and Fig. 15 below shows the enterprise-derivative RM.

MATRIX	CASTER	TF	нѕм								
000 0.5	CRSTER	TF	HSM								
000 0.5	CRSTER	TF	HSM								
000 0.5	CASTER	TF	HSM								
000	CASTER	TF	HSM								
000				PICKLE	CRM	GAL	TEMP A	ANNEAL	TEMP B	CRI	PRODUCT (TONS)
0.9											
0.5	200										
	0.990										
	0.550	0 980									
-	-	0.500	0.873								0.10
				0.288			0.672				0.20
_					0.930						
						0.920					
											0.99
								0.485		0.291	0.20
									0.950		
											0.94
											0.91
98 000	300 9702	9508	8300	2391	2223	2045	5578	2705	2570	1623	792:
80 0.9	90 0.980	0.970	0.960	0.930	0.920	0.990	0.970	0.950	0.940	0.910	
20	16 22	: 18	22	15	21	19	21	17	21	16	
00 1568	213444	171143	182610	35858	46687	38861	117136	45990	53970	25971	
00 10.0	00 10.000	4.000	8.000	4.000	5.000	5.000	3.000	6.000	9.000	4.000	
00 8.0	4.000	8.000	6.000	7.000	3.000	2.000	5.000	3.000	2.000	4.000	
00 18.0	000 14.000	12.000	14.000	11.000	8.000	7.000	8.000	9.000	11.000	8.000	
755 56.3	318 71.753	86.344	104.525	124.220	143.717	152.240	116.005	131.584	151.685	136.269	
	00 98 80 0.5 20 100 1568 100 10.6 100 18.6 100 18.6	00 9800 9702 80 0.990 0.980 20 16 22 00 156800 213444 00 10.000 10.000 100 8.000 4.000 100 18.000 14.000 155 56.318 71.753	00 9800 9702 9508 80 0.990 0.980 0.9702 20 16 22 18 000 156800 213444 171143 000 10.000 4.000 8.000 100 18.000 14.000 12.000 105 56.318 71.753 86.344	00 9800 9702 9508 8300 00 9800 9702 9508 8300 80 0.990 0.980 0.970 0.960 20 16 22 18 22 000 156800 213444 171143 182610 000 10.000 4.000 8.000 6.000 000 18.000 14.000 12.000 14.000 105 55.318 71.753 66.344 104.525	0.000 900 </td <td>0.000 0.000 0.288 0.000 0.288 0.930 0.000 0.000 0.000 0.000 9800 9702 9508 000 9800 9702 9508 8300 2391 000 9800 9702 9508 8300 2391 2223 880 0.990 0.980 0.970 0.960 0.930 0.920 20 16 22 18 22 15 21 000 156800 213444 171143 182610 35888 46687 000 10.000 4.000 8.000 6.000 7.000 3.000 000 18.000 14.000 12.000 14.000 11.000 8.000 000 18.000 14.000 12.000 14.025 124.220 143.717</td> <td>0.000 9702 9508 9300 2391 2223 2045 00 9800 9702 9508 9300 2391 2223 2045 00 9800 9702 9508 9300 2391 2223 2045 00 9800 9702 9508 9300 2391 2223 2045 00 16 22 18 22 15 21 19 00 156800 213444 171143 182610 35858 46687 38861 00 10.000 4.000 8.000 4.000 5.000 7.000 3.000 2.000 18.000 14.000 12.000 14.000 11.000 8.000 7.000 155 56.318 71.753 86.344 104.525 124.220 143.717 152.240</td> <td>Image: constraint of the system of</td> <td>0.000 9702 9508 8300 2391 2223 2045 5578 2705 00 9800 9702 9508 8300 2391 2223 2045 5578 2705 00 9800 9702 9508 8300 2391 2223 2045 5578 2705 00 9800 9702 9508 8300 2391 2223 2045 5578 2705 00 9800 9702 9508 8300 2391 2223 2045 5578 2705 00 156800 213444 17113 182610 38858 46687 38861 117136 45990 00 10.000 10.000 8.000 6.000 7.000 3.000</td> <td>Image: constraint of the second sec</td> <td>0.000 <th< td=""></th<></td>	0.000 0.000 0.288 0.000 0.288 0.930 0.000 0.000 0.000 0.000 9800 9702 9508 000 9800 9702 9508 8300 2391 000 9800 9702 9508 8300 2391 2223 880 0.990 0.980 0.970 0.960 0.930 0.920 20 16 22 18 22 15 21 000 156800 213444 171143 182610 35888 46687 000 10.000 4.000 8.000 6.000 7.000 3.000 000 18.000 14.000 12.000 14.000 11.000 8.000 000 18.000 14.000 12.000 14.025 124.220 143.717	0.000 9702 9508 9300 2391 2223 2045 00 9800 9702 9508 9300 2391 2223 2045 00 9800 9702 9508 9300 2391 2223 2045 00 9800 9702 9508 9300 2391 2223 2045 00 16 22 18 22 15 21 19 00 156800 213444 171143 182610 35858 46687 38861 00 10.000 4.000 8.000 4.000 5.000 7.000 3.000 2.000 18.000 14.000 12.000 14.000 11.000 8.000 7.000 155 56.318 71.753 86.344 104.525 124.220 143.717 152.240	Image: constraint of the system of	0.000 9702 9508 8300 2391 2223 2045 5578 2705 00 9800 9702 9508 8300 2391 2223 2045 5578 2705 00 9800 9702 9508 8300 2391 2223 2045 5578 2705 00 9800 9702 9508 8300 2391 2223 2045 5578 2705 00 9800 9702 9508 8300 2391 2223 2045 5578 2705 00 156800 213444 17113 182610 38858 46687 38861 117136 45990 00 10.000 10.000 8.000 6.000 7.000 3.000	Image: constraint of the second sec	0.000 0.000 <th< td=""></th<>

Fig. 15. Once the user has entered all the Enterprise information and the sensitivity parameters have been computed, the EM (products transferred from process to process in tons) or the RM (ratio of material moved from one process to the next) can be displayed. Here the RM is shown.

To run an analysis or optimization routine, click on the **OPTIMIZATION** button on the **MAIN FORM**. The user can run a risk analysis, alternative analysis or optimization #1: increase throughput maximize profit. The **RISK FORM** (Fig. 16) shows the amount of increase in tons there will be per additional amount of product produced as well as energy and profit increases or decreases. The annual worth is a measure for ith new operational strategy. The **ALTERNATIVE ANALYSIS FORM** (Fig. 17) shows the rankings of annual worth and energy used for each new operation strategy introduced.

The combo box on the optimization form allows the user to see the calculations needed to perform the optimization. For example, Fig. 18 shows the differences in the sensitivity parameters before and after optimization. The **OPTIMIZED ENTERPRISE MATRIX FORM** (Fig. 19) shows the new matrix flow due to the optimization.

STRATEGY	PROCESS	ADDITIONAL PRODUCT	ANNUAL EXPENSE	INVESTMENT	PRODUCT 1	PRODUCT 2	PRODUCT 3	PRODUCT 4	PRODUCT 5	ENERG
1	1	84	\$975.00	\$14,000.00	3	3	3	3		
2	1	54	\$1,050.00	\$17,500.00						
3	1	51	\$900.00	\$18,500.00	0		0			0
4	2	55	\$935.00	\$16,000.00	5.50	14.85	6.93	21.66	12.99	5864.2
5	3	86	\$1,555.00	\$25,000.00	8.60	23.22	10.84	33.86	20.32	7277.5
6	3	74	\$1,960.00	\$38,500.00	7.40	19.98	9.32	29.14	17.48	6262.0
7	4	23	\$925.00	\$13,500.00	2.30	6.21	2.90	9.06	5.43	1532.3
8	4	45	\$955.00	\$12,500.00	4.50	12.15	5.67	17.72	10.63	2998.0
9	4	100	\$1,950.00	\$26,000.00	10.00	27.00	12.60	39.38	23.63	6662.2
10	4	38	\$1,750.00	\$21,500.00	3.80	10.26	4.79	14.96	8.98	2531.6
11	5	42	\$675.00	\$10,500.00		12.60	5.88	18.38	11.02	2185.0
12	6	12	\$1,225.00	\$11,500.00		12.00				480.0
13	6	33	\$450.00	\$11,000.00		33.00				1320.0
14	6	21	\$1,350.00	\$13,000.00	8	21.00	8	8	0	840.0
15	7	20	\$675.00	\$17,500.00		20.00				380.0
16	8	15	\$1,300.00	\$10,500.00		15.00				
17	9	35	\$480.00	\$12,000.00			5.83	18.23	10.94	867.7
18	9	63	\$1,280.00	\$21,500.00			10.50	32.81	19.69	1561.8
19	9	14	\$275.00	\$14,500.00			2.33	7.29	4.38	347.0
20	10	20	\$625.00	\$19,000.00				20.00		420.0
21 00	11	36	\$520.00	\$12,000.00				36.00	<i></i>	
22	11	22	\$950.00	\$21,000.00	5	÷	5	22.00		0
23	12	20	\$595.00	\$15,750.00					20.00	

Fig. 16. RISK FORM showing the amount of increase in tons there will be per additional amount of product produced as well as energy and profit increases or decreases.

	N ME CENS							
STRATEGY	PROCESS	ADDITIONAL PRODUCT	ANNUAL EXPENSE	INVESTMENT	STRATEGY	ANNUAL WORTH	STRATEGY	ENERGY USED
1	1	84	\$975.00	\$14,000.00	2	(\$596,594.42)	1	
2	1	54	\$1,050.00	\$17,500.00	3	(\$596,591.25)	2	
3	1	51	\$900.00	\$18,500.00	1	(\$596,005.54)	3	
4	2	55	\$935.00	\$16,000.00	12	(\$1,113.48)	16	1226225
5	3	86	\$1,555.00	\$25,000.00	16	(\$366.65)	21	1226225
6	3	74	\$1,960.00	\$38,500.00	19	(\$359.37)	22	1226225
7	4	23	\$925.00	\$13,500.00	22	(\$183.31)	23	1226225
8	4	45	\$955.00	\$12,500.00	20	(\$134.66)	19	1226572
9	4	100	\$1,950.00	\$26,000.00	14	(\$108.72)	15	1226605
10	4	38	\$1,750.00	\$21,500.00	15	(\$84.42)	20	1226645
11	5	42	\$675.00	\$10,500.00	23	(\$7.48)	12	1226705
12	6	12	\$1,225.00	\$11,500.00	7	\$319.72	14	1227065
13	6	33	\$450.00	\$11,000.00	10	\$424.58	17	1227093
14	6	21	\$1,350.00	\$13,000.00	6	\$1,881.28	13	1227545
15	7	20	\$675.00	\$17,500.00	17	\$2,869.57	7	1227757
16	8	15	\$1,300.00	\$10,500.00	13	\$2,884.93	18	1227787
17	9	35	\$480.00	\$12,000.00	4	\$3,002.17	11	1228410
18	9	63	\$1,280.00	\$21,500.00	8	\$3,523.08	10	1228757
19	9	14	\$275.00	\$14,500.00	21	\$4,018.11	8	1229223
20	10	20	\$625.00	\$19,000.00	11	\$4,451.90	4	1232089
21	11	36	\$520.00	\$12,000.00	18	\$4,763.90	6	1232487
22	11	22	\$950.00	\$21,000.00	5	\$5,807.98	9	1232887
23	12	20	\$595.00	\$15,750.00	9	\$8,262.32	5	1233503

Fig. 17. ALTERNATIVE ANALYSIS FORM shows the rankings of annual worth and energy used for each new operation strategy introduced.

*RED SIGNIFIES	TRED SIGNIFIES A DECREASE *BLUE SIGNIFIES AN INCREASE											
Please choose a grid from below												
View Changes In Process Decementary After Optimization 1												
view changes	IN FICE	iss Para	amecers	AICEL	opermis	acion i		<u> </u>				
Process	1	2	3	4	5	6	7	8	9	10	11	12
P Original	10000	9800	9702	9508	8300	2391	2223	2045	5578	2705	2570	162
P New	10000	9800	9702	9508	8341	2415	2246	2066	5635	2782	2643	166
P Change					41	24	23	21	57	77	73	4
¥ Original	0.980	0.990	0.980	0.970	0.960	0.930	0.920	0.990	0.970	0.950	0.940	0.91
Y New	0.980	0.990	0.980	0.975	0.965	0.930	0.920	0.990	0.988	0.950	0.954	0.91
Y Change				0.005	0.005				0.018		0.014	
E Original	200000	156800	213444	171143	182610	35858	46687	38861	117136	45990	53970	2597:
E New	200000	156800	213444	171143	183501	36223	47162	39257	118328	47299	55507	2671
E Change					891	365	475	395	1192	1309	1537	73:
Ft Original	7.000	10.000	10.000	4.000	8.000	4.000	5.000	5.000	3.000	6.000	9.000	4.00
Ft New	7.000	10.000	10.000	4.100	8.081	4.000	5.000	5.000	3.312	6.000	9.197	4.00
Ft Change				0.100	0.081				0.312		0.197	
ACT Original	37.8	56.3	71.8	86.3	104.5	124.2	143.7	152.2	116.0	131.6	151.7	136.
ACT New	37.8	56.3	71.8	86.0	103.7	123.4	142.8	151.3	113.5	128.9	146.9	133.
ACT Change	ACT Change -0.3 -0.8 -0.9 -0.9 -0.9 -2.5 -2.7 -4.8 -2.8											

Fig. 18. Differences in the sensitivity parameters before and after optimization.

APPL	PPLICATION VIEW OPTIMIZED ENTERPRISE MATRIX															
T																
*R P	ED SIGNIFIES & DE lease choose a gr: lew Optimized Ent	CREASE *1 id from be erprise M	BLUE SIGN :low atrix	VIFIES AN	INCREAS	E	<u> </u>									
		EAF	LMF	CASTER	TF	HSH	PICKLE	CRM	GAL	TEMP A	ANNEAL	TEMP B	CRI	PRODUCT (TONS)	REVENUE (\$/TON)	PROFIT (\$/TON)
	INITIAL	10000				-								· · · · · · · · · · · · · · · · · · ·		
1	TAF	6	9800				6									
1	hæ			9702												
	CASTER	Ĵ.			9508				i i							
	F	1				8341								927	\$100.00	\$12,949.36
1	ISM						2415	1		5635						
1	PICKLE							2246								
1	CRM	s			_		3		2066							
1	FAL													2045	\$165.00	\$28,012.91
	TENP A										2782		1669	1113	\$135.00	\$23,977.39
1	INNEAL											2643				
2	END B													2522	\$175.00	\$70,980.57
1	RI													1519	\$145.00	\$17,519.38
4	TOTAL TONS	10000	9800	9702	9508	8341	2415	2246	2066	5635	2782	2643	1669	8126	\$720.00	\$153,439.61
	TIELD &	0.980	0.990	0.980	0.975	0.965	0.930	0.920	0.990	0.988	0.950	0.954	0.910			
1	SNERGY KW-H/TON	20	16	22	18	22	15	21	19	21	17	21	16			· · · · · · · · · · · · · · · · · · ·
1	INERGY TONS/KW-H	200000	156800	213444	171143	183501	36223	47162	39257	118328	47299	55507	26710	1295374		
1	IXED COST	7.000	10.000	10.000	4.100	8.081	4.000	5.000	5.000	3.312	6.000	9.197	4.000			
	FARIABLE COST	5.000	8.000	4.000	8.000	6.000	7.000	3.000	2.000	5.000	3.000	2.000	4.000			
-	TOTAL COST	12.000	18.000	14.000	12.100	14.081	11.000	8.000	7.000	8.312	9.000	11.197	8.000			
i	ACCUMILATED COST	37.755	56.318	71.753	86.027	103.733	123.369	142.792	151.305	113.455	128.901	146.851	133.468			

Fig. 19. OPTIMIZED ENTERPRISE MATRIX FORM shows the new matrix flow due to the optimization.

5. CONCLUSIONS

In the new economy, companies will be looking at R&D investments as a means to increase market share and equity along with revenue, profit, and dividends. They will be concerned with understanding the technology's complete impact, what its total cost of ownership will be, and what the uncertainty and risk associated its R&D investments is. In light of this, companies will be looking for ways to reduce or eliminate these risks. The EDA based on MS Access, will help in this by making available to these companies new tools for developing and managing investment strategies and risks.

The benefits derived from conducting an energy-derivative analysis using EDA are many and include:

- Quantifying the impact that a particular technology has in a plant in terms of economic benefits, energy saved, efficiency increases, and product gains.
- Providing metrics for a strategic decision making process.
- Identifying unique parameters that can be used to characterize a system's performance.
- Contrasting and comparing different technologies for a particular process or across the enterprise.
- Selecting best technology mix based on a set of criteria (optimization).
- Calculating total impact on an enterprise and total cost of ownership.
- Tracking process and economic impact over time.
- Strategizing (risk management) based on expectations.

An energy-derivative analysis can have a major impact on how companies manage risk and make R&D investment decisions in the future.

The Enterprise Derivative Application is an MS Access application which implements energyderivative analysis for optimization of an industrial process. It is a tool to help industry planners choose the most productive way of making their products while minimizing their cost. Based on the calculation of Enterprise-Derivative sensitivity parameters, the EDA can display a particular sensitivity or all sensitivities can be compared for all processes. This was shown for a specific application of a steel mini mill production process.

Energy-derivative analysis was demonstrated to be flexible enough to be applied to many other industrial processes besides the steel process shown here. Examples of processes where energy-derivative analysis would prove useful are:

- Wireless monitoring of processes in the petroleum cracking industry;
- Wireless monitoring of motor failure for determining the optimum time for replacement of parts;
- Optimizing the air-transport of cargo; and
- Optimizing the design of new military material design and deployment strategies (e.g., Future Combat Systems).

A particular advantage of the MS Access-based application is its flexibility in defining the process flow and establishing the relationships between parent and child process and between processes and products. The application can be easily modified to apply to many different industrial and organizational environments. Another advantage is the flexibility of defining sensitivity parameters. Sensitivities can be determined between all possible variables in the process flow as a function of time. The dynamic development of the process can be tracked over time and optimized. The energy-derivative analysis is a uniquely flexible and efficient way for planners to choose the most productive way of optimizing production while minimizing costs. The MS Access-based EDA is a particularly flexible and robust implementation of energy-derivative analysis and it should prove useful in the analysis and optimization of industrial processes.

6. REFERENCES

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APPENDIX A: SET UP FORM FOR EDA

APPENDIX A: SET UP FORM FOR EDA

Before the application can be used, the user must work through a series of steps to ensure the application works correctly. This user's guide will walk the user through the steps of determining the parent-child relationships. The parent-child relationships determine the flow of product from one process to another as well as any final product.

To begin, open the EDA.mdb database. The **MAIN FORM** will open (Fig. 1). The form shows the default process flow, in this case DEMO 1_1, as indicated in the forms caption bar. To create a new process flow, click on the **BUILD PROCESS FLOW** button at the top left of the form.

On the **SET UP** form (Fig. A1) the user can build a process flow or load an existing process flow to work with. This figure shows the options available when the user clicks on the **BUILD PROCESS FLOW** button. The user is guided through the order from determining the processes/products to saving the process flow diagram. If a problem occurs, any part of the process can be reset. Following the given steps is self explanatory and once the user saves the process flow and clicks on the **EXIT** button, they can begin populating their process flow as given in the process flow overview.

The first step in building a process flow is to specify the number of processes and products as seen in Fig. A2. Click on the **Go** menu option (Fig. A1) under the **Determine Processes/Products** pull-down menu item, and enter the number of process and products needed for the process flow (Fig. A2). The number of products can not exceed the number of processes.

JILD PROCESS FLOW LOAD EXISTING PRO	CESS	FLOW EXIT		
Determine Processes/Products	•	Go		
Draw Process Flow Diagram	Þ	Reset		
Align Processes/Products				
Create Parent-Child Relationships	•			
Create Names And Acronyms For Processes	;)			
Save Process Flow Diagram				
Reset All				
		1		

Fig. A1. SET UP FORM for building a process flow or loading a previously built process.





Once these have been saved, the next step is to draw the process flow diagram. Upon choosing the **Draw Process Flow Diagram** pull-down menu item and selecting **Start** option (Fig. A3), a grid appears with buttons to the left (Fig. A4). Draw the process flow diagram as you want it to appear on the main form. How it is drawn here is how it will look. Simply drag each button to a place on the grid and drop it. It is not important to exactly align the buttons; this will be done later; for now just get each button approximately aligned. Be sure to place the numbers in numerical order as seen in Fig. A5.

D APPLICATION				
UILD PROCESS FLOW	OAD EXISTING PROC	ESS	FLOW EXIT	
Determine Processes/Pr	oductsFINISHED	÷,	1	
Draw Process Flow Diag	ram	►	Start	1
Align Processes/Product	:S		Finish	
Create Parent-Child Rel	ationships	•	Reset	
Create Names And Acro	nyms For Processes	Ъ		
Save Process Flow Diag	ram			
Reset All				
		-		

Fig. A3. To get the grid for creating the process flow, click on the Start

APPLICATION												
OLD PROCESS FLOW	ISTING PROCESS	reow e										
Process 0 Process												
Process 1									_			
Process 2												
Process 3												
Product 1												
			_									

Fig. A4. Grid for creating the process flow.

Once the user is finished with drawing the process flow diagram, click on the **Align Processes/Products** pull-down to provide the aligned process flow (Fig. A5).

ED APPLICATION	
BUILD PROCESS FLOW LOAD EXISTING PROCESS FLOW	EXIT
Determine Processes/ProductsFINISHED Draw Process Flow DiagramFINISHED Align Processes/ProductsFINISHED Create Parent-Child Relationships Greate Names and Acronyms For Processes Save Process Flow Diagram Reset All Process 3	Process 0 Process 1 Process 2 Process 4

Fig. A5. Process flow after placing processes and products on the grid.

To create parent child relationships, simply choose that option on the pull-down menu (Fig. A6) and click first on the parent and click on the child. A line will be drawn connecting the two, signifying the relationship has been made. You do not have to create the relationships in order.

D APPLICATION		
UILD PROCESS FLOW LOAD EXISTING PROCESS FLO	DW EXIT	
Determine Processes/ProductsFINISHED Draw Process Flow DiagramFINISHED Align Processes/ProductsFINISHED Create Description Child Pathooching Sector Processes/ProductsFINISHED	Process 0	
Create Names and Acronyms For Processes F Save Process Flow Diagram R	Finish Reset Process 1	
Reset All	Process 2	
Process	5 3 Pro	ocess 4
Product	5 1	oduct 2

Fig. A6. Select Create Parent-Child Relationships from pull-down menu.

The next step is to assign names and acronyms to processes. The user chooses the pull-down menu option **Create Names and Acronyms for Processes** (Fig. A7), then selects **Create**, and fills in the names and acronyms for the processes as shown in Fig. A8.

ED APPLICATION			
BUILD PROCESS FLOW LOAD EXISTING PROCESS F	LOW EXIT		
Determine Processes/ProductsFINISHED Draw Process Flow DiagramFINISHED Align Processes/ProductsFINISHED Greate Parent-Child RelationshipsFINISHED		Process 0	
Create Names and Acronyms For Processes Save Process Flow Diagram Reset All	Create Reset	Process 1	
Proce	.55 3	Process 2	Process 4
Produ	let 1		Product 2

Г	Process 2	
Process	3 Proce	ss 4
DA APPLICATIO	NCREATE PROCESS NAME AND ACR	ONYM
SAVE EXIT		
	Process Name	Process Acronym
Process 0	Initial	INITIAL
Process 1	Process 1	PROCS 1
Process 2	Process 2	PROCS 2
Process 3	Process 3	PROCS 3
	Process 4	PROCS 4

Process 0

Fig. A7. Select Create Names and Acronyms for Processes

Fig. A8. Entering names and acronyms for processes.

The completed process flow diagram is shown in Fig. A9. The last step is to save the process flow diagram information by clicking on the pull-down item **Save Process Flow Diagram**. At this time, enter a name for the new process flow. The user can now exit out of the **Build Process Flow** feature and start populating the newly created process flow diagram.



Fig. A8. Final process flow diagram. User can now save the diagram and exit the process flow set-up.

APPENDIX B: FIX FOR RUNNING APPLICATION

APPENDIX B: FIX FOR RUNNING APPLICATION

We ran into a problem implementing the EDA on machines that did not have Visual Basic installed. On these machines you may get the error that certain system routines are missing (in our case the routine was **mschrt20.ocx**). The failure occurred when selecting the menu item **Sensitivities** which is using charting capability to chart the sensitivity values for all processes. This was corrected by downloading the routine (**mschrt20.ocx**) and moving it to the C:\Windows\System32 directory. The file must be registered using the following command:

C:\Windows\System32>regsvr32 mschrt20.ocx

mschrt20.ocx was obtained from this site: <u>http://www.ocxdump.com/download-ocx-files_new.php/ocxfiles/M/mschrt20.ocx/6.00.81774/download.html</u>.

This fixed the problem and we were able to successfully run the application and produce the charts.